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ELECTRICAL DOUBLE LAYER.

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**ADSORPTION AT THE MERCURY-AQUEOUS SOLUTION
ELECTRICAL DOUBLE LAYER**

Alan R. Sears

**A Dissertation Presented to the Faculty
of the Graduate School of Yale University
in Candidacy for the Degree of
Doctor of Philosophy**

1971

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SUMMARY

The adsorption of KBr from $x\text{M}\text{KBr} + (1-x)\text{MKF}$ and of $x\text{M}6\text{-amino-hexanoic} + .5\text{MKF}$ at the mercury aqueous solution interface has been investigated. The necessary data were obtained by determining the differential capacity curve, the streaming electrode potential and the surface tension at the point of zero charge. The adsorption of KBr from $\text{KBr} + \text{KF}$ has been shown to be similar to KCl from $\text{KCl} + \text{KF}$ if the data in the same range of specifically adsorbed charge are compared. The results at larger values of specifically adsorbed charge have not previously been observed for halide systems. They can be explained by assuming a standard free energy with both linear and quadratic terms and variable isotherm parameters. The bromide and chloride results imply that the simpler picture for the iodide ion is due to the limited range of surface charge which has been studied. Within the range of surface charge available, 6 amino-hexanoic acid is maximally adsorbed when the surface charge density is -6 , with a quadratic standard free energy of adsorption. The expectation that this system would show some of the characteristics of ionic adsorption proved to be incorrect. The quadratic standard free energy, which implies the adsorption of a point dipole, indicates that in this system adsorption should be considered to occur in the entire double layer rather than only in the inner layer. This assumption is necessitated by the dipole being significantly larger than the inner layer.

Glossary

The symbols occurring below are those which frequently are used in the text.

γ	surface tension
Γ_X	surface excess of X in Gibbs model
$\Gamma_{X,w}$	relative surface excess of X
Γ^d	surface concentration in the diffuse layer
Γ^i	surface concentration in the inner layer.
q, q^M	surface charge density on mercury
q^s	surface charge density in solution
q^d	surface charge density in diffuse layer
q^l	surface charge density of specifically adsorbed ions
E^\pm	potential of cell against a reversible electrode
E, E_{ref}	potential of cell against a reference electrode
E_z	potential of cell at the point of zero charge
ϕ^m	potential in the mercury electrode
ϕ^1	potential at the inner Helmholtz layer
ϕ^2	potential at the outer Helmholtz layer
ϕ^{m-2}	potential drop across the inner layer

C	capacity of the double layer
C^d	capacity of the diffuse layer
C^i	capacity of the inner layer
$q C^i$	differential capacity at constant amount adsorbed.
$q^i C^i$	differential capacity at constant charge
$q K^i$	integral capacity at constant amount adsorbed
$q^i K^i$	integral capacity at constant charge
X_1	position of the inner Helmholtz layer
X_2	position of the outer Helmholtz layer
ξ	$\xi = \gamma + qE$
E^b	value of E for base solution
C^b	value of C for base solution
ξ^b	value of ξ for base solution
$\Delta \frac{1}{C}$	$\frac{1}{C} - \frac{1}{C^b}$
ΔE	$E - E^b$
Φ	$\xi - \xi^b$ surface pressure
δ	$q - q_{\max}$

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I. THEORY OF THE ELECTRICAL DOUBLE LAYER

The region of the electrode solution interface is known as the electrical double layer. The generally accepted model of this interface consists of the metallic phase, the compact or inner layer and the diffuse layer as is shown in Figure 1. The compact layer is divided into two parts. The inner Helmholtz plane is the plane of closest approach of specifically adsorbed ions. An ion is specifically adsorbed if its adsorption can not be explained by diffuse layer theory. All adsorption of neutral molecules is therefore specific adsorption. The outer Helmholtz plane is the plane of closest approach of completely solvated ions. The diffuse layer begins at the outer Helmholtz plane and extends into the solution until the solution has its bulk concentration. The thermodynamic theory does not depend on the above model, but only on the existence of an interface and the absence of charge transfer across the interface. The Gouy-Chapman-Stern theory presupposes the model used and is applicable only to the diffuse layer. The thermodynamic derivation and that of the Gouy-Chapman-Stern theory are classical. The most complete discussion of both may be found in Mohilner's article.¹ The entire theory of the double layer is also discussed by Delahay.² The material discussed in Sections C and D is based on a method of analysis developed by Grahame and Parsons over the last twenty years. No single source is available in which the complete theory of the double layer is presented. A careful review of the theory was therefore considered advisable.

A. The Thermodynamic Derivation of the Electrocapillary Equation

The system which I will first describe is represented by the

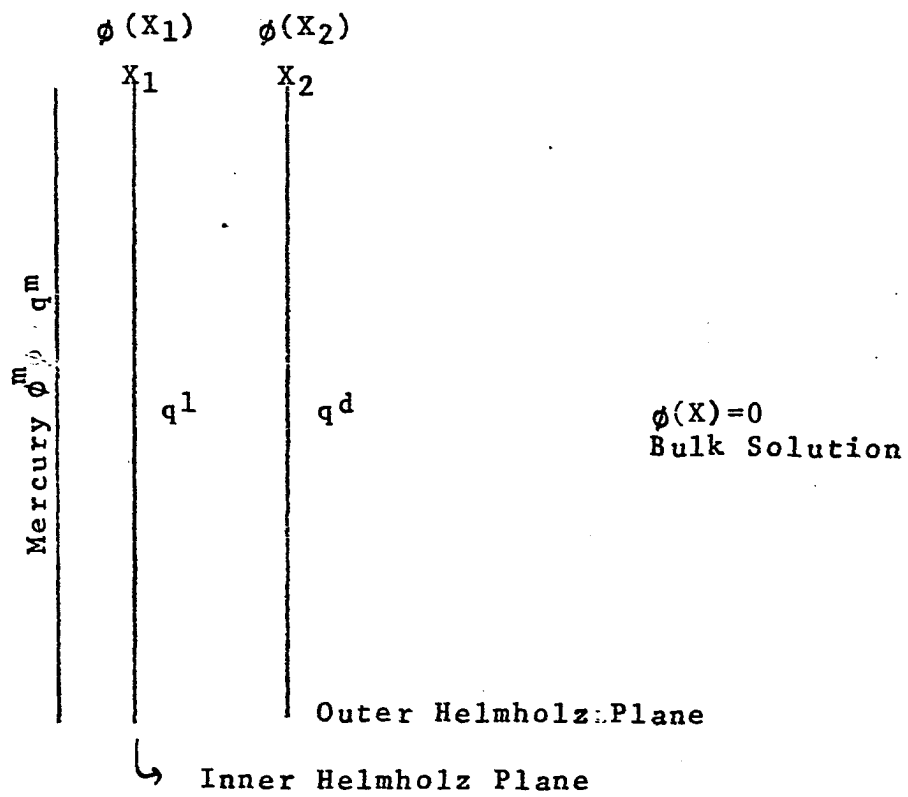
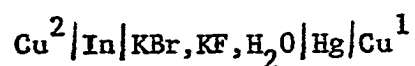


Figure 1. A Schematic Representation of The Electrical Double Layer

following cell:



The electrode In is a hypothetical K^+ reversible electrode in contact with the solution. A Br^- or F^- reversible electrode could also be used in the derivation. It will later be shown that a constant potential electrode may always be used instead of a reversible electrode. We assume that if a potential is imposed across the cell, equilibrium is reached, and that no charge transfer occurs across the interface. We then get the Gibbs absorption equation for this system:

$$\begin{aligned} dy = & - \Gamma_e d\bar{\mu}_e - \Gamma_{\text{Hg}^+} 2d\bar{\mu}_{\text{Hg}^+2} - \Gamma_{\text{K}^+} d\bar{\mu}_{\text{K}^+} - \Gamma_{\text{F}^-} d\bar{\mu}_{\text{F}^-} \\ & - \Gamma_{\text{Br}^-} d\bar{\mu}_{\text{Br}^-} - \Gamma_{\text{H}_2\text{O}} d\mu_{\text{H}_2\text{O}} \end{aligned}$$

The μ are the electrochemical potentials in either mercury or the solution. The Γ are the surface excesses per unit area and will depend on the choice of the Gibbs plane. γ is the surface tension.

In the metallic phase

$$\mu_{\text{Hg}} = \bar{\mu}_{\text{Hg}^+2} + 2\bar{\mu}_{e^-}$$

and

$$\bar{\mu}_{e^-}^{\text{Hg}} = \bar{\mu}_{e^-}^{\text{Cu}^1}$$

therefore

$$\begin{aligned} - \Gamma_e d\bar{\mu}_e^{\text{Hg}} - \Gamma_{\text{Hg}^+2} d\bar{\mu}_{\text{Hg}^+2} &= - (\Gamma_e - 2\Gamma_{\text{Hg}^+2}) d\bar{\mu}_e^{\text{Cu}^1} \\ &- \Gamma_{\text{Hg}^+2} d\mu_{\text{Hg}} \end{aligned}$$

Let q^M be the charge per unit area on the metal surface and
 $d\mu_{Hg} = 0$ since we are restricting ourselves to constant T and P.

$$q^M = -F(\Gamma_{e^-} - 2\Gamma_{Hg^{+2}})$$

and

$$dY = \frac{q^M}{F} d\bar{\mu}_{e^-}^{Cu^I} - \Gamma_K^+ d\bar{\mu}_K^+ - \Gamma_{Br^-} d\bar{\mu}_{Br^-} \\ - \Gamma_F^- d\bar{\mu}_F^- - \Gamma_{Br^-} d\bar{\mu}_{Br^-} - \Gamma_{H_2O} d\mu_{H_2O}$$

also

$$\mu_{KF} = \bar{\mu}_K^+ + \bar{\mu}_F^-$$

$$\mu_{KBr} = \bar{\mu}_K^+ + \bar{\mu}_{Br^-}$$

therefore

$$- \Gamma_K^+ d\bar{\mu}_K^+ - \Gamma_F^- d\bar{\mu}_F^- - \Gamma_{Br^-} d\bar{\mu}_{Br^-} = \\ - (\Gamma_K^+ - \Gamma_F^- - \Gamma_{Br^-}) d\bar{\mu}_K^+ - \Gamma_F^- d\mu_{KF} - \Gamma_{Br^-} d\mu_{KBr}$$

Let q^S be the charge per unit area in the solution:

$$q^S = F(\Gamma_K^+ - \Gamma_F^- - \Gamma_{Br^-})$$

therefore

$$dY = \frac{q^M}{F} d\bar{\mu}_{e^-}^{Cu^I} - \frac{q^S}{F} d\bar{\mu}_K^+ - \Gamma_F^- d\mu_{KF} \\ - \Gamma_{Br^-} d\mu_{KBr} - \Gamma_{H_2O} d\mu_{H_2O}$$

The indicator electrode is reversible to the K^+ ion.

therefore

$$\bar{\mu}_{K^+}^{In} + \bar{\mu}_e^{-In} = \mu_K$$

and

$$d\bar{\mu}_e^{-In} = d\bar{\mu}_{K^+}^{In}$$

also

$$d\bar{\mu}_{K^+}^{In} = d\bar{\mu}_{K^+}^{(solution)}$$

$$d\bar{\mu}_e^{-In} = d\bar{\mu}_e^{-Cu^2}$$

and

$$q^M = -q^S$$

to preserve electroneutrality. Therefore

$$\frac{q^M}{F} d\bar{\mu}_e^{-Cu^1} - \frac{q^S}{F} d\bar{\mu}_{K^+} = + \frac{q^M}{F} d(\bar{\mu}_e^{-Cu^1} - \bar{\mu}_e^{-Cu^2})$$

but

$$\bar{\mu}_e^{-Cu^1} = \mu_e - F\phi^{Cu^1}$$

$$\bar{\mu}_e^{-Cu^2} = \mu_e - F\phi^{Cu^2}$$

therefore

$$\begin{aligned} \frac{q^M}{F} d(\bar{\mu}_e^{-Cu^1} - \bar{\mu}_e^{-Cu^2}) &= -q^M d(\phi^{Cu^1} - \phi^{Cu^2}) \\ &= -q^M dE^+ \end{aligned}$$

where E^+ is the potential of the cell with a cation reversible indicator electrode. The symbol q will now be used in place of q^M to designate the surface charge per unit area on the mercury surface.

We now have:

$$dy = - qdE^+ - \Gamma_{Br^-} d\mu_{KBr} - \Gamma_{F^-} d\mu_{KF} - \Gamma_{H_2O} d\mu_{H_2O}$$

The Gibbs-Duhem gives us

$$d\mu_{H_2O} = - \frac{x_{KBr}}{x_{H_2O}} d\mu_{KBr} - \frac{x_{KF}}{x_{H_2O}} d\mu_{KF}$$

therefore

$$dy = - qdE^+ - \left(\Gamma_{Br^-} - \frac{x_{KBr}}{x_{H_2O}} \Gamma_{H_2O} \right) d\mu_{KBr} \\ - \left(\Gamma_{F^-} - \frac{x_{KF}}{x_{H_2O}} \Gamma_{H_2O} \right) d\mu_{KF}$$

or

$$dy = - qdE^+ - \Gamma_{F^-,w} d\mu_{KF} - \Gamma_{Br^-,w} d\mu_{KBr}$$

The quantities $\Gamma_{F^-,w}$, $\Gamma_{Br^-,w}$ are called the relative surface excesses. They are the experimentally determined surface excesses and are independent of the position of the Gibbs surface. If we had used a fluoride reversible indicator electrode, we would get the equation:

$$dy = - qdE^- - \Gamma_{K^+,w} d\mu_{KF} - \Gamma_{Br^-,w} d\mu_{KBr}$$

If neutral molecules were present, terms such as $-\Gamma_{N,w} d\mu_N$ must be added. The procedure could also be extended to include amalgam electrodes.

In interpreting a system we are actually interested in the quantities Γ^{OHP} , Γ^d , Γ^i . Γ^{OHP} is the surface excesses calculated at the outer Helmholtz plane. Γ^d is that part of the surface excess

which is in the diffuse layer. Γ^i is the surface concentration of specifically adsorbed ions. As will be further discussed, compelling evidence indicates that KF is not specifically adsorbed, but is present only in the diffuse layer. $\Gamma_{K^+}^{OHP}$ and $\Gamma_{K^+}^d$ are equal and can be used to evaluate diffuse layer parameters. To use this approach one must assume that $\Gamma_{F^-,w} = \Gamma_{F^-}^{OHP}$ which is equivalent to $\frac{x_{KF}}{x_{H_2O}} \Gamma_{H_2O}$ being negligible. The same situation arises in determining Γ^i . This approximation is only valid at low concentrations (1M and below).³

As was mentioned earlier, the use of a reversible electrode is not necessary. If a reference electrode, for example a calomel electrode, is used instead, the potential can be written:

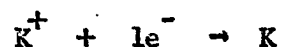
$$E_{ref} = E_{Hg} - E_{cal}$$

$$E^+ = E_{Hg} - E_{In}$$

therefore

$$E_{ref} = E^+ + E_{In} - E_{cal}$$

For a K^+ reversible half cell E_{In}



$$E_{In} = E^0 + \frac{RT}{F} \ln a_{K^+}$$

therefore

$$E_{ref} = E^+ + \frac{RT}{F} \ln a_{K^+} + \text{constant}$$

In evaluating data, only dE^+ is used. If an experiment is run in which a_{K^+} varies, one simply calculates E^+ from the above equation. The

only questionable but necessary practice is using a_{\pm} for a_K^+ .

The general form for any system will be $dy = -qdE - \Gamma_{x,w} d\mu_{MX} - \Gamma_{N,w} d\mu_N$ where MX is a salt and N a neutral molecule. The second derivative of γ , C

$$C = \left(\frac{\partial q}{\partial E} \right)_{\mu} = - \left(\frac{\partial^2 \gamma}{\partial E^2} \right)_{\mu}$$

is an experimentally available quantity known as the differential capacity. If C is measured as a function of E at constant μ , the integration of the $C - E$ curves will give γ and q . Two integration constants are needed and can be obtained either directly or from the base solution values in a region where there is no specific absorption. The directly available constants are E_z , the potential at which $q = 0$, which is obtained by use of the streaming electrode and γ at E_z which is obtained by using the capillary electrometer. It then follows that

$$q = \int_{E_z}^E C dE$$

$$\gamma - \gamma(E_z) = - \int_{E_z}^E \int_{E_z}^E C dE dE$$

If alternatively, the curves of C versus E are identical in a given region for two solutions of the same ionic strength in neither of which specific absorption occurs in that region, the values of C , q , E , and γ at a point in this region for one solution may be used to integrate the other solution. To check this procedure, one compares the back integrated value of E_z to the streaming electrode value.

Let us assume that the curve has been integrated such that values of γ and E are known at integral values of q . We now define the function of $\xi = \gamma + qE$ which is a Legendre transformation of γ .

$$d\xi = Edq - \Gamma d\mu$$

If values of ξ at constant q are differentiated with respect to μ , Γ is obtained. Γ could also be found from the derivative of γ by μ at constant E . The choice depends on whether you wish to further evaluate your data at constant q or constant E . The surface charge density q is directly related to the field in the interface. The potential difference across the cell E is a more complicated quantity. The choice of constant q is both intuitively satisfactory and leads to a somewhat easier analysis. Theoretical and experimental attempts to resolve this problem have been inconclusive.^{4,5}

B. The Gouy-Chapman-Stern Theory of the Diffuse Double Layer

The G.C.S. theory deals only with the diffuse layer. We assume that the closest approach of an ion to the mercury surface is the outer Helmholtz plane, X_2 . One assumes that the concentration at a distance X from the electrode surface is given by

$$C_i(X) = C_i^b \exp\left(-\frac{Z_i F \phi(X)}{RT}\right)$$

where Z_i is the charge, $\phi(X)$ the potential at X , and C_i^b the bulk concentration. In the equations below $\rho(X)$ is the charge density, \vec{D} the displacement vector and \vec{E} the electric field vector. It then follows from standard electromagnetic theory that

$$\nabla \cdot \vec{D} = \rho$$

$$\vec{D} = \epsilon \vec{E} = -\epsilon \nabla \phi$$

$$\nabla \cdot \epsilon \nabla \phi = -\rho(X)$$

$$\nabla^2 \phi = -\frac{\rho(X)}{\epsilon}$$

or

$$\frac{d^2 \phi(X)}{dX^2} = -\frac{1}{\epsilon} \sum_i z_i F C_i^b \exp\left(-\frac{z_i F \phi(X)}{RT}\right)$$

if ϕ is a function of X only and ϵ is a constant. We now multiply both sides by $2 \frac{d\phi(X)}{dX}$.

$$2 \frac{d\phi}{dX} \frac{d^2 \phi}{dX^2} = \frac{d}{dX} \left(\frac{d\phi}{dX} \right)^2 = -\frac{2}{\epsilon} \sum_i z_i F C_i^b \frac{d\phi}{dX} \exp\left(\frac{-z_i F \phi(X)}{RT}\right)$$

We now integrate and get the constant of integration from the fact that $\frac{d\phi(X)}{dX}$ goes to zero as X goes to infinity.

$$\left(\frac{d\phi}{dX} \right)^2 = \left(\frac{2RT}{\epsilon} \right) \sum_i C_i^b \left[\exp\left(\frac{-z_i F \phi}{RT} - 1\right) \right]$$

$$\vec{E} = -\frac{d\phi}{dX} \hat{i} = \pm \left(\frac{2RT}{\epsilon} \right)^{\frac{1}{2}} \left(\sum_i C_i^b \left[\exp - \frac{z_i F \phi}{RT} - 1 \right] \right)^{\frac{1}{2}} \hat{i}$$

Let X_2 be the position of the outer Helmholtz plane.

$$E(X_2) = -\left. \frac{d\phi(X)}{dX} \right|_{X=X_2}$$

and

$$D(X_2) = q^M + q^l$$

where q^M is the charge density on the metal and q^1 is the charge density of the specifically absorbed species. Therefore

$$q^M + q^1 = \pm (2RT\epsilon)^{\frac{1}{2}} \left(\sum C_i^b \left[\exp - \frac{z_i F \phi}{RT} - 1 \right] \right)^{\frac{1}{2}}$$

For a 1-1 electrolyte or for a mixture of 1-1 electrolytes with one ion in common at constant ionic strength.

$$q^M + q^1 = (8RT\epsilon C^b)^{\frac{1}{2}} \sinh \frac{|z| F \phi^2}{2RT}$$

Since q^M and q^1 are experimentally available, the capacity due to the diffuse layer is easily found.

$$C^d = \frac{\partial \phi^2}{\partial (q^M + q^1)} = \left(\frac{2|z| F^2 \epsilon C^b}{RT} \right)^{\frac{1}{2}} \cosh \left(\frac{F \phi^2}{2RT} \right)$$

also

$$\phi^2 = \frac{2RT}{|z| F} \ln \left\{ \left(\frac{q^M + q^1}{2A} \right) + \left[\left(\frac{q^M + q^1}{2A} \right)^2 + 1 \right]^{\frac{1}{2}} \right\}$$

where $A = (2RT\epsilon C^b)^{1/2}$ and ϕ^2 is the potential at the outer Helmholtz plane. The surface excess due to the diffuse layer which is equivalent to the surface excess with the Gibbs surface at the outer Helmholtz plane is given by

$$\Gamma_i^d = C_i^b \int_{X_2}^{\infty} \left[\exp \left(- \frac{z_i F \phi(X)}{RT} \right) - 1 \right] dx$$

and for a 1-1 electrolyte

$$\Gamma_+^d = \frac{A}{|z| F} \left(\exp \left(- \frac{|z| F \phi^2}{2RT} \right) - 1 \right)$$

$$\Gamma_-^d = \frac{A}{|z| F} \left(\exp \left(\frac{|z| F \phi^2}{2RT} \right) - 1 \right)$$

$$q_+^d = |z| F \Gamma_+^d \quad \text{and} \quad q_-^d = |z| F \Gamma_-^d$$

The general approach when dealing with absorption from a single salt solution is to find $\Gamma_{+,w}$ from $\left(\frac{\partial \xi}{\partial \mu}\right)_q$. Unless the cation is one of the few which is absorbed, q_+ can be completely assigned to the diffuse layer. Using the equation for q_+ , one finds ϕ^2 and from it q_-^d . The amount of specifically adsorbed anion q_-^1 then follows from

$$q^M = -q^S = -(q_-^1 + q_-^d + q_+^d)$$

It has already been pointed out that at high concentrations an error can result from equating $\Gamma_{+,w}$ to Γ_+^{OHP} . Another source of error arises when there is weak specific adsorption. At positive surface charges Γ_+ has the limiting value of $-A$, but ϕ^2 goes to infinity. It follows that a small error in $\Gamma_{+,w}$ when $\Gamma_{+,w} \approx -A$ will cause a large error in ϕ^2 . This makes the calculation of q_-^d and q_-^1 suspect when $\Gamma_{+,w}$ is near $-A$.⁶

C. The Components of the Capacity

1. No specific absorption

The potential drop across the cell with or without specific absorption may be written

$$E = (\phi^M - \phi^2) + \phi^2 - \phi^{\text{ref}}$$

In the absence of specific adsorption, ϕ^2 is a function of q only at constant μ . Therefore

$$\left(\frac{\partial E}{\partial q}\right)_\mu = \left(\frac{\partial(\phi^M - \phi^2)}{\partial q}\right)_\mu + \left(\frac{\partial \phi^2}{\partial q}\right)_\mu$$

or

$$\frac{1}{C} = \frac{1}{C^i} + \frac{1}{C^d}$$

C^i , which is the capacity of the inner layer, may be obtained from measured values of C and computed values of C^d . With fluoride salts of unadsorbed cations C^i , Figure 2, is a function of charge only. The total capacity measured for any concentration, and that calculated using C^i values measured at another concentration and computed C^d values are in agreement.⁷ Furthermore, plots of $\frac{1}{C}$ versus $\frac{1}{C^d}$ at constant q are linear. This affords strong support for the validity of G.C.S. theory and the assumption that fluoride ions are not adsorbed. No theory at present can satisfactorily predict the dependence of C^i on q even in the simplest case of fluoride salts. One point of particular controversy is the anodic peak in the C^i curve which is most evident with specific adsorption. In 1MKF at 25°C it is almost a plateau.⁸ These peaks have been ascribed to specific adsorption peaks and to the reorientation of the solvent layer. The anodic rise which follows the peak has been associated with electrostriction and with specific adsorption. The situation is at present unresolved.

Another support for our assumption of no fluoride ion specific adsorption comes from the Esin-Markov effect. We begin with the function ξ .

$$d\xi = E^+ dq - \Gamma_{F^-,w} d\mu_{KF}$$

$$\left(\frac{\partial E^+}{\partial \mu}\right)_q = - \left(\frac{\partial \Gamma_{F^-,w}}{\partial q}\right)_\mu$$

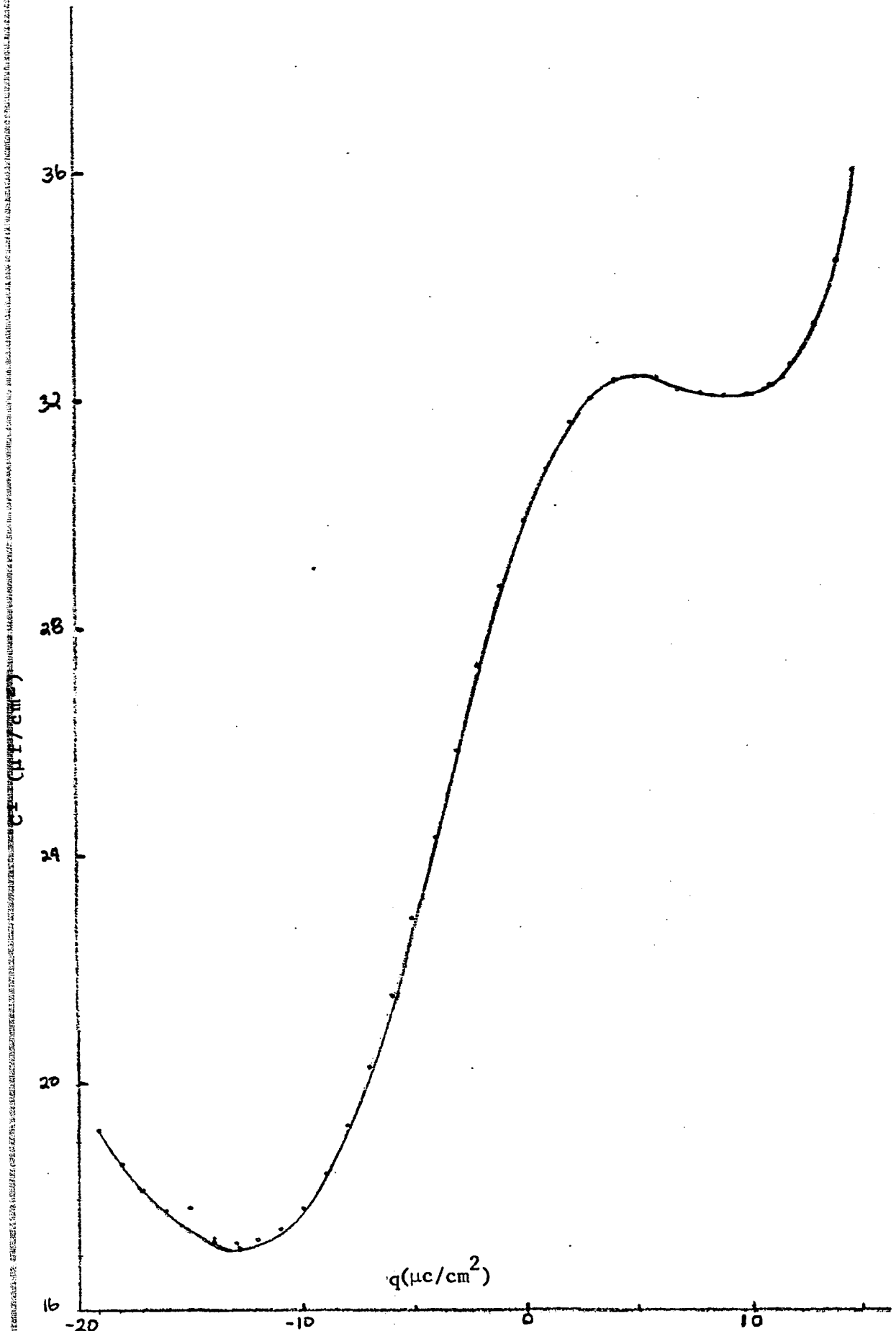


Figure 2. The Inner Layer Capacity of LMKF Plotted as a Function of the Surface Charge Density

for a cation reversible electrode

$$E^+ = E_{\text{ref}} - \frac{RT}{2F} \ln a_{\pm}^2$$

and

$$q_{F^-} = -F\Gamma_{F^-}, w$$

therefore

$$\left(\frac{\partial E_{\text{ref}}}{\partial \ln a_{\pm}^2} \right)_q = \frac{RT}{F} \left[\left(\frac{\partial q_-}{\partial q} \right)_\mu + \frac{1}{2} \right]$$

where we have assumed that $q_{F^-} = q_-^d$.

Also

$$q_-^d = -A \left(\exp\left(\frac{RT\phi^2}{2F}\right) - 1 \right)$$

$$\phi^2 = \frac{2RT}{F} \sinh^{-1} q/2A$$

therefore

$$\left(\frac{\partial q_-^d}{\partial q} \right)_\mu = -\frac{1}{2} - \frac{1}{2} \left\{ \frac{q/2A}{[1 + (q/2A)^2]^{1/2}} \right\}$$

For $q = 0$, we find that

$$\left(\frac{\partial E_{\text{ref}}}{\partial \ln a_{\pm}^2} \right)_q$$

should equal zero. In other words E_z measured against a reference electrode is independent of concentration. Parsons found this to be the case with NaF solutions. Furthermore, he compared the experimental and theoretical values of $\left(\frac{\partial E_{\text{ref}}}{\partial \ln a_{\pm}^2} \right)_q$ at different values of q and also found agreement.⁹

2. Specific adsorption present

In the presence of specific adsorption we may still write^{10,11}

$$E = \phi^{m-2} + \phi^2 - \phi^{\text{ref}}$$

where ϕ^{m-2} is the potential drop across the inner layer.

Also

$$\left(\frac{\partial E}{\partial q}\right)_{\mu} = \left(\frac{\partial \phi^{m-2}}{\partial q}\right)_{\mu} + \left(\frac{\partial \phi^2}{\partial q}\right)_{\mu}$$

but ϕ^2 is now a function of both q and q^1

therefore

$$\left(\frac{\partial \phi^2}{\partial q}\right)_{\mu} = \left(\frac{\partial \phi^2}{\partial q^d}\right)_{\mu} \left(\frac{\partial q^d}{\partial q}\right)_{\mu}$$

$$q = -q^1 - q^d$$

$$\left(\frac{\partial \phi^2}{\partial q}\right)_{\mu} = \frac{1}{C^d} \left[1 + \left(\frac{\partial q^1}{\partial q}\right)_{\mu} \right]$$

so that

$$\frac{1}{C} = \frac{1}{C^i} + \frac{1}{C^d} \left[1 + \left(\frac{\partial q^1}{\partial q}\right)_{\mu} \right]$$

C , C^d , and $\left(\frac{\partial q^1}{\partial q}\right)_{\mu}$ are known, which allows the computation of C^i .

ϕ^{m-2} may be expressed as

$$\phi^{m-2} = E - \phi^2 - Ez$$

where Ez is the potential at point of zero charge for KF in the same cell. This is essentially a method of putting all of the systems on

the same scale independent of the experimental design. ϕ^{m-2} may be considered a function of q and q^1 . Therefore

$$d\phi^{m-2} = \left(\frac{\partial \phi^{m-2}}{\partial q} \right)_q dq + \left(\frac{\partial \phi^{m-2}}{\partial q^1} \right)_q dq^1$$

$$\frac{1}{C^i} = \left(\frac{\partial \phi^{m-2}}{\partial q} \right)_q = \left(\frac{\partial \phi^{m-2}}{\partial q} \right)_q + \left(\frac{\partial \phi^{m-2}}{\partial q^1} \right)_q \left(\frac{\partial q^1}{\partial q} \right)_q$$

or

$$\frac{1}{C^i} = \frac{1}{q C^i} + \frac{1}{q^1 C^i} \left(\frac{\partial q^1}{\partial q} \right)_q$$

$$q C^i = \left(\frac{\partial q}{\partial \phi^{m-2}} \right)_q \quad q^1 C^i = \left(\frac{\partial q^1}{\partial \phi^{m-2}} \right)_q$$

$q C^i$ and $q^1 C^i$ both have the dimensions of capacity. $q^1 C^i$ can be obtained from the slope of a plot of ϕ^{m-2} versus q^1 at constant q .

Two other integral capacities can be obtained from this plot.

$$q^1 K^i = \frac{\Delta q^1}{\Delta \phi^{m-2}} \quad \text{at constant } q$$

$$q K^i = \frac{\Delta q}{\Delta \phi^{m-2}} \quad \text{at constant } q^1$$

$q^1 K^i$ will equal $q^1 C^i$ if the plots are linear. $q K^i$ is equal to the difference Δq between a q and $q = 0$ curve divided by $\Delta \phi^{m-2}$ for the same value of q^1 . For $q = 0$, $q K^i = q C^i$. $q C^i$ is obtained by solving the equation for $1/C^i$. $q K^i$ and $q^1 K^i$ have both been interpreted as the capacities of two parallel plate capacitors.

$${}_q K^i = \frac{\epsilon}{4\pi X_2} = \frac{q}{q \phi^{m-2}}$$

$${}_q 1 K^i = \frac{\epsilon}{4\pi(X_2 - X_1)} = \frac{q^1}{q^1 \phi^{m-2}}$$

where X_1 is the position of the inner Helmholtz layer, ${}_q \phi^{m-2}$ is the part of ϕ^{m-2} due to the surface charges and ${}_q 1 \phi^{m-2}$ is the part of ϕ^{m-2} due to the absorbed charges. The ratio

$$\frac{{}_q K^i}{{}_q 1 K^i} = \frac{X_2 - X_1}{X_2}$$

is known as the distance ratio. If the field in the inner layer is constant then we may write

$$\begin{aligned} \phi_1 &= \phi^m - \sigma X \\ \phi_2 &= \phi^m - \sigma X_1 \\ \phi &= \phi^m - \sigma X_2 \\ \phi^{m-2} &= \phi^m - \phi^2 = \sigma X_2 \end{aligned}$$

where ϕ^1 is the potential at the inner Helmholtz plane. A latter modification of this equation is

$$\phi^1 - \phi^2 = [(X_2 - X_1)/X_2] {}_q \phi^{m-2} + \left[\frac{\gamma}{\gamma + \beta} \right] {}_q 1 \phi^{m-2}$$

$\gamma/\gamma + \beta$ will approach unity when q^1 is large and most of the potential drop across the inner layer occurs between the inner and outer Helmholtz planes. At low values of q^1 ,

$$\frac{y}{y+\beta} = \frac{x_2 - x_1}{x_2}$$

in order that

$$\phi^1 - \phi^2 = \frac{x_2 - x_1}{x_2} \phi^{m-2}$$

An adsorption isotherm may be used to obtain the value of $\frac{x_2 - x_1}{x_2}$.

For example, for KI + KCl, Parsons assumed the following:¹²

$$q^1 = K^1 a_{\pm} \exp(\phi^1 F/RT)$$

where $q^1 = |q^1|$ and K^1 is a function of q only. Then

$$\ln q^1/a_{\pm} - \frac{\phi^2 F}{RT} = \ln K^1 + \frac{\phi^{m-2} F}{RT} \left(\frac{x_2 - x_1}{x_2} \right)$$

If we plot ϕ^{m-2} versus the left side of the equation, the slope gives the distance ratio. More complicated isotherms and the modified expression for $\phi^1 - \phi^2$ can also be used. The capacity ratio method was used for a number of systems, but recently situations where $q^1 K^1$ is negative were found.^{13,14} Since x_2 must be greater than x_1 , the interpretation cannot be meaningful for these systems. The earlier success was fortuitous since the physical situation in the inner layer does not correspond to two capacitors in series. The above equations are based on the assumption that

$$\phi^{m-2} = q \phi^{m-2} + q^1 \phi^{m-2}$$

or

$$\phi^{m-2} = \frac{q}{q^1 K^1} + \frac{q^1}{q^1 K^1}$$

This is not the equation for two capacitors in series or in parallel and its physical meaning is obscure. Values of the distance ratio determined by the isotherm method and those determined by the capacity ratio method have generally not been in agreement.

C_q^i is theoretically an experimentally determinable quantity. We return to the equation

$$\frac{1}{C^i} = \frac{1}{C_q^i} + \frac{1}{C_1^i} \left(\frac{\partial q^1}{\partial q} \right)$$

At infinite frequency, the second term is zero and we are measuring C_q^i . This assumes that diffuse layer theory is still valid at infinite frequency. C_q^i is of particular importance in explaining the peaks in C^i versus charge curves. If the peak is due solely to specific adsorption, then C_1^i which is measured at constant q^1 should not contribute to it. The fact that there are peaks in C^i suggests that solvent reorientation plays a part in peak formation.

D. Adsorption Isotherms and the Shape of the Capacity Curve.

Theoretically, the shape of the capacity versus charge curve can, under certain conditions, be directly predicted from the adsorption isotherm.^{15,16,17} The determination of the isotherm also provides information on the charge or potential dependence of the free energy of adsorption. The constants of the isotherm give information concerning the interaction of adsorbed ions. The two isotherms which are most frequently used are the Frumkin and virial. The isotherms and equations of state are given below.

Frumkin:

$$\text{isotherm} \quad \ln \frac{a\beta}{\Gamma_S} = \ln \frac{\theta}{1-\theta} + A\theta$$

$$\text{equation of state} \quad \frac{\bar{\phi}}{kT\Gamma_S} = -\ln(1-\theta) + \frac{A}{2}\theta^2$$

Virial:

$$\text{isotherm} \quad \ln \Gamma + 2B\Gamma = \ln a\beta$$

$$\text{equation of state} \quad \bar{\phi} = kT(\Gamma + B\Gamma^2)$$

$\bar{\phi}$ is the surface pressure and for constant q , $\bar{\phi} = \xi - \xi^b$ where ξ is the base solution value of ξ . β equals $\exp(-\Delta G/R\Gamma)$, Γ_S is the saturation concentration, a the activity, $\theta = \Gamma/\Gamma_S$, and A and B are isotherm constants. The problem of whether to study adsorption at constant q or E arises again at this point. As previously mentioned, it is unresolved.

The method of testing the Frumkin isotherm is to pick a value of A , allow θ to vary from $0 < \theta < 1$ and get a universal curve of $\ln(\bar{\phi}/kT\Gamma_S)$ versus $\ln(a\beta/\Gamma_S)$. This curve is compared with an experimental curve of $\ln \bar{\phi}$ versus $\ln a$. If the data fit a Frumkin isotherm, the two curves are superimposable if the scale of $\ln \bar{\phi}$ and $\ln a$ are changed to $\ln \bar{\phi} + C_1$ and $\ln a + C_2$. Obviously $C_1 = -\ln kT\Gamma_S$ and $C_2 = \ln \beta/\Gamma_S$. The values of A and Γ_S can be adjusted to get the best fit of the experimental data. The virial isotherm is much easier to handle. One rearranges the isotherm into the form

$$\Gamma = \frac{1}{2B} \ln \frac{a}{\Gamma} + \frac{1}{2B} \ln \beta$$

The experimental values of Γ are plotted against $\ln a/\Gamma$ and the slope gives $\frac{1}{2\beta}$, the intercept in β . The method used for the Frumkin isotherm can be used for any isotherm where $K\bar{\phi}$, K a constant, and β are functions only of θ and any number of isotherm constants. In studying the adsorption of a single ion, the question arises whether to use the salt activity (a_{\pm}^2) or the ion activity a_{\pm} in the isotherm. It seems logical to use a_{\pm} , but this question is also unresolved.

The assumption which is necessary in order to relate the isotherm to the capacity curves is that $\Gamma = \Gamma(\beta a)$. This means that all isotherm constants are independent of the surface charge and the amount of specific adsorption. We begin with the differential form of ξ .

$$d\xi = E dq - \Gamma d\mu$$

$$\left(\frac{\partial E}{\partial \mu}\right)_q = -\left(\frac{\partial \Gamma}{\partial q}\right)_\mu$$

$$dE = -\int \left(\frac{\partial \Gamma}{\partial q}\right)_\mu d\mu \quad q = \text{constant}$$

but since

$$\Gamma = \Gamma(\beta a)$$

$$\frac{1}{\beta} \left(\frac{\partial \Gamma}{\partial a}\right)_\beta = \frac{1}{a} \left(\frac{\partial \Gamma}{\partial \beta}\right)_a$$

and

$$\left(\frac{\partial \Gamma}{\partial q}\right)_\mu = \left(\frac{\partial \Gamma}{\partial \beta}\right)_\mu \left(\frac{\partial \beta}{\partial q}\right)_\mu$$

therefore

$$dE = -\int \frac{a}{\beta} \left(\frac{\partial \Gamma}{\partial a}\right)_\beta \frac{\partial \beta}{\partial q} d\mu$$

and

$$\Delta E = E - E^b = - RT \left(\frac{\partial \ln \beta}{\partial q} \right) \Gamma \quad \text{at constant } q$$

E^b is the value of E for the base solution at the same value of q . If $\ln \beta$ is linear in q , then plots of $E - E^b$ versus $\ln a$ should be part of the same curve if $\ln \beta$ is added to $\ln a$. The isotherm and $\frac{d \ln \beta}{dq}$ can be obtained directly from this type of plot.

More generally, we can now take the derivative of the equation for ΔE by q at constant μ .

$$\left(\frac{\partial E}{\partial q} \right)_{\mu} - \left(\frac{\partial E^b}{\partial q} \right)_{\mu} = - kT \frac{\partial}{\partial q} \left[\frac{\partial \ln \beta}{\partial q} \cdot \Gamma \right]$$

or

$$\frac{1}{C} - \frac{1}{C^b} = - kT \left[\left(\frac{\partial \ln \beta}{\partial q} \right)^2 \left(\frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu} + \Gamma \frac{\partial^2 \ln \beta}{\partial q^2} \right]$$

at any given value of q . Let us first assume that

$$\frac{d \ln \beta}{dq} = K$$

$$\frac{d^2 \ln \beta}{dq^2} = 0$$

Then

$$\Delta \frac{1}{C} = \frac{1}{C} - \frac{1}{C^b} = - kTK^2 \left(\frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu}$$

$\left(\frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu}$ is obtained from the isotherm. For a Frumkin isotherm

$$\frac{\partial \Gamma}{\partial \ln \beta} = \Gamma_S \left\{ \frac{1}{\theta(1-\theta)} + A \right\}^{-1}$$

and is symmetrical about $\theta = .5$ where it is a maximum. A plot of $-\frac{1}{\Delta C}$ versus Γ at constant charge should give a maximum at $\theta = .5$. When $-\frac{1}{\Delta C}$ is a maximum C is also a maximum. Alternatively let us assume that a virial isotherm is obeyed.

$$\frac{1}{C} - \frac{1}{C^b} = -kTK^2 \left(\frac{\Gamma}{1+2B\Gamma} \right)$$

For large values of Γ , $-\frac{1}{\Delta C}$ reaches the limiting value of $\frac{kTK^2}{2B}$ and this would be evident in plots of $-\frac{1}{\Delta C}$ versus Γ at constant q . Plots of $-\frac{1}{\Delta C}$ versus q at constant μ will have the same characteristics if $\frac{d^2 \ln \beta}{dq^2} = 0$.

If we assume that $\ln \beta$ is a quadratic function of q , we may write it as follows

$$\ln \beta = \ln \beta_{\max} - \frac{b}{2} \delta^2$$

where

$$\delta = q - q_{\max}$$

also

$$\frac{d \ln \beta}{dq} = -b\delta$$

$$\frac{d^2 \ln \beta}{dq^2} = -b$$

A quadratic standard free energy is based on the assumption that ΔG is given by:

$$\Delta G = \Delta G^0 + \frac{1}{2} q^2 \left[\frac{1}{C^S} - \frac{1}{C^b} \right] + q \left[\frac{\mu^b}{e^b} - \frac{\mu^S}{e^S} \right]$$

μ^S , C^S and ϵ^S are the dipole moment per unit volume, the capacity per unit area and the dielectric constant when the surface is saturated with adsorbate; μ^b , C^b , and ϵ^b are for the base solution. ΔG^0 is the non-electrical part of ΔG . This equation may be rearranged to the form

$$\Delta G = \Delta G_{\max} + \frac{1}{2} b^1 \delta^2$$

by finding ΔG_{\max} from the derivative $\partial \Delta G / \partial q$ when it equals zero. ΔG and ΔG_{\max} are negative, b^1 is positive. Since $\beta = \exp(-\Delta G/RT)$

$$\ln \beta = \ln \beta_{\max} - \frac{1}{2} b^1 \delta^2$$

We then have for $\Delta 1/C$ the following equation.

$$\Delta \frac{1}{C} = kT \left[\Gamma b - b^2 \delta^2 \left(\frac{\partial \Gamma}{\partial \ln \beta} \right)_{\mu} \right]$$

If we take the derivative of $\Delta \frac{1}{C}$ by δ at constant μ and set it equal to zero, we find the values at which $\Delta \frac{1}{C}$ is an extreme. This expression is

$$b \delta^2 = \frac{3(\partial \Gamma / \partial \ln \beta)_{\mu}}{(\partial^2 \Gamma / \partial \ln \beta^2)_{\mu}}$$

There are three values of δ which satisfy this equation. One is $\delta = 0$, independent of the isotherm chosen. This point corresponds to maximum adsorption since $\ln \beta$ is a maximum at $\delta = 0$. $\Delta \frac{1}{C}$ will be a maximum and C will have its minimum value. The other two values of δ correspond to maxima in C and minima in $\Delta \frac{1}{C}$. They depend on the particular isotherm obeyed. As δ goes to plus or minus infinity, $\Delta \frac{1}{C}$ goes to

zero for any isotherm. C is then equal to C^b and there is complete desorption. Quadratic dependence is easily demonstrated by a plot of $\Delta \frac{1}{C}$ versus q at constant μ . Plots of $\Delta \frac{1}{C}$ versus Γ at constant q may be used as an alternative method of finding q_{\max} . The curve for $q = q_{\max}$ should be linear and have the largest slope which will equal kTb .

This analysis has been used to explain the shape of capacity curves with adsorption. It is truly rigorous only for the adsorption of neutral molecules. With ionic adsorption one must decide whether to use $\Delta \frac{1}{C}$ or $\Delta \frac{1}{C^i}$. The derivation necessitates the use of $\Delta \frac{1}{C}$, but unlike neutral adsorption the value of C^d for the base solution will not be the same as that for the solution with adsorption. Using $\Delta \frac{1}{C^i}$ solves this problem and is intuitively appealing, but without rigorous justification. Another problem arises with adsorption from a single salt solution, what do we use for the base solution values of C^b ? The values used in the literature are the C values for KF at the same concentration. Actually, the derivation indicates that the base solution is the solvent, and that the use of KF values needs further justification. These problems can be alleviated by working with a mixed electrolyte system at constant ionic strength such as $xM\text{KBr} + (1-x)M\text{KF}$. C^d is then always large and makes a minor contribution to C . Equating the base solution to $1M$ KF is also justified in this type of system.

With single salt adsorption, the use of the surface pressure also becomes ambiguous.^{11,18} We begin with

$$d\xi^+ = Edq - (\Gamma_{\text{Br}^-}^d + \Gamma_{\text{Br}^-}^i) d\mu_{\text{KBr}}$$

We then assume that the surface pressure can be written as

$$\bar{\phi} = \xi^+ + I - \xi_0^+$$

where

$$I = \int_{-\infty}^{\mu} \Gamma_{Br}^d - d\mu_{KBr}$$

and ξ_0^+ is the value of ξ when $\mu = -\infty$ or

$$\bar{\phi}' = \xi^+ + I$$

$$I' = \int_{\mu_1}^{\mu_2} \Gamma_{Br}^d - d\mu_{KBr}$$

The magnitude of $\bar{\phi}'$ will differ from $\bar{\phi}$ by a constant at constant q . A significant problem in this approach is whether the surface pressure due to the anion is $\bar{\phi}$ or $\bar{\phi}/2$. It is essentially the same problem of whether to use a_{\pm} or a_{\pm}^2 in the isotherm.¹⁹ Using $\bar{\phi}$ implies that all of the effect is due to the anion, whereas $\bar{\phi}/2$ implies that only half of the change is caused by the anion. Since the cation is also adsorbed, though not specifically, it must also have an effect on the surface pressure. A more basic difficulty, is whether the entire concept is valid in single salt solutions with varying ionic strength. This again reduces to the identification of the base solution. With organic adsorption, or adsorption from a solution of fixed ionic strength, this problem does not exist. Let us assume we have system governed by the equation:

$$d\xi = Edq - \Gamma_{N,w} d\mu_N - \Gamma_{F,w} d\mu_{KF}$$

$$d\mu_{KF} = 0$$

Then the surface pressure is given by

$$\xi = \xi - \xi_0$$

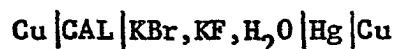
where ξ_0 is the value of the KF solution in the absence of N and there is no ambiguity.

II. EXPERIMENTAL PROCEDURE

Three separate experiments are needed in order to obtain the data required to interpret the structure of the electrical double layer. These are the determination of the potential (E_z), and the interfacial tension (γ_{Ez}) at the point of zero charge ($q = 0$), and the determination of the differential capacity curve for each concentration of adsorbate studied. The potential and interfacial tension at the point of zero charge are the two constants needed to integrate the differential capacity curve.

A. The Determination of E_z

Let us assume that we have the following cell:



CAL is a calomel reference electrode. A potentiometer is connected between the two copper leads. The mercury electrode consists of a capillary with its top in the solution connected to a mercury reservoir. The reservoir is in turn connected to a tank of nitrogen so that the pressure in the reservoir may be varied at will. The pressure on the mercury is then increased until a rate of flow is reached at which a stable potential exists between the reservoir and the calomel electrode. The pressure is then varied and the potential recorded as a function of pressure. As the pressure increases, the potential will become more negative, reach a plateau and then increase slightly. The potential in the plateau region is the potential of zero charge. The concept behind this experiment is that once an adequate rate of flow is reached, any excess charge on the mercury

will be carried off and furthermore the area of the electrode is effectively infinite. Therefore the surface charge density is zero. The slight rise in potential which occurs at large pressures was unexpected and remains unexplained. It has been observed in a sufficient number of systems that the nature of the adsorbate cannot be the cause. Grahame did an extensive amount of work on the determination of E_z , and found that this is the most reliable method.²⁰ E_z is reproducible to 1 mv or less and even this variation could be due to variations in the liquid junction potential. This method assumes that equilibrium has been reached at the electrode surface. If this is not the case, E_z must be determined by finding the maximum in the electrocapillary curve.

B. The Determination of γ_{Ez}

The capillary electrometer and its use for determining the electrocapillary curve were developed by Gouy early in this century. The same cell used to determine E_z , is used in this experiment, except that a much finer capillary is needed. A potential is applied across the cell. The capillary is connected to a mercury reservoir which can be varied in height above the capillary tip. The criterion for choosing a capillary is that it be able to support a column of mercury at least 60 cm high when E_z is the applied potential. The capillary is calibrated by using a solution whose electrocapillary curve is known. We apply a potential and measure the position of the mercury meniscus in the capillary. At the interface,

$$\Delta P = \frac{2\gamma}{r}$$

ΔP is computed from the height of the mercury and corrected for the solution height above the tip. Since γ is known, the radius of the capillary at a fixed position is also known. We now may use the capillary for any other solution. At each value of the imposed potential, the mercury reservoir is adjusted until the meniscus is at the calibrated position. We then compute γ using the known value of the radius. There are several possible sources of error in this experiment. We assume that the contact angle between the solution and the mercury is zero, and that we may accurately return the meniscus to the calibrated position. We have no choice concerning the contact angle since it cannot be measured, but the agreement of E_z values obtained from the electrocapillary curve and those obtained from the streaming electrode supports the zero contact angle assumption. The other problem depends on the capillary. If the radius is changing rapidly, then large errors will be made in positioning the meniscus, but if the radius changes too slowly, a definite equilibrium position is not easily achieved. If the results are reproducible, one may assume the taper of the capillary curve is correct. The potential at which the electrocapillary curve is a maximum is E_z . Unfortunately, the curve is quite flat in this region. This allows an accurate measurement of γ_{E_z} , but a poor measurement of E_z . The best procedure is to obtain E_z from the streaming electrode and γ_{E_z} from the electrocapillary curve.

C. The Differential Capacity Curve

The procedure for measuring the differential capacity was first developed by Grahame and improved by Hills and Payne.²¹ A schematic of the apparatus is shown in Figure 3. The cell consists of three

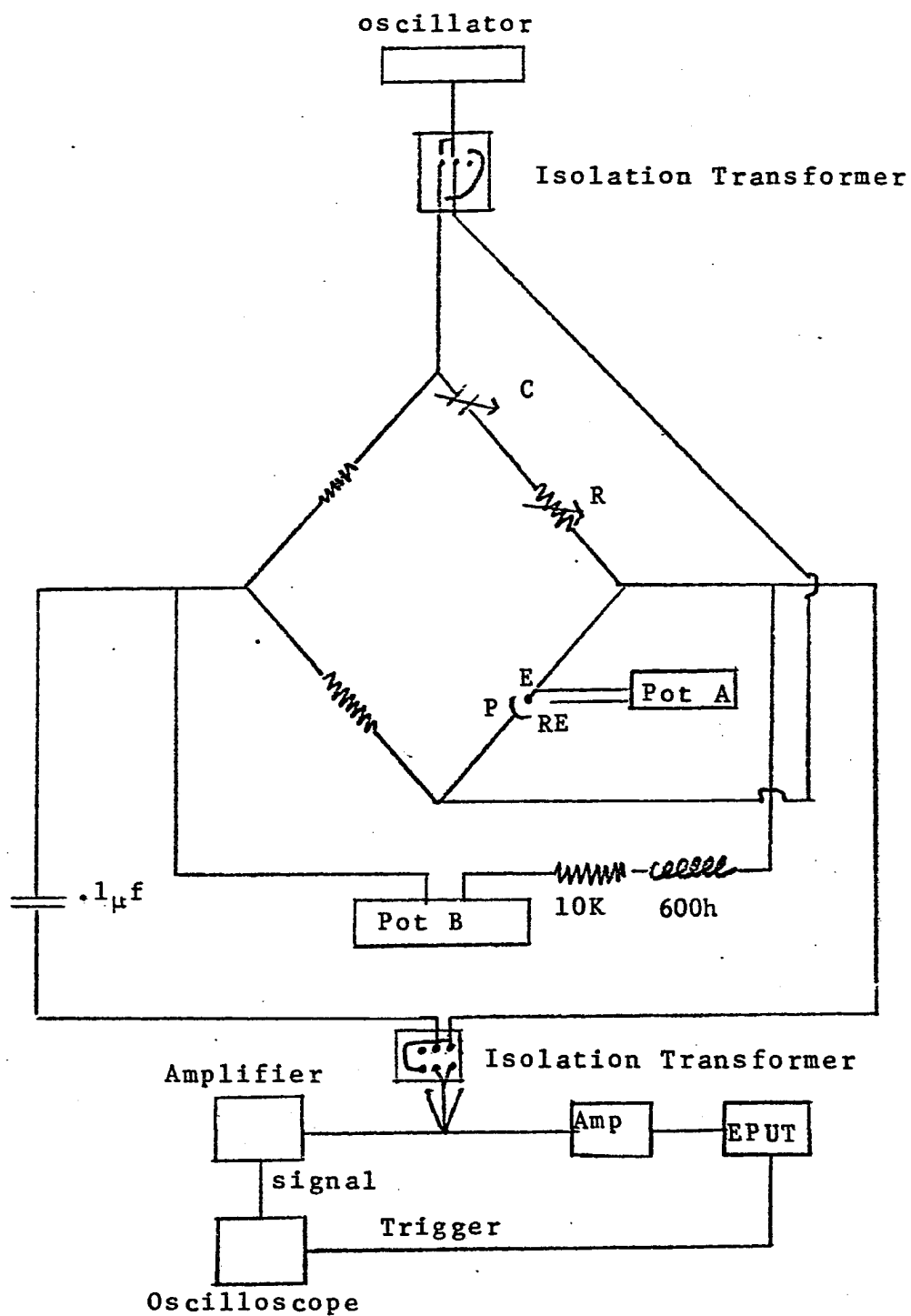


Figure 3. A Schematic Representation of the Apparatus Used to Determine The Differential Capacity

electrodes. A dropping mercury electrode (E) is attached to one terminal of the bridge. Its tip is inside a platinum mesh basket (P) which is attached to another terminal. Together they form one of the four bridge arms. The third electrode is a reference electrode (RE) which is separated by two stopcocks from the solution being measured. The closed stopcocks are ungreased allowing electrical contact but preventing the diffusion of chloride ions from the reference electrode into the solution. Potentiometer A measures the potential between the dropping electrode and the reference electrode. Potentiometer B imposes a constant potential across the entire bridge. The only direct current which flows is that to charge the capacitors. An alternating voltage of 10 mv is impressed across the bridge and the bridge output fed into two amplifiers. The first amplifier feeds the signal to the vertical plates of an oscilloscope. The second amplifier takes the signal to a modified Beckman EPUT meter. The maximum output of the bridge occurs when a drop falls off. At this point the bridge is completely out of balance. The EPUT meter has been modified in such a way that in the TIM mode it can be used both as a timer and as trigger pulse. One adjusts the EPUT meter so that it will not begin counting until a drop has fallen off. It then counts for 10 sec and provides a pulse which is used to trigger the scope. The scope is also calibrated so that the time it takes for a signal to get to the 5 cm line is known. The oscillator frequency is 1000 Hz and the scope sweep time about 1 sec/cm. The individual waves are therefore not resolved, rather they appear as a wedge shaped image on the screen. One adjusts the variable capacitor (C) and resistor (R) until the wedge goes to a minimum at the center of the screen. This means that at the time represented by the 5 cm line

the bridge is in balance. Since the electrical double layer is a pure capacity, the value of the variable capacitor is the capacity of the drop. The EPUT meter and scope repeat this sequence for each drop. The surface area of the drop is determined by measuring the flow rate of the mercury. From the flow rate we get:

$$V = \frac{4}{3}\pi r^3 = \frac{mt}{d}$$

where m is the flow rate, t the time in the life of the drop and d the density of mercury. It follows that

$$A = 4\pi r^2 = 4\pi^{2/3} \sqrt{\frac{3}{4\pi} \frac{mt}{d}}$$

The capacity per unit area is now determinable for each value of potential set by potentiometer B and read on potentiometer A.

The main source of error in this experiment lies in the improper choice and preparation of capillaries. The capillary must be thoroughly cleaned and then coated with dimethyl-dichloro-silane. This prevents the solution from getting inside the capillary. The tip of the capillary must be even. A sliver of glass projecting from the tip will effectively decrease the surface area of the drop. The flow rate must also vary during the course of the experiment since the interfacial tension is a function of potential and the actual pressure causing flow is $(P - \frac{2\gamma}{r})$. The variation in the rate of flow is not significant. It is also assumed in this experiment that the mercury surface is at equilibrium. At very low concentrations where this is not the case, an extrapolation must be made to the zero frequency value of the capacity.

III. The Adsorption of Halide Ions

A. Review of Previous Work

The halide systems have received particular attention in the study of the electrical double layer. They exhibit a continuous variation between the non-specifically adsorbed fluoride ion and the strongly adsorbed iodide ion. Compared with most other anions studied, the halides have a simple structure which can, to a first approximation, be represented by a point charge. This removes the complication introduced by permanent dipole moments, and the further difficulty with polynuclear anions of several possible orientations relative to the mercury surface. The halide systems are then obviously the first place to begin looking for a coherent explanation of anionic specific adsorption.

1. The fluoride ion

Grahame's work, which has been previously discussed, clearly shows that the fluoride ion is not specifically adsorbed.^{7,8} It should be mentioned that the identity of the cation has a slight quantitative effect, but no qualitative significance. The remaining question is to explain the shape of the C^i versus q curve. Unfortunately an adequate theory is still not in existence. On Figure 2, the C^i versus q curve for IMKF is plotted. The slight anodic peak is clearly evident. For NaF, Grahame found that this peak disappears with increasing temperature and that the capacity at 85°C rises continuously as q becomes more positive. The shape of the curve was independent of concentration at constant charge and temperature. These results lend support to the belief that the peak is due to a local maximum in the dielectric constant of the inner layer. The maximum could be caused by the reorientation of the water dipole. If one assumes that the dipole is preferentially oriented with its positive side to the mercury,

then reorientation would occur at positive surface charges. In the region where reorientation is occurring, the dipole should be freer to rotate with the alternating field. This results in a larger dielectric constant. One could also explain the peak by a variation in the thickness of the inner layer, which in fact was Grahame's choice. Peaks which can not be ascribed to specific adsorption also occur in other solvents at both positive and negative surface charge densities.²² This tends to support the dipole reorientation interpretation as opposed to a change in thickness. The remainder of the curve can be explained by a combination of electrostriction and dielectric saturation.

2. The chloride ion.

The adsorption of KCl was studied by Grahame and Parsons.¹² The isotherms at constant charge are definitely curved and would give a value of $q^1 = -q$ at infinite dilution if the linearity at low concentration was maintained. This effect has been observed in the adsorption of the I^- , Cl^- , Br^- , NO_3^- ions from single salt solutions.²³ At infinite dilution one would expect q^1 to equal zero rather than $-q$. There is at present no reasonable explanation for this effect. The variation of q^1 with q at constant concentration is similar to that for KI and KBr, and the linear portions have the same slope. The components of the capacity were obtained from plots of ϕ^{m-2} versus q^1 at constant surface charge. The points at constant surface charge were considered to lie on a straight line. Therefore $q^1 C^i = q^1 K^i$ and $q^1 K^i$ is a function of surface charge only. There are large systematic deviations from a straight line which cast doubt on the constancy of $q^1 K^i$. In any case, using the constant values, the other components of the capacity were derived. $q^1 K^i$ decreases with increasing surface charge and $q^1 K^i$ must therefore also vary with q^1 . Parsons compared

$q K^i$ at $q^1 = 0$ to the integral capacity of the inner layer in a KF solution and found reasonable agreement. The integral capacity is given by

$$K = \frac{1}{\phi^{m-2}} \int_0^{\phi^{m-2}} C^i d q$$

The distance ratio was calculated by both the isotherm and capacity ratio methods. The values obtained from the two methods are different, but in each case they are lower than those obtained for KI. On this basis it is assumed that X_1 is larger for the chloride ion than for the iodide ion.

Payne has studied the adsorption of KCl from constant ionic strength solutions of KCl and KF.²⁴ The capacity curves have a distinct peak which becomes more prominent with increasing concentration. The peak remains when the inner layer capacity is determined and C^i is almost independent of concentration except at low concentrations. As in the pure KCl system, $q^1 C^i = q^1 K^i$ and is a function of charge only. In contrast to pure KCl, $q^1 K^i$ increases with increasing surface charge. The fact that C^i is almost independent of concentration is due to a simultaneous decrease in $q^1 C^i$ and increase in $\left| \frac{1}{q^1 K^i} \left(\frac{\partial q^1}{\partial q} \right) \right|$ as $|q^1|$ increases. The adsorption was found to fit a virial isotherm with $\ln \beta$ a non-linear function of the surface charge. Both the virial isotherm and the non-linear dependence of $\ln \beta$ on q are supported by Payne's plots of $-\Delta \frac{1}{C}$ versus q^1 at constant surface charge. These plots approach a limiting value for each charge. The limiting values are different due to the second term in $-\Delta \frac{1}{C}$. When $-\Delta \frac{1}{C}$ is plotted versus q at constant concentration, a peak occurred near $q=6$, and was followed by a decrease and approach to a limiting value. This is not true quadratic behavior in which the peak would be followed by a minimum and then another peak. Payne found that his isotherms could not be superimposed on the

pure KCl isotherms whether he used a_{\pm} or a_{\pm}^2 for the activity.

3. The bromide ion.

Recently, the adsorption of the bromide ion has been studied as part of an experiment whose primary purpose was to compare the two distinct methods of investigating the electrical double layer.²⁵ These are the electrocapillary curve and the differential capacity curve. It was determined that neither a virial or Frumkin isotherm fit the data. A complete analysis of specific adsorption was not presented.

4. The iodide ion

Grahame performed the most complete study of the adsorption of KI in water.²⁶ He found that q^1 was an approximately linear function of q at constant concentration except at quite negative values of q . The isotherms at constant charge were linear except at low concentrations where they begin to approach $q^1 = -q$. Grahame assumed this was due to experimental error and he used values of q^1 obtained by extrapolating the linear part of the curve. In a latter paper, Parsons, using Grahame's data, found that iodide adsorption fits a virial isotherm with $\ln \beta$ a linear function of the surface charge. It is not clear whether Parsons used Grahame's experimental data or his "corrected" data. The compounds of the capacity were then analyzed and ${}_q^1 C^i$ was found to be a function of charge only. ${}_q^1 C^i$ changes from $83 \mu\text{f}/\text{cm}^2$ at $q = -12$ to $70 \mu\text{f}/\text{cm}^2$ at $q = 16$. There are systematic deviations from these constant values which he assumed to be within experimental error. The intercept for the $q = 0$ line gave a value of E_z for KF which was 16 mv too cathodic. There must therefore be some curvature at low concentrations. Using his values of ${}_q^1 C^i$, he determined ${}_q^i C^i$. The value of ${}_q^i C^i$ was independent of q^1 and approximately equal to

C^i for KF at the same value of q . The equivalence of C^i and C_q^i implies that the adsorbed ions do not have the same effect as the surface charges.

Dutkiewicz and Parsons studied the adsorption of KI from constant ionic strength solutions of KI in KF.²⁸ Parsons was able to fit the ΔE versus $\ln x$ curves to a single composite curve and found the $\ln \beta$ was a linear function of the surface charge. The highest value of the surface charge used in this work appears to be $q = -4$ and the largest value of q^1 was -12 . Presumably the rapid rise in the capacity at more positive charge did not allow accurate data to be obtained. Plots of $\Delta \frac{1}{C}$ versus concentration indicate a Henry's law isotherm with $\frac{\partial \ln \beta}{\partial q}$ a constant. Plots of ϕ^{m-2} versus q^1 at constant charge were linear and parallel within experimental error. $q^1 K^i$ was equal to $89 \mu\text{f}/\text{cm}^2$. The intercept found from these plots is quite different than that found from the pure KI data which should not be the case. The distance ratio is larger in KI+KF than in pure KI implying that X_1 is smaller in KI+KF. The constant value of $\partial \ln \beta / \partial q$ is supported by the ΔE versus $\ln x$ curves which can be fit to a single composite curve. If the adsorption isotherms at constant charge are plotted against the salt activity, the curves for KI and KF + KI can be superimposed. This can not be done if the anion activity is used. At the time this result appeared to resolve the question of which activity to use in the isotherm, but further work has shown it to be limited to the iodide system.

B. The adsorption of KBr from a constant ionic strength solution of KBr in KF .

Introduction

As should be obvious from the discussion of previous research, the adsorption of halide ions is not as simple as one would first expect. One of the main problems is to explain the different behavior of KCl and KI

when they are adsorbed from constant ionic strength solutions with KF. The difference between the iodide and chloride ion is much more pronounced in the mixed electrolyte systems than in the single salt systems. One possible explanation is that there are no qualitative differences, and that this would be apparent if iodide adsorption could be studied at positive surface charge densities. The bromide ion is intermediate in its strength of adsorption between the chloride and iodide, and the purpose of this experiment was to study its adsorption as compared to the other halides. The mixed electrolyte system was chosen for two main reasons: 1) The analysis can be more rigorously justified than that for a single salt. 2) The data for KI+KF and KCl+KF is more complete and probably more reliable than the earlier work on the single salt systems.

One of the benefits of choosing the mixed electrolyte system is a simplification which occurs in the electrocapillary equation and allows the specifically adsorbed charge to be determined without first determining the diffuse layer charge. We begin with the previously derived equation:

$$d\gamma = -q dE - \Gamma_{F,w}^- d\mu_{KF} - \Gamma_{Br,w}^- d\mu_{KBr}$$

We assume that the activity coefficients of KBr and KF are dependent only on the total ionic strength.

Therefore

$$d\mu_{KF} = RT d \ln m_{KF} = kT d \ln(1-x)$$

$$d\mu_{KBr} = RT d \ln m_{KI} = kT d \ln x$$

where x is the molarity of KBr, the total molarity being $1M$. Substituting in the electrocapillary equation gives

$$d\gamma = -q dE - \left[\Gamma_{Br,w}^- - \left(\frac{x}{1-x} \right) \Gamma_{F,w}^- \right] kT d \ln x$$

From diffuse layer theory and the assumption that the fluoride ion is not specifically adsorbed, one gets the relationship:

$$\frac{\Gamma_{\text{Br}^-}^{\text{d}}}{\Gamma_{\text{F}^-}^{\text{d}}} = \frac{x}{1-x}$$

also

$$\Gamma_{\text{Br}^-} = \Gamma_{\text{Br}^-}^{\text{i}} + \Gamma_{\text{Br}^-}^{\text{d}}$$

Therefore

$$d\gamma = -q dE - \Gamma_{\text{Br}^-}^{\text{i}} kT d \ln x$$

and

$$d\xi = E d q - \Gamma_{\text{Br}^-}^{\text{i}} kT d \ln x$$

The specifically adsorbed charge is determined directly from the differentiation of ξ and γ . The assumptions used here are more general than those needed for adsorption from a single salt. We are assuming that $\Gamma_{\text{Br}^-}^{\text{d}}$ is proportional to x , whereas in the single salt system we would have to derive $\Gamma_{\text{Br}^-}^{\text{d}}$ from a specific equation. The determination of the amount specifically adsorbed is therefore more reliable. Another simplification arises when isotherms are considered. In the mixed electrolyte system the choice of activity does not arise since the assumption that the activity coefficients are constant is equivalent to setting $d \ln a_{\text{K}^+} = 0$ in the following equation.

$$d \ln a_{\text{KBr}} = d \ln a_{\text{K}^+} + d \ln a_{\text{Br}^-} = d \ln m$$

but

$$d \ln a_{\text{Br}^-} = d \ln m$$

Either assumption leads to using x for the activity.

Experimental

All experiments were performed with the previously discussed equipment. Reagent grade chemicals were used without further purification, but the water used was distilled from alkaline potassium permanganate. The reliability of the equipment and the absence of adsorbable impurities in the salts was confirmed by comparing our results for 1 MKF and 1MKBr with those previously reported in the literature. The capacity was measured at 50 mv intervals from at least -1.4v to the most positive voltage obtainable. This is usually -.2 volts. In the region where the capacity peak occurs, smaller voltage intervals were used. Five capacitance decades from $1\mu\text{f}$ to $.0001\mu\text{f}$ were available and balance was reproducible to $\pm .0002\mu\text{f}$, which represents .1% in the measured capacity. Streaming electrode potentials were as previously stated reproducible to within 1 mv.

Results

The capacity of eleven solutions of $x\text{MKBr} + (1 - x)\text{MKF}$ were measured at 25°C and are shown in Figure 4. These curves are qualitatively similar to those found in $\text{KCl} + \text{KF}$ in that a distinct peak occurs at higher concentrations. The peak in the KBr curves occurs at a higher value of the capacity and a more negative value of the potential than in KCl. It is also less pronounced. This shift in the peak height and position is due to the stronger adsorption of the bromide ion. The capacity curves are equivalent when the potential is less than -1.3 volts. This fact was used in integrating the curves. The capacity curve is integrated by fitting each successive set of three points to a parabola. The first integral gives q and the second γ and ξ . The values of q , C , E , γ , and ξ are then

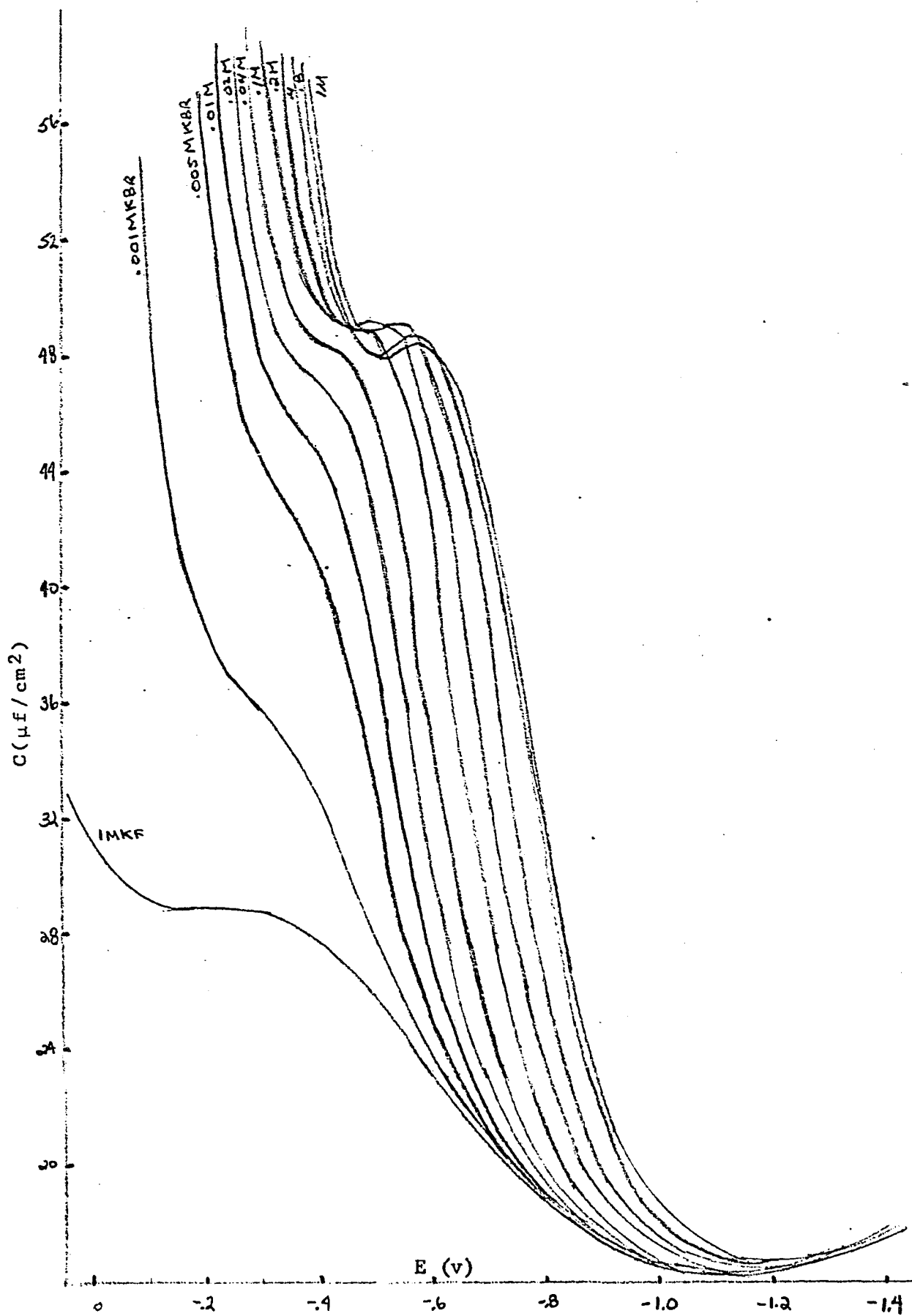


Figure 4. The Capacity of The Double Layer as a Function of Potential for $x\text{MKBr} + (1-x)\text{MKF}$

found for all integral values of q which occur in the range covered by the three experimental capacity points. The program then reads another experimental point and uses the determined values of the second point for the integration constants. The program is discussed in more detail in the appendix. One set of integration constants is needed to use the program. These are usually E , C , γ at $E = E_z$. Due to the fact that all of the curves are equivalent at large negative values of the potential, we may avoid the determination of γ . We integrate the LMKF curve assuming $\gamma = 0$ at $E = E_z$, and obtain the value of γ , C , E at $q = -19$. The KBr + KF curves can now be integrated from $q = -19$ using the LMKF data for the integration constants. If this procedure is valid, the values of E_z computed by the integration and those directly determined by the streaming electrode method must be equivalent. The two sets of values are presented in Table 1.

Table 1

Solution	Concentration x	E_z (Ex)	E_z (Com)
1	0	-.4740	-
2	.001	-.4820	-.4828
3	.005	-.4996	-.4988
4.	.01	-.5130	-.5127
5	.02	-.5295	-.5300
6	.04	-.5486	-.5486
7	.1	-.5769	-.5776
8	.2	-.6004	-.6020
9	.4	-.6245	-.6252
10	.8	-.6477	-.6472
11	1	-.6550	-.6568

The agreement is well within the acceptable limits. The second program then takes the derivative of ξ by $\ln x$ at constant q to give q^1 since

$$d\xi = E d q + \frac{k T N}{F} q^1 d \ln x$$

The programs and data are presented in the appendix. In the course of evaluating the data, we decided not to use the .001M KBr set. It was decided that the results of the second program were more reliable if this set of data were excluded. It would be interesting to study the adsorption of KBr at low concentrations, but this would require the use of a frequency extrapolation of the capacity. The reliability of this procedure has not been demonstrated for ionic solutions. To show that the procedure was reliable, the equivalence of the twice integrated capacity curves and experimentally determined electrocapillary curves must be demonstrated. There is also the possibility that at very low concentrations the streaming electrode potential may not be the same as the potential at the point of zero charge. This will occur if equilibrium is not reached at the streaming electrode.

The specifically adsorbed charge is plotted against the surface charge at constant concentration in Figure 5 and the isotherms are plotted in Figure 6 at constant charge. The q^1 versus q curves are similar to those for KCl + KF. The major difference is that they become almost linear at lower values of the surface charges. The effect of the stronger adsorption of Br^- than Cl^- is also evident in the isotherms. The isotherms for KCl + KF and KI + KF are similar in shape to the KBr + KF isotherms for $q < 0$. In the case of KI no data was taken above $q = -4$, for KCl the amount adsorbed at any concentration and charge is almost 40% less than for KBr. The change in the curvature of the isotherms has not been previously noted and at $q > 12$ appears to indicate that saturation is being approached. An attempt was made to determine the isotherm and the charge dependence of the standard free energy. The surface pressure versus $\ln x$ curves can not be superimposed on one common curve with the same accuracy

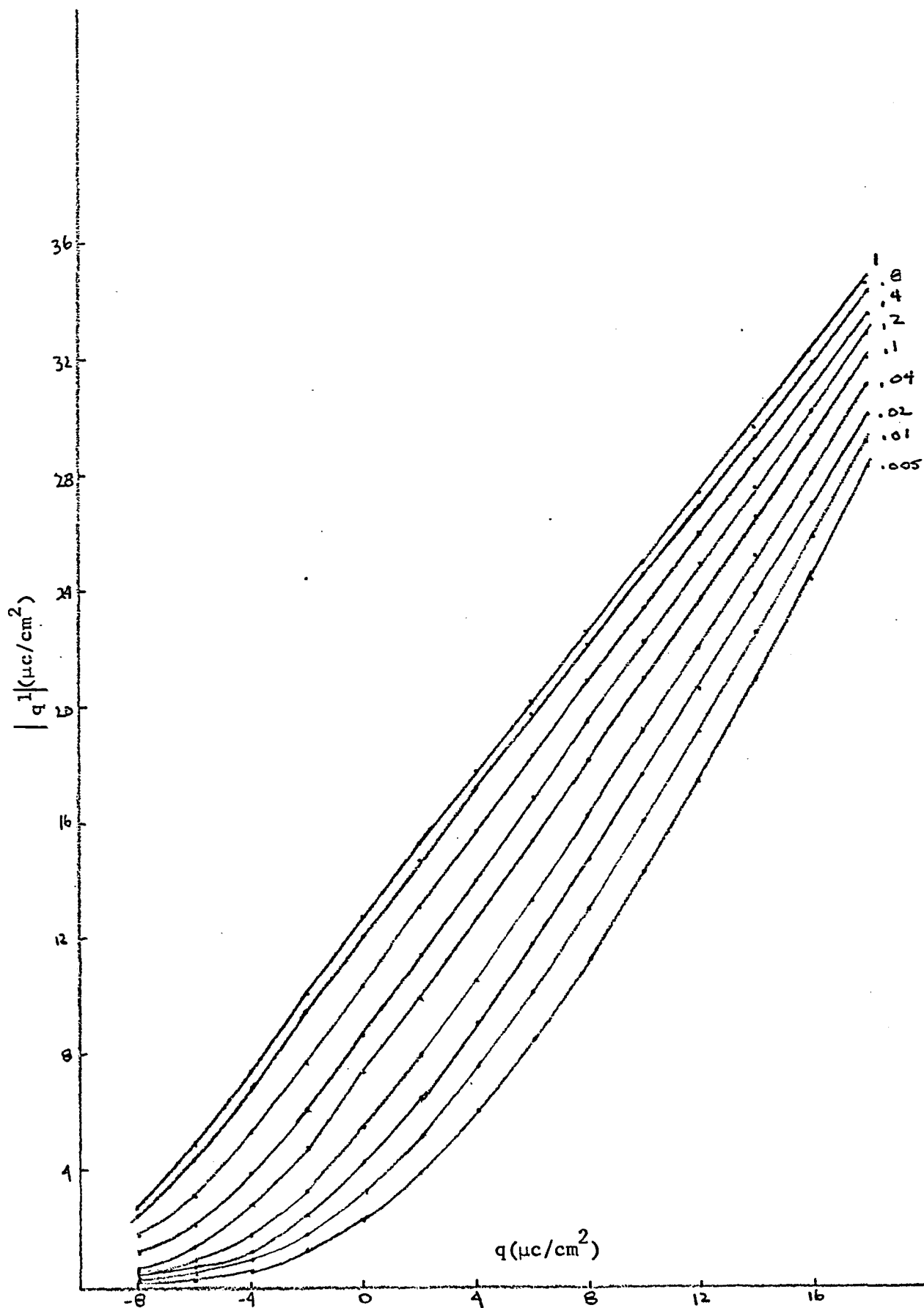


Figure 5. The Variation of The Amount Specifically Adsorbed with The Surface Charge Density at Constant Concentration for x MKBr + $(1-x)$ MKF

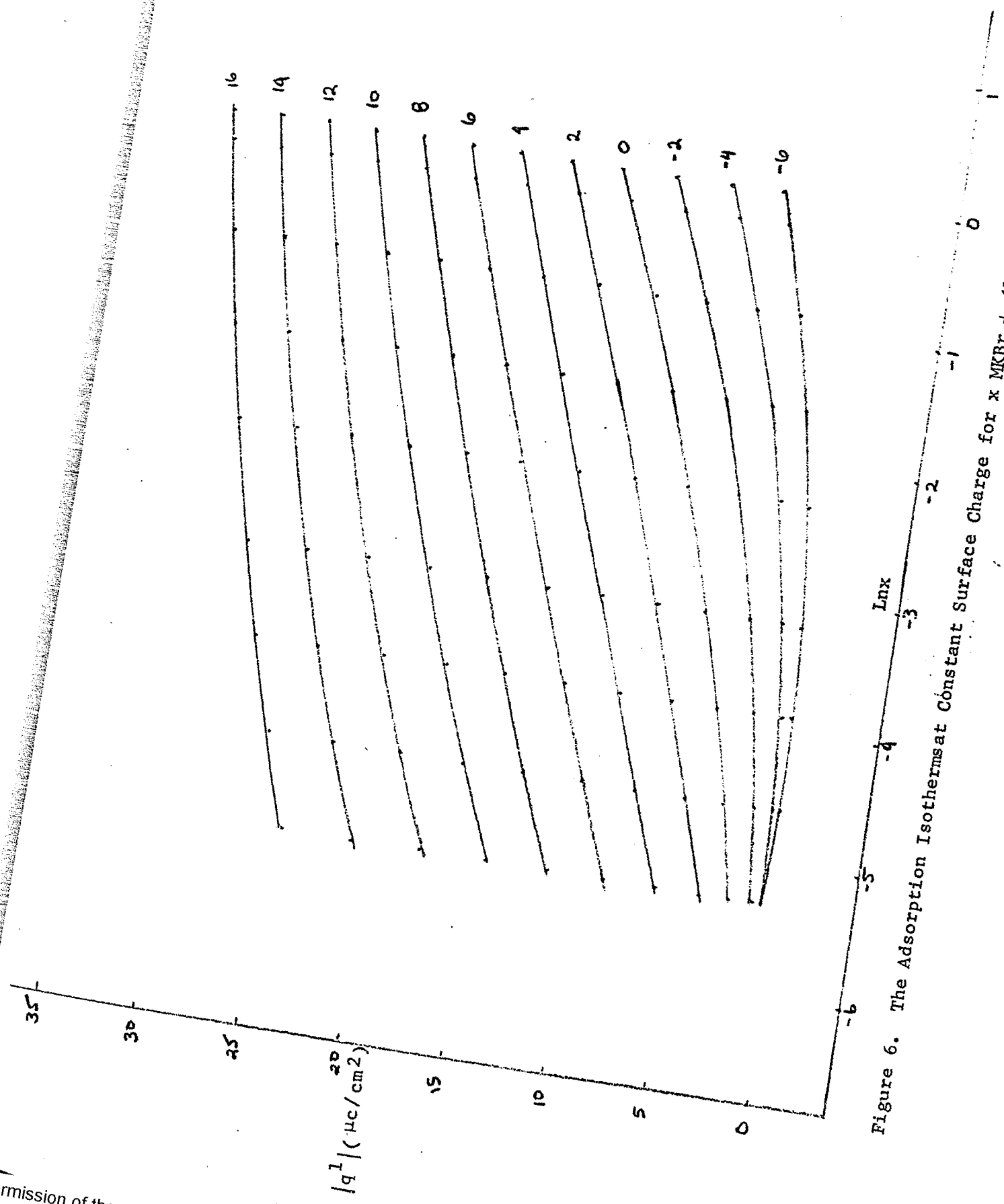


Figure 6. The Adsorption Isotherms at Constant Surface Charge for x MKBr + $(1-x)$ MKF

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as in the KCl-KF system. Payne claims that his deviations from a common curve using a virial isotherm are no greater than $.2 \text{ ergs/cm}^2$. In this system deviations of up to 5 ergs/cm^2 occur at large $q > 8$ if the best possible curve is drawn. One explanation is that the isotherm constants are a function of the surface charge. Another is that the surface pressure method is inaccurate due to the ambiguities in choosing LMKF as the base solution. To avoid the surface pressure problem, the virial isotherm was checked by plotting Γ_{Br^-} versus $\ln x/\Gamma_{\text{Br}^-}$ at constant q . As is evident in Figure 7, straight lines are not obtained. The low concentration values for $q=-4$, $q=-6$, can be disregarded because of the small value of q^1 . If a virial isotherm were obeyed, the curves should be both linear and parallel. If one assumes that virial isotherm is obeyed but that B is not constant, it follows from Figure 7 that B is increasing with q at constant q^1 and increasing with $|q^1|$ at constant q . The increase in B with $|q^1|$ is quite reasonable and simply means that repulsion between adsorbed ions is occurring. The increase in B with increasing surface charge could only be explained by competitive adsorption of water. If it is harder for a bromide ion to displace a water molecule at large values of the surface charge than at low values, B will increase with the charge. Competitive adsorption results in a quadratic standard free energy and the fact that this system demonstrates quadratic behavior supports the above interpretation.

In Figure 8, the inner layer capacity is shown as a function of charge for several concentrations. The solutions not shown are virtually identical with the LMKBr line. The concentration independence of C^i is also present in the KCl+KF system. In order to interpret the variation of C^i with q , the components of the capacity were determined. In Figure 9, ϕ^{m-2} is plotted against q^1 at constant q and the best straight line has been

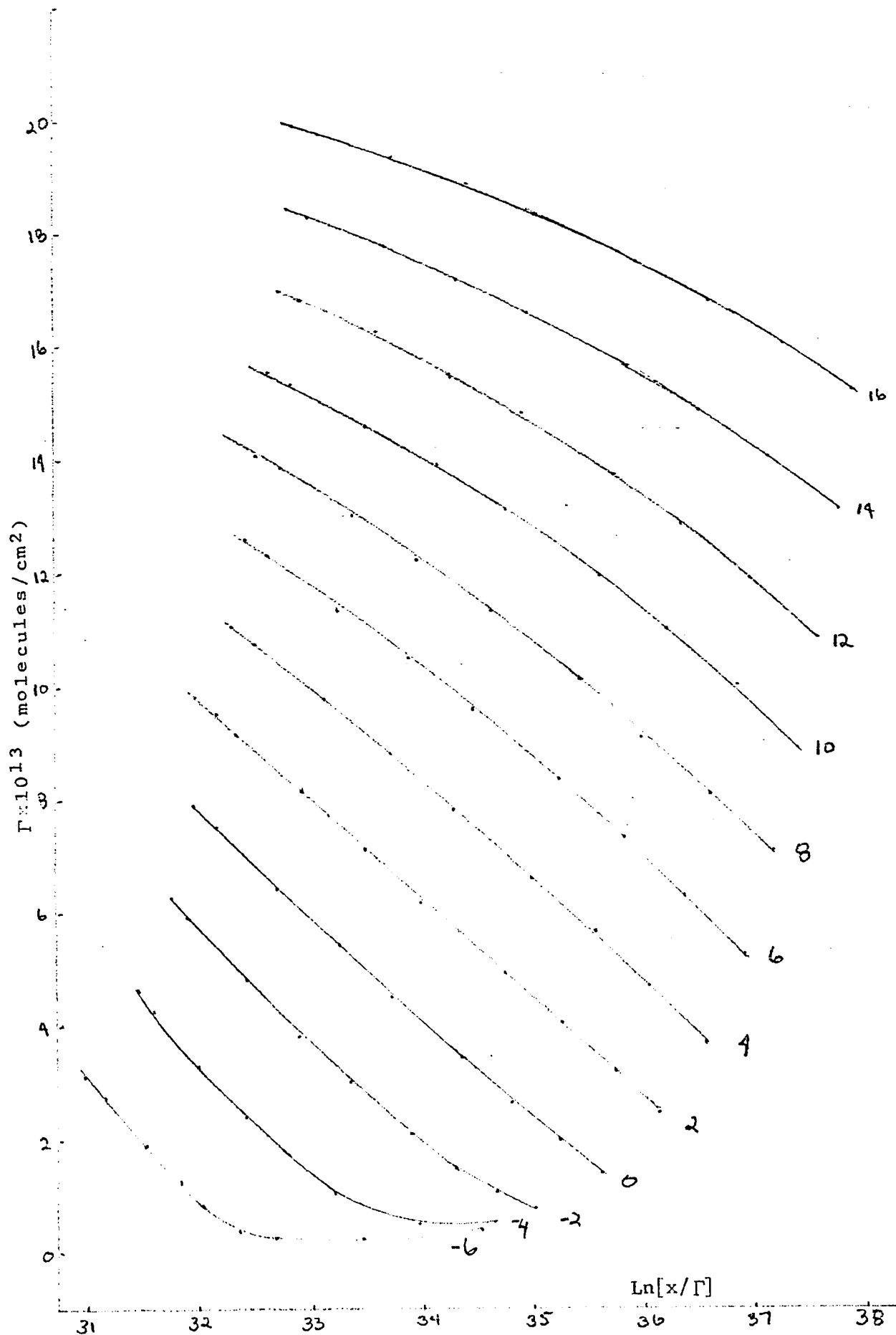


Figure 7. The Amount Specifically Adsorbed (Γ) Plotted as a Function of $\ln[x/\Gamma]$ for PMVPr + (1-x)MVE

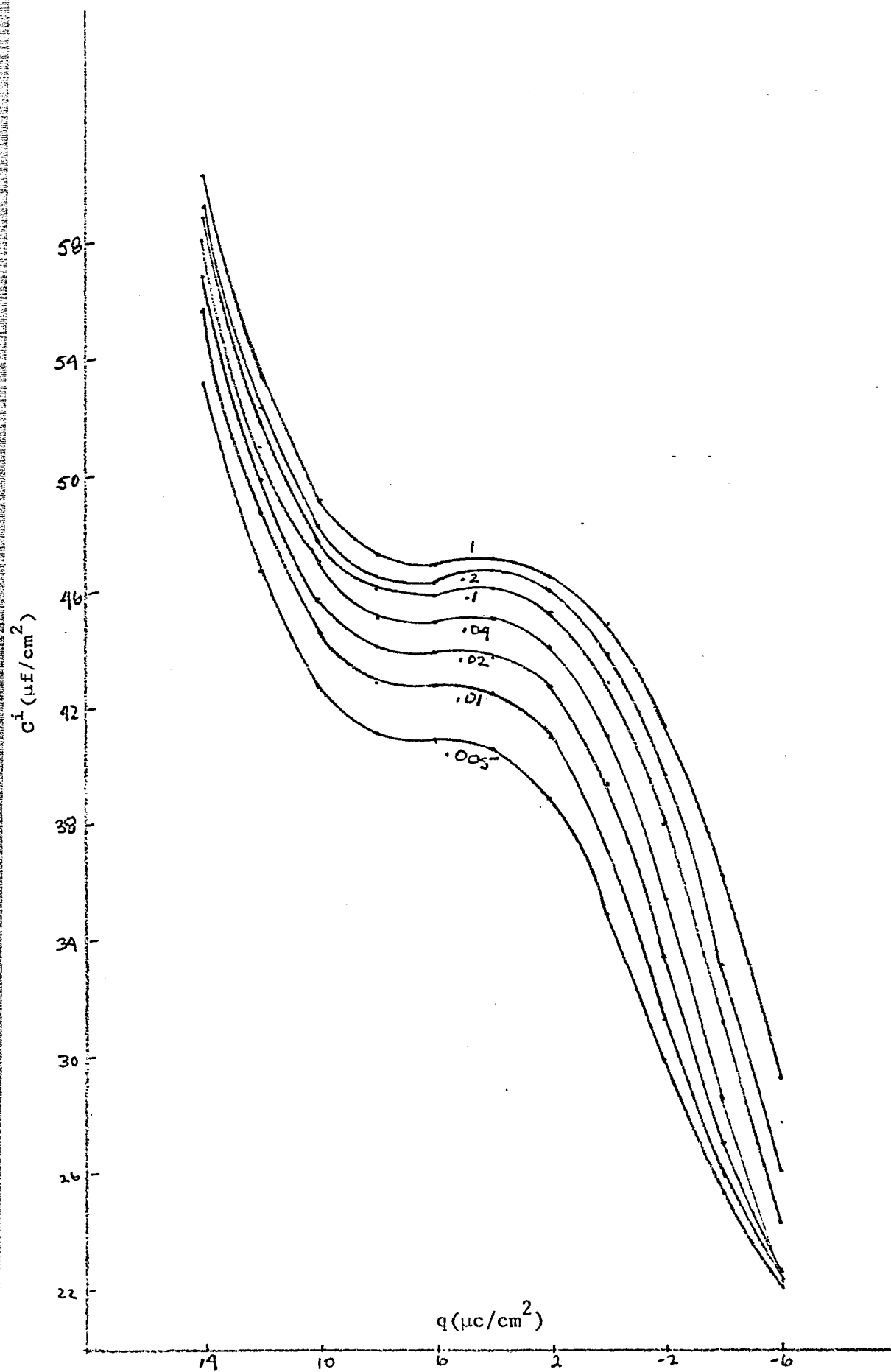


Figure 8. The Inner Layer Capacity of $x\text{MKBr} + (1-x)\text{MKF}$ as a Function of Surface Charge Density

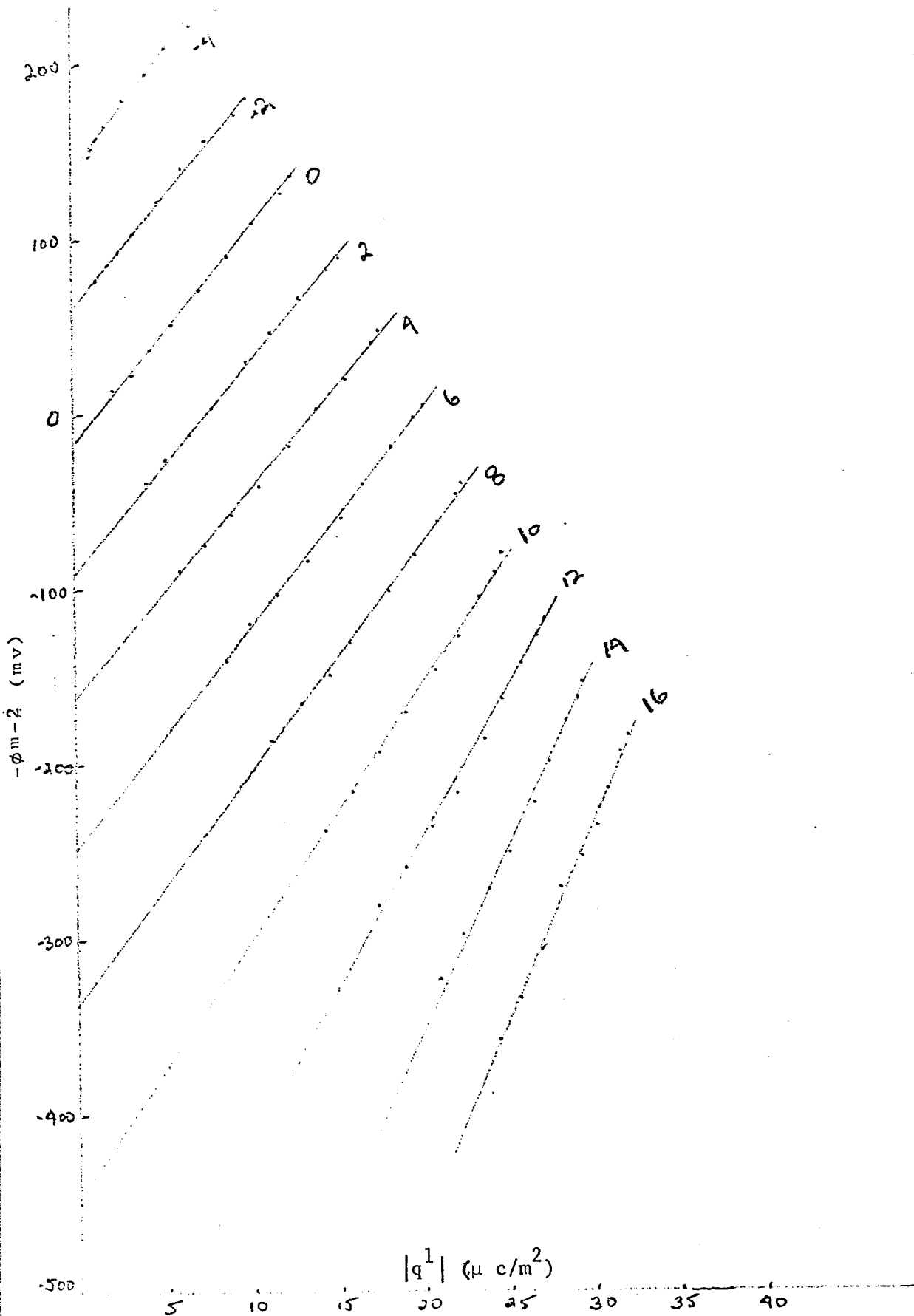


Figure 9. The Potential Across the Inner Layer Plotted as a Function of Specifically Adsorbed Charge for $x\text{MKBr} + (1-x)\text{MKF}$

drawn through the points. Though it is not apparent on this graph due to its scale, the points appear to lie on a parabola rather than a straight line. The equation for the components of the capacity is:

$$\frac{1}{C^i} = \frac{1}{q C^i} + \frac{1}{q^1 C^i} \left(\frac{\partial q^1}{\partial q} \right)_u$$

$\left(\frac{\partial q^1}{\partial q} \right)_u$ was obtained by fitting the q^1 versus q data to a cubic equation and obtaining its shape. These values were checked against the graphically determined values. ${}_q^1 C^i$ is obtained either from the inverse of the slope of the lines in Figure 9, in which case it is equal to ${}_q^1 K^i$ or from the inverse of the slope of a quadratic equation giving ϕ^{m-2} as a function of q^1 . Both of these methods were used to evaluate ${}_q^1 C^i$. The values of ${}_q^1 K^i$ obtained from the Figure 8 are presented in Table 2.

Table 2

q	${}_q^1 K^i$
-6	84.7
-4	80.0
-2	84.8
0	86.8
2	85.0
4	83.8
6	80.4
8	74.1
10	66.3
12	60.3
14	52.1

The decrease in ${}_q^1 K^i$ with increasing charge would be explained by a decrease in $\epsilon/(x_2 - x_1)$ according to the present model. A decrease in either ϵ or x_1 seems perfectly reasonable, but no distinction between the two is possible. The intercept of ϕ^{m-2} at $q^1 = 0$ are not the ϕ^{m-2} values for LMKF solution, so that if the model is valid, the lines must be curved at lower concentrations. The two sets of values for ${}_q^1 C^i$ were used to obtain ${}_q C^i$. Figure 10 shows ${}_q C^i$ as a function of q for four concentrations where the linear value of ${}_q^1 C^i$ were used. In Figure 11, the quadratic values were used. The most important point is that independent of the method used, ${}_q C^i$ has a distinct peak in the region $q = 0$ to $q = 4$. This peak can not be due to specific adsorption since the peak height and position are virtually independent of concentration and therefore of specific adsorption. In Figure 11, ${}_q C^i$ remains independent of the amount of specific adsorption even at large values of the surface charge whereas the curves in Figure 10 are different in this region. A peak in ${}_q C^i$ which is independent of q^1 , must be due to some alteration of the interaction between the electrode and the solvent. As mentioned previously, ${}_q C^i$ is independent of concentration in KI solutions. In the KCl+KF system, ${}_q K^i$ decreases as $|q^1|$ increases at constant q . It follows that if ${}_q K^i$ is plotted against q at constant concentration, the curves at higher concentrations are lower. In the KI system, ${}_q K^i$ is independent of concentration and increases with increasing charge. In KBr+KF, ${}_q K^i$ is independent of concentration when $q < +4$. At larger values of the surface charge, ${}_q K^i$ eventually begins to increase depending on the concentration. The variation of ${}_q K^i$ with surface charge at constant concentration is shown in Figure 12 for three concentrations. The increase in ${}_q K^i$ with increasing q^1 is evident from the vertical distance between the curves in the

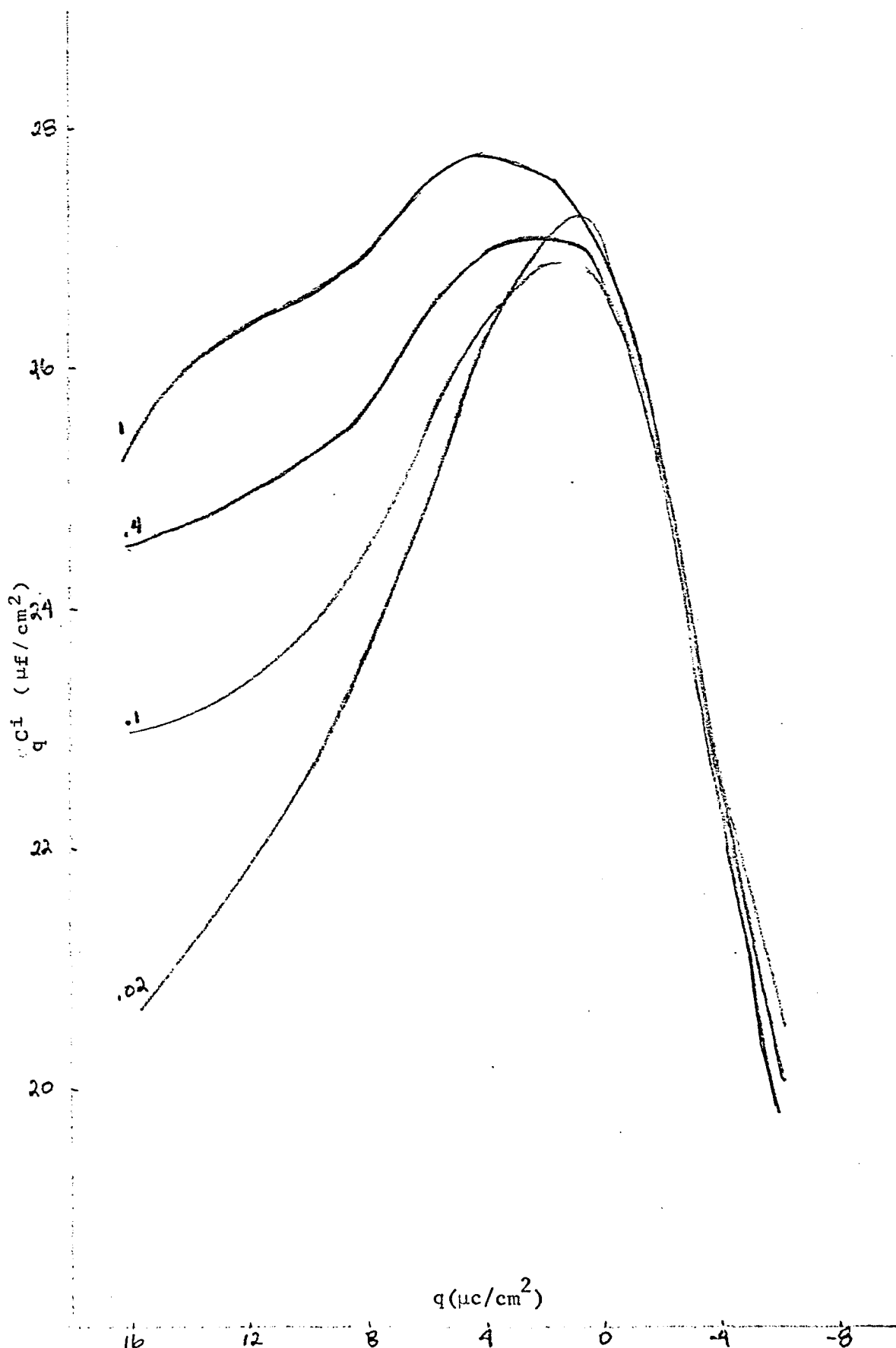


Figure 10. The Differential Capacity at Constant Amount Adsorbed as a Function of Surface Charge Density for $x\text{MKBr} + (1-x)\text{MKF}$ Using Values of C_1 Determined from Figure 9.

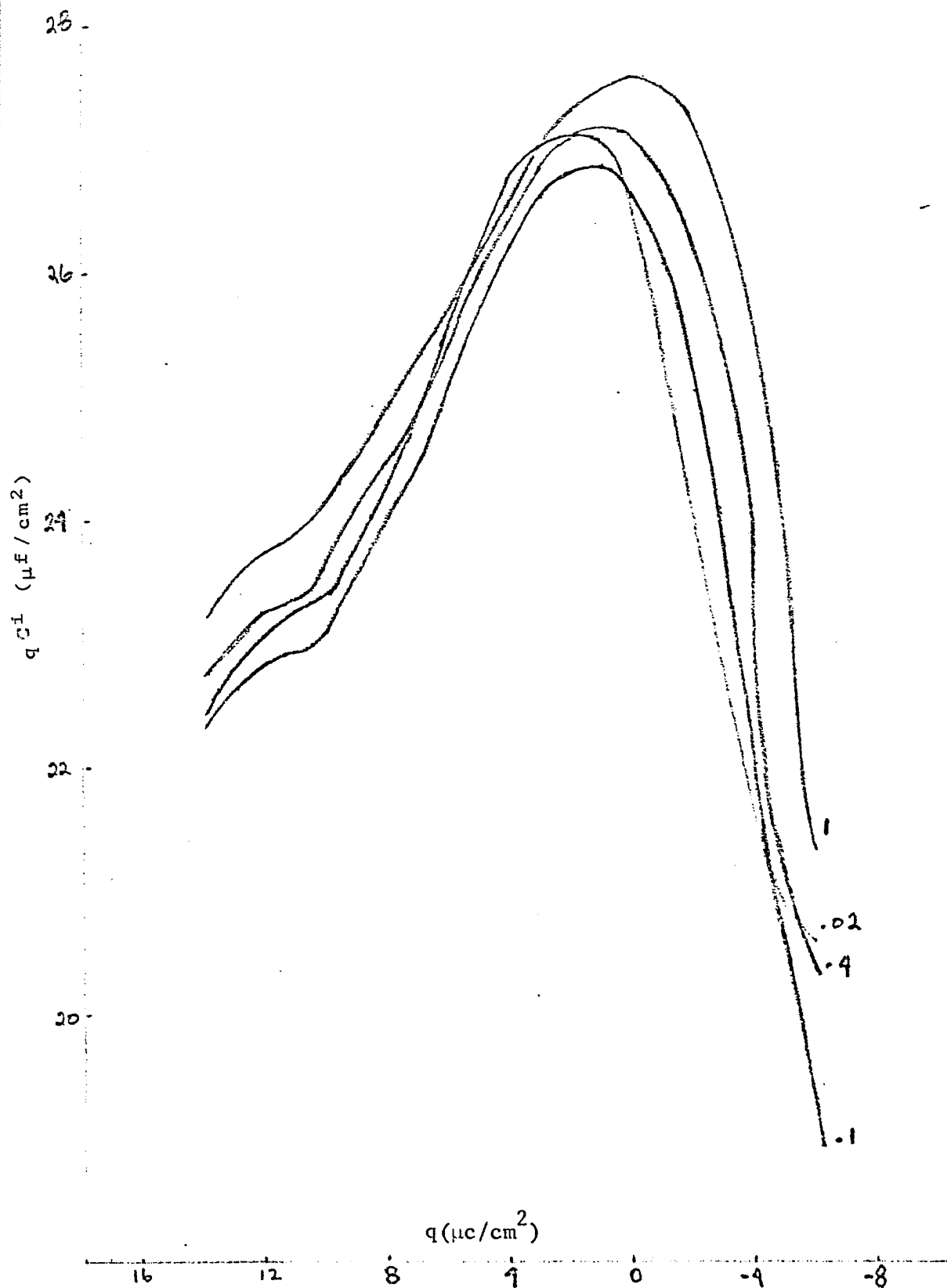


Figure 11. The Differential Capacity at Constant Amount Adsorbed as a Function of Surface Charge Density for $xMKBr + (1-x)MKF$ Using Values of $|c_1|$ Determined by Program III.

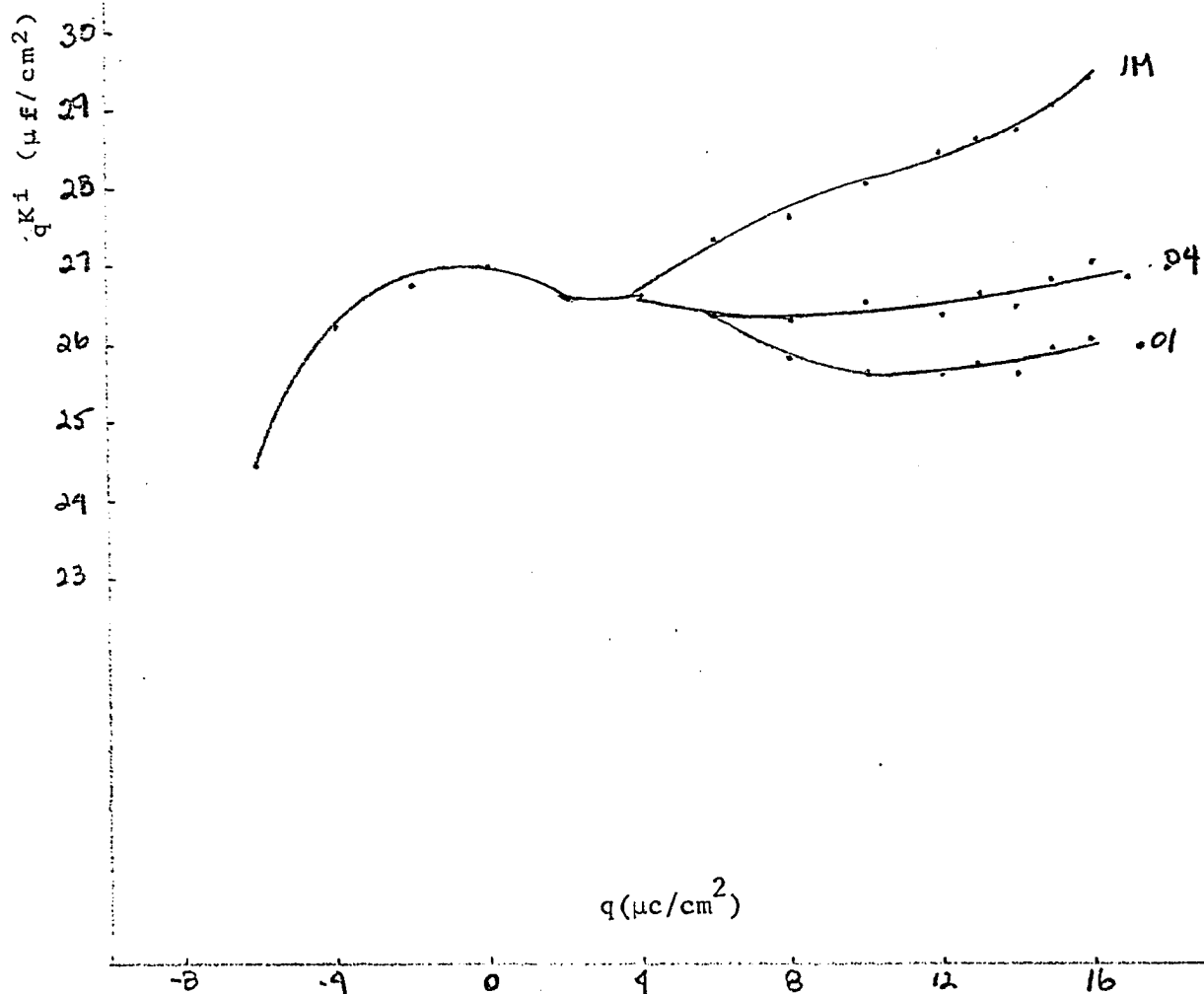


Figure 12. The Integral Capacity at a Constant Amount Adsorbed as a Function of Surface Charge Density for $x\text{MKBr} + (1-x)\text{MKF}$

anodic region. There is no convincing argument to explain the different behavior of the three systems.

As derived in the theoretical section, the equation relating the capacity to the isotherm is the following.

$$-\Delta \frac{1}{C^i} = -k T \left[\left(\frac{\partial \ln \beta}{\partial q} \right)^2 \frac{\partial |q^1|}{\partial \ln \beta} + |q^1| \frac{\partial^2 \ln \beta}{\partial q^2} \right]$$

We have also shown that $-\Delta \frac{1}{C}$ should reach a limiting value for large values of Γ if a virial isotherm is obeyed. In Figure 13, $-\Delta \frac{1}{C^i}$ has been plotted against $|q^1|$ at constant charge. The curves for $q > 6$ represent amounts of specific adsorption greater than those observed by Payne. Payne ascribed the decrease in the limiting value with increasing q to the neglect of the second term in the brackets which is negative. Let us assume $\ln \beta$ may be written as follows:

$$\ln \beta = \ln \beta_{\max} + a q - \frac{b}{2} \delta^2$$

$$|a| \gg |b| \quad \delta = (q - q_0)$$

Our equation for $-\Delta \frac{1}{C}$ is then

$$-\Delta \frac{1}{C^i} = k T \left[a^2 \frac{\partial |q^1|}{\partial \ln \beta} - b |q^1| \right]$$

where we have set $\frac{\partial \ln \beta}{\partial q} = a$ and q_0 is a constant value of q . This equation will still give a limiting value of $-\Delta \frac{1}{C^i}$ if $|q^1|$ is not too large. The curves at higher q also appear to approach a limiting value, though now at progressively lower values of B if we assume a and b are constant. We have already shown that if a virial isotherm is assumed, B increases with increas-

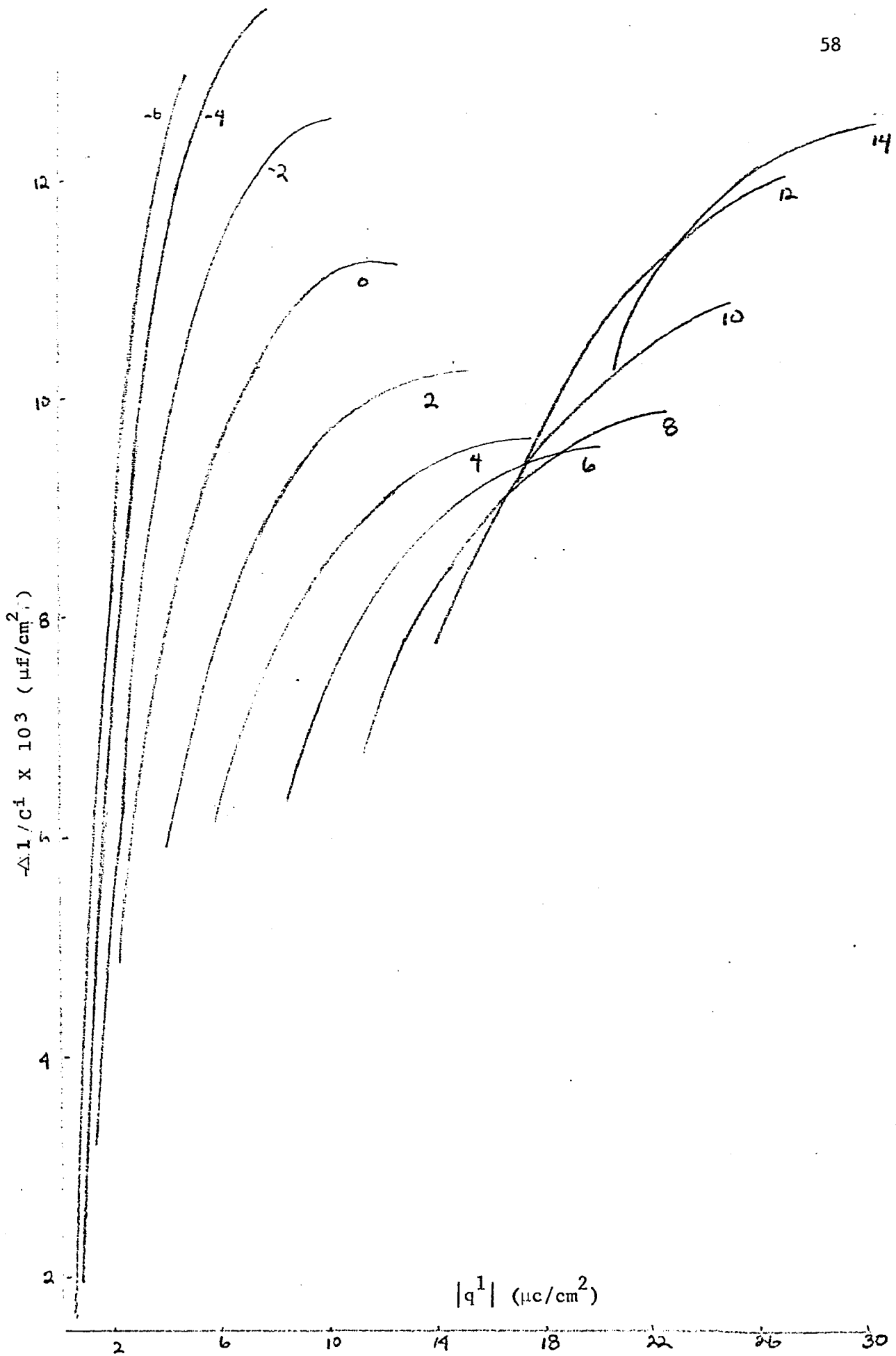


Figure 13. $-\Delta 1/C^1 \times 10^3$ Plotted Against the Amount Adsorbed at Constant Surface Charge Density

ing charge. One could also assume that \underline{a} increases faster with increasing charge than B which would give a higher value of $-\Delta \frac{1}{C^i}$ at the limit since

$$-\Delta \frac{1}{C^i} = \frac{k T a^2}{2B}$$

We also investigated the possibility that at high values of q , the KBr + KF system might begin to behave like the KI - KF system. In the KI+KF system, a Henry's law isotherm is obeyed. That is, if we assume the following isotherm:

$$|q^1| = \beta C K$$

C = concentration

K = constant

$$\frac{\partial \ln \beta}{\partial q} = a$$

$$-\Delta \frac{1}{C} = k T a^2 K \beta C$$

In this case the curves are straight lines at constant charge when plotted against concentration and the slope increase with increasing charge. A plot of $-\Delta \frac{1}{C^i}$ versus concentration for this system does not give straight lines except at high concentrations. Figure 14 is a plot of $-\Delta \frac{1}{C}$ versus $|q^1|$ at constant q . It is included to demonstrate that the choice between $\Delta \frac{1}{C^i}$ and $\Delta \frac{1}{C}$ is not trivial and requires more justification than it has received. Figure 15 is a plot of $-\Delta \frac{1}{C^i}$ versus q at constant concentration and Figure 16 a plot of $-\Delta \frac{1}{C^i}$ versus $|q^1|$ at constant concentration. The KCl + KF system shows the same behavior for $q < 6$ except that the peak occurs at $0 < q < 4$ depending on the concentration whereas here it occurs

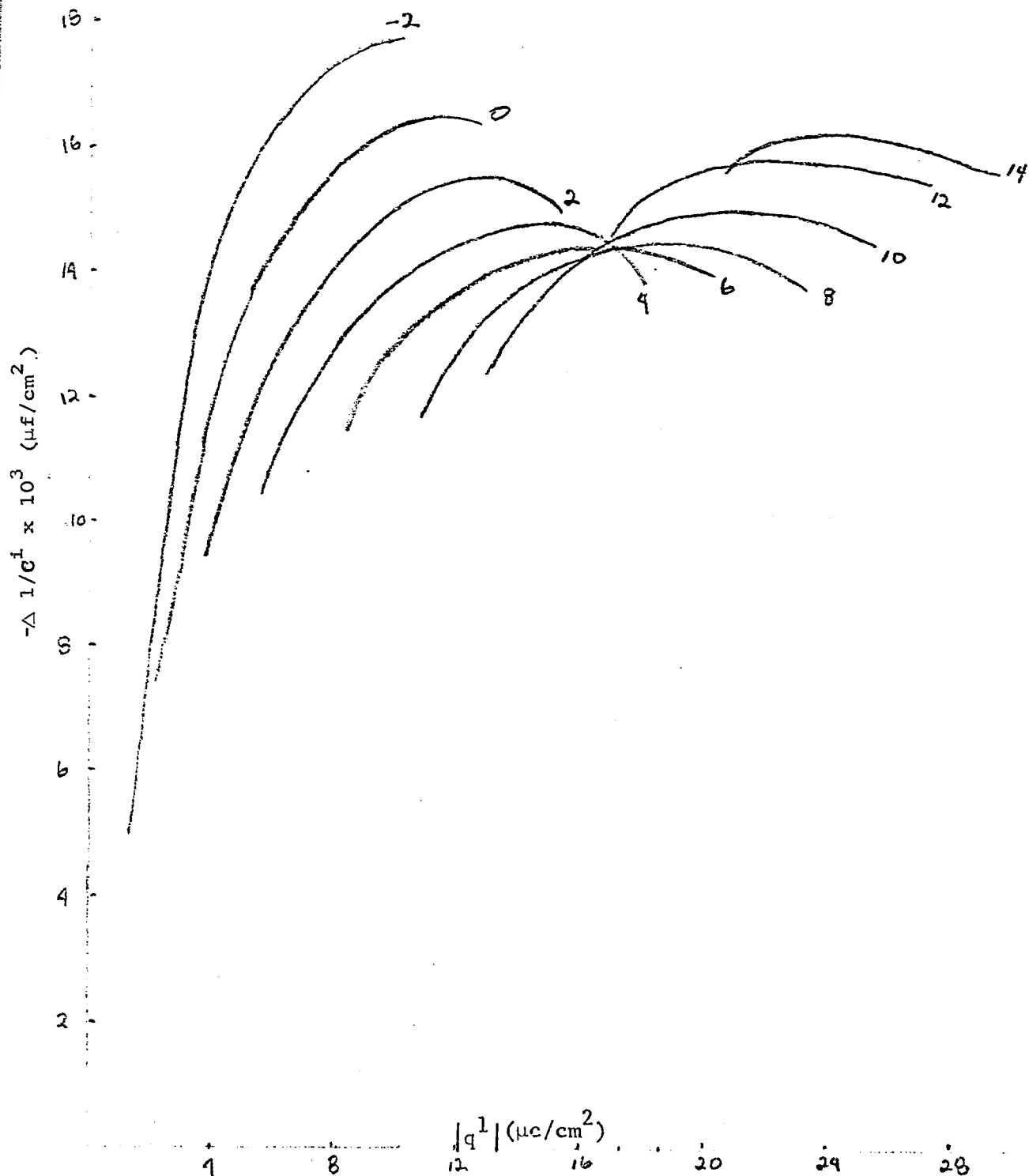


Figure 14. $-\Delta 1/C^i \times 10^3$ Plotted Against the Amount Adsorbed at Constant Surface Charge Density

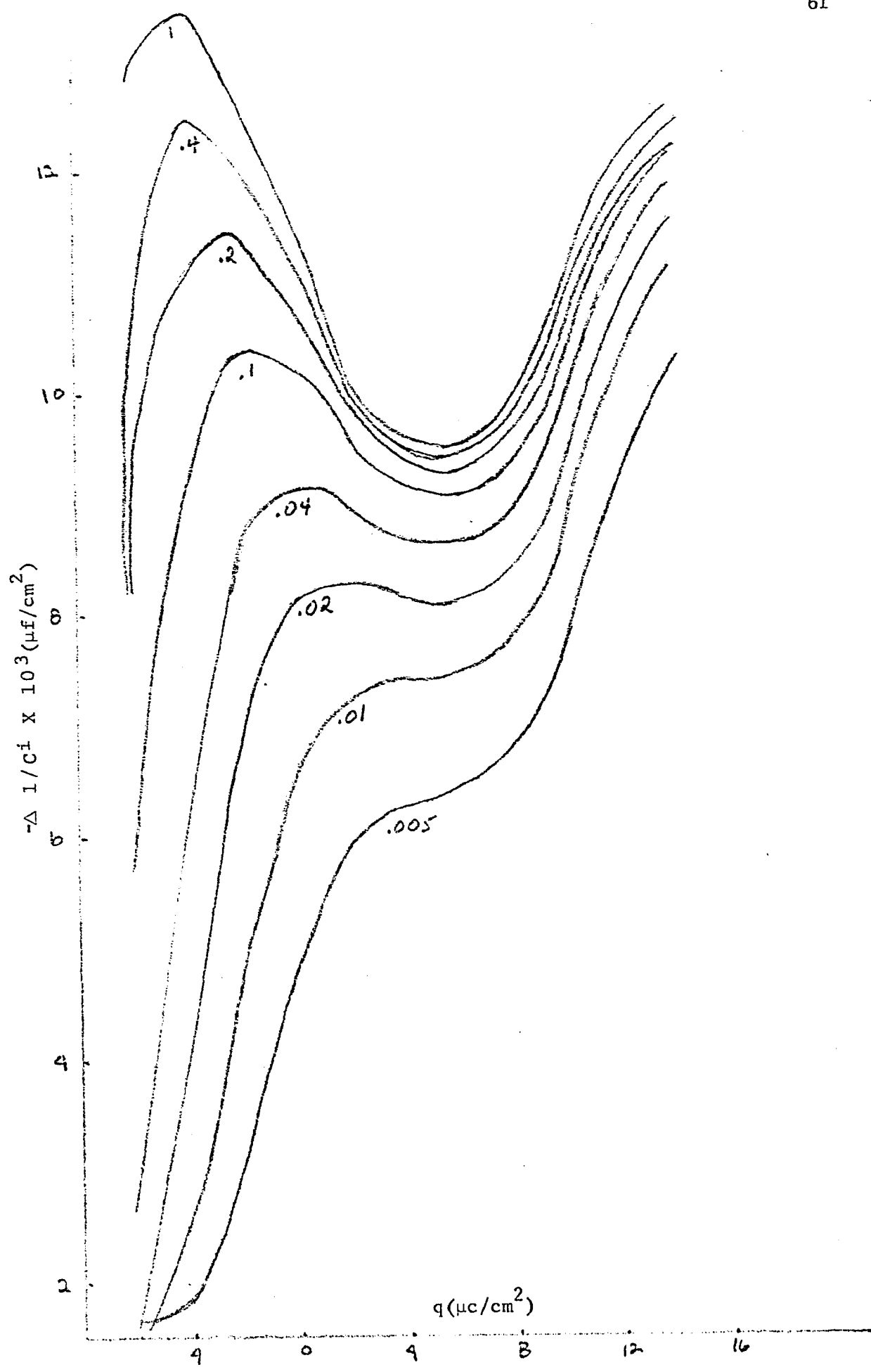


Figure 15. $-\Delta 1/C^i \times 10^{-3}$ Plotted Against the Surface Charge Density at Constant Concentration $C^i = 10^{-3}$ M.

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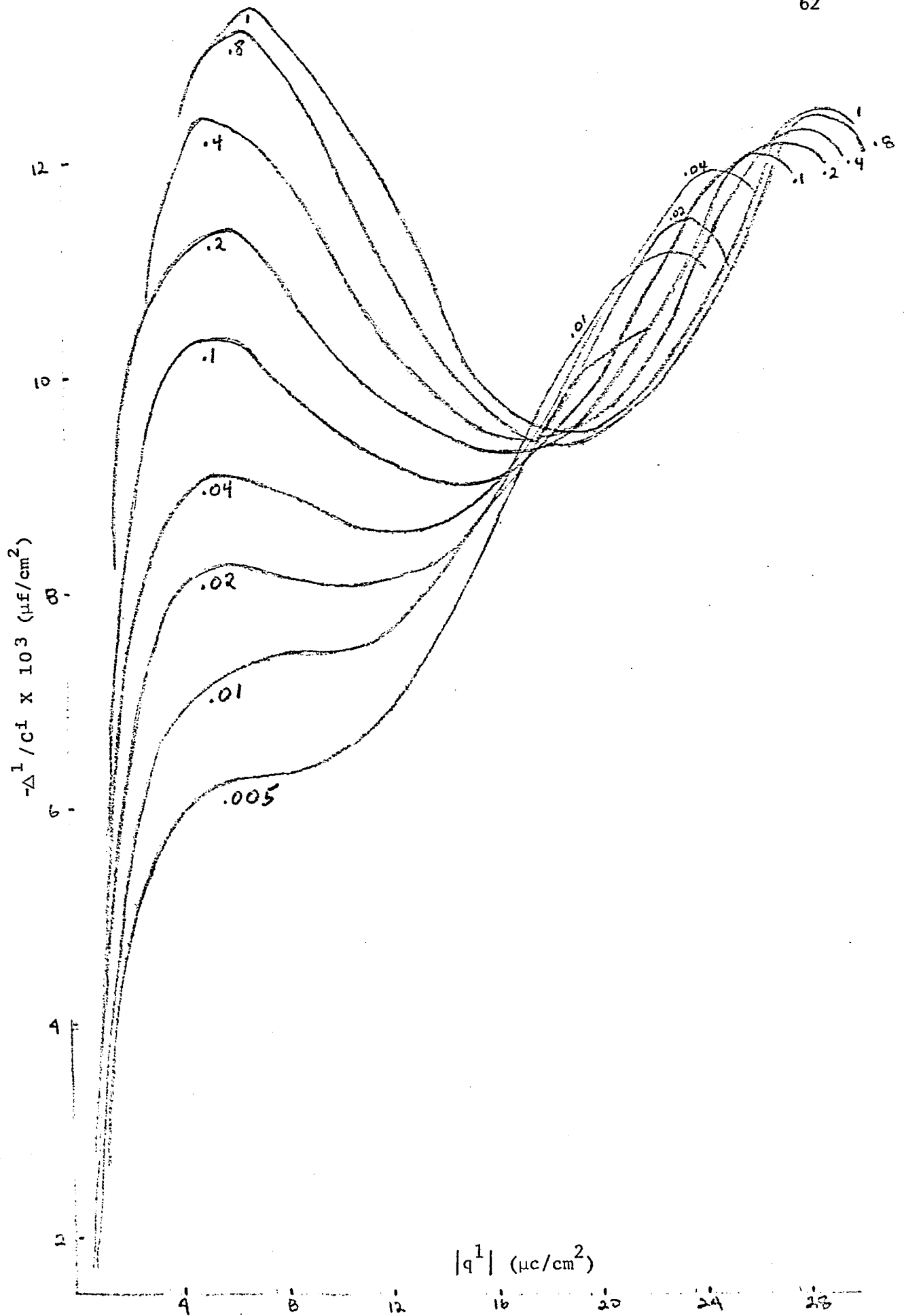


Figure 16. $-\Delta^1 / C^1 \times 10^3$ Plotted Against the Amount Specifically Adsorbed at Constant Concentration for $xMKB + (1-x)MKB$

at $-4 < q < 0$. This is no doubt due to increased adsorption. The increase for $q > 6$ or $|q^1| > 18$ is not found in KCl + KF. As discussed previously, the existence of two peaks is indicative of a quadratic standard free energy of adsorption. For a purely quadratic $\ln\beta$, $-\Delta \frac{1}{C}$ must change sign which is not the case either here or with KCl + KF. Our equation for $\ln \beta$ would result in two peaks and a minimum all at positive values of $-\Delta \frac{1}{C}$, but there really is very little justification in pushing the analysis any further.

Conclusion

The adsorption of KBr from KBr + KF has been shown to be similar to KCl from KCl + KF if the data in the same range of specifically adsorbed charge are compared. The results at large values of q^1 have not previously been observed for halide systems. They can be explained by assuming a standard free energy with both a linear and quadratic terms and variable isotherm parameters. This obviously leaves much to be desired, but nothing further can be done with the present state of the theory. The bromide and chloride results strongly imply that the simpler picture for the iodide ion is due to the limited range of surface charge which was studied.

IV. THE ADSORPTION OF 6-AMINO-HEXANOIC ACID

Introduction

The adsorption of neutral molecules with permanent dipole moments have previously been studied. The most complete investigations have been for thiourea in aqueous solution,^{15,28} and in formamide.²⁹ The sulfur in thiourea is strongly bound to the mercury surface at all but large negative surface charges. This gives the adsorption many of the characteristics of anion adsorption. The purpose of this experiment was to study the adsorption of a permanent dipole formed by two full charges which does not have a strong chemical interaction with mercury. Three amino acids: glycine, 4-amino-butyric acid, and 6-amino-hexanoic were chosen. All are zwitterions in neutral solutions. Preliminary work indicated that glycine and 4-amino-butyric acid are virtually unadsorbed. The electrocapillary curve for .3M glycine in 1MKF and the value of E_z (-.479v) indicated that adsorption was minimal. The differential capacity curve for 4-amino butyric acid (.15M4AB + .5MKF) also indicated very slight adsorption. For this reason the only system studied in detail was 6-amino-hexanoic acid.

Experimental

Eight solutions of xM6AH + .5MKF were investigated. The amino acid was purified by dissolving it in water and precipitating it with alcohol three times. The first precipitate to appear and that remaining after total precipitation were discarded. The differential capacity, the streaming electrode potential, and the surface tension at E_z were measured for each solution. This data is recorded in Table II of the appendix.

Results

The differential capacity curves for xM6AH + .5MKF are presented in Figure 17. The inner layer capacity for .5MKF is shown in Figure 18. A comparison of Figures 2 and 18 or of Table III and IV confirms the lack of specific adsorption in KF solutions. The maximum difference in C^i is less than $.3\mu\text{f}/\text{cm}^2$. This is also the maximum difference between our values and Payne's and is probably due to using different capillaries. Programs I and II were used as discussed in the Appendix except that Program II was changed to a quadratic fit of ξ to $\ln x$, and values of Γ are not as reliable as the value of q^1 in the previous system. This is due to the smaller total variation of ξ with $\ln x$ at constant q . Our original assumption was that this system would show two regions of maximum adsorption. One would correspond to the positive end of the dipole being adsorbed at negative surface charges and the other to the negative end being adsorbed at positive surface charges. This did not turn out to be the case; rather the maximum adsorption at each concentration occurred at $q = -6$. Figure 19 shows the constant charge isotherm for several concentrations. The data do not fit a virial isotherm and the surface pressure values are too low to attempt to fit a Frumkin isotherm. The .01M values are not used in any of the figures, since Program II gave negative values of Γ for some values of q . This is due to ξ being almost constant at low concentration.

Further analysis of the data is in line with maximum adsorption occurring at $q = -6$ and with a quadratic free energy of adsorption. We will begin with the equation for $-\Delta 1/C$.

$$-\Delta \frac{1}{C} = -kT[\Gamma b - b^2 \delta^2 \left(\frac{\partial \Gamma}{\partial \ln \beta} \right)_\mu]$$

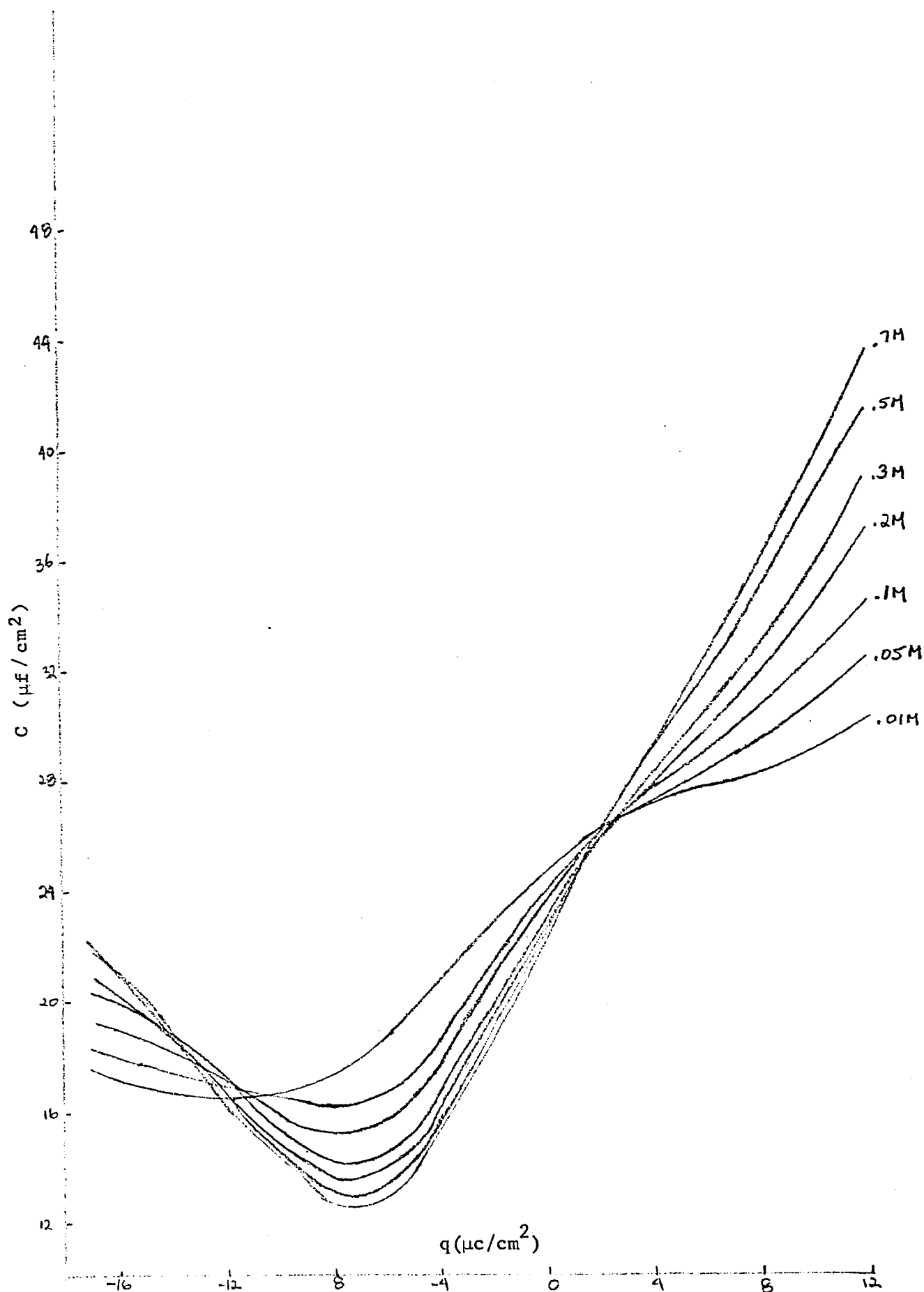


Figure 17. The Differential Capacity of x M 6-amino Hexanoic + .5MKF Acid Plotted as a Function of the Surface Charge Density

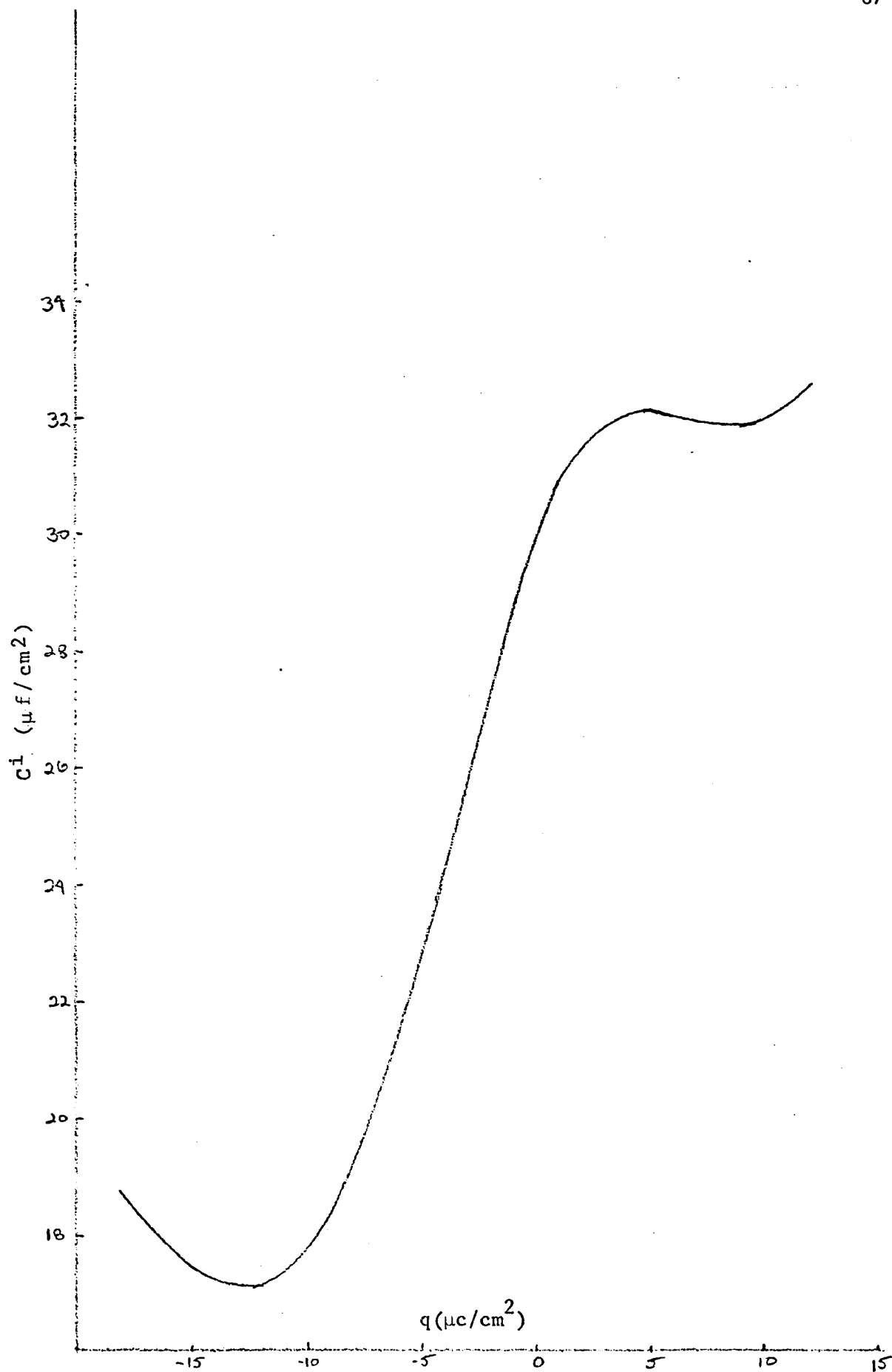


Figure 18. The Inner Layer Capacity of .5MKF Plotted as a Function of The Surface Charge Density

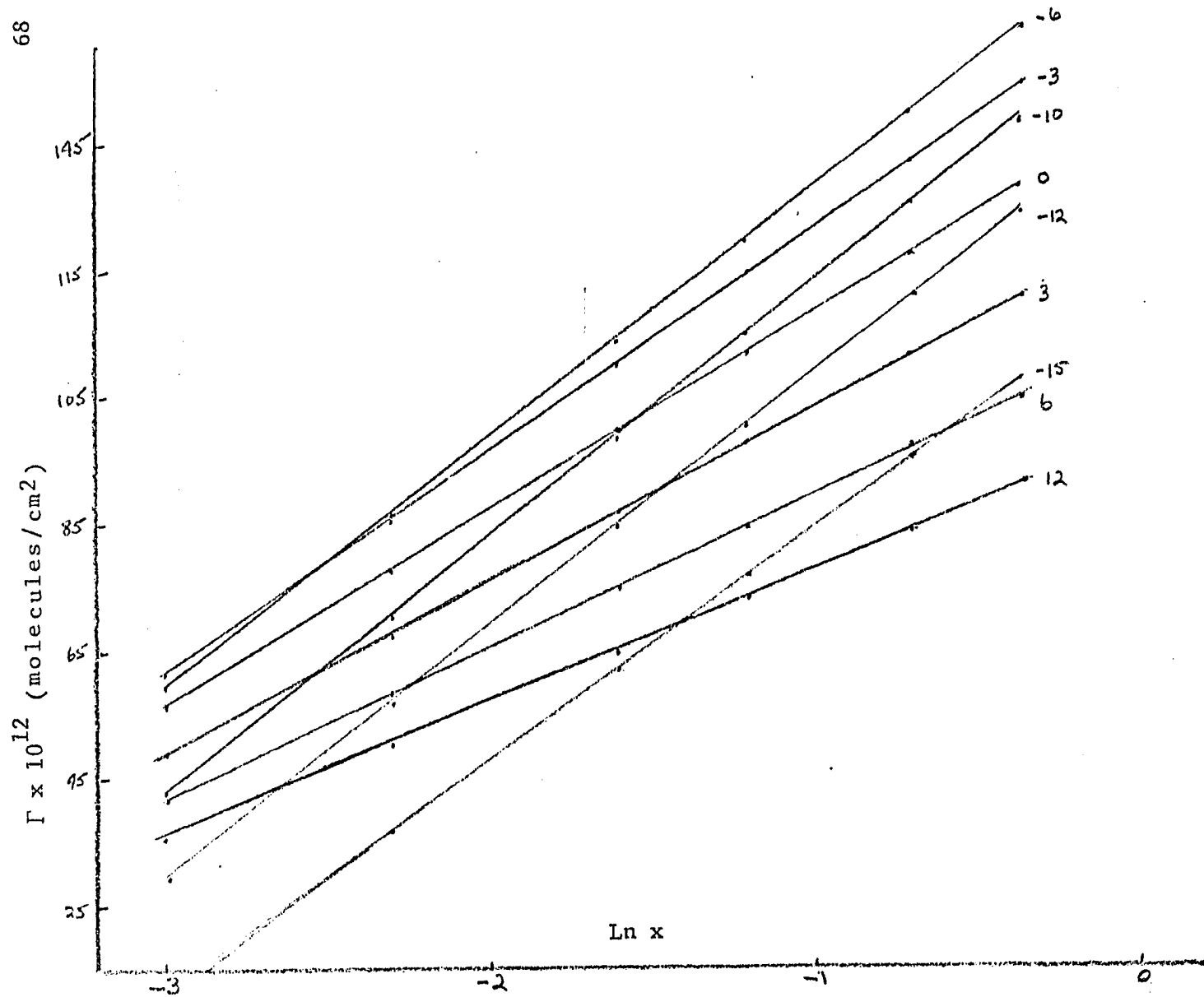


Figure 19. The Amount of xM6-Amino Hexanoic Acid ($\Gamma \times 10^{12}$) Plotted as a Function of $\ln x$ at Constant Surface Charge

assuming

$$\ln \beta = \ln \beta_{\max} - \frac{b}{2} \delta^2$$

$$\delta = q - q_{\max}$$

In Figure 20, $-\Delta 1/C$ is plotted against q for four different concentrations. In this system there is no ambiguity concerning C since C^d is the same in the base solution as in the mixed solution at constant q . $\Delta \frac{1}{C}$ therefore equals $\Delta 1/C^i$. As the equation for $\Delta 1/C$ predicts, the minimum occurs at $q = -6$, $\delta = 0$ and becomes more negative with increasing Γ . In the range of charge available, desorption is not complete so that the curves do not return to $\Delta \frac{1}{C} = 0$ but are still part of the desorption peaks. Figure 21 is a plot of $-\Delta 1/C$ versus Γ at constant q . As expected, the curve at $q = -6$ has the minimum slope which will equal $-kTb$. The quadratic form of $\ln \beta$ is again supported by the plots of ϕ^{m-2} versus Γ in Figure 22. We begin by recognizing that for the adsorption of a neutral compound³⁰

$$\phi^{m-2} = E - E^b \quad q = \text{const}$$

since

$$E = \phi^{m-2} + \phi^2 - \phi^{\text{ref}}$$

$$E^b = \phi_b^{m-2} + \phi_b^2 - \phi^{\text{ref}}$$

and

$$\phi^2 = \phi_b^2$$

$$E - E^b = \phi^{m-2} - \phi_b^{m-2} \quad q = \text{constant}$$

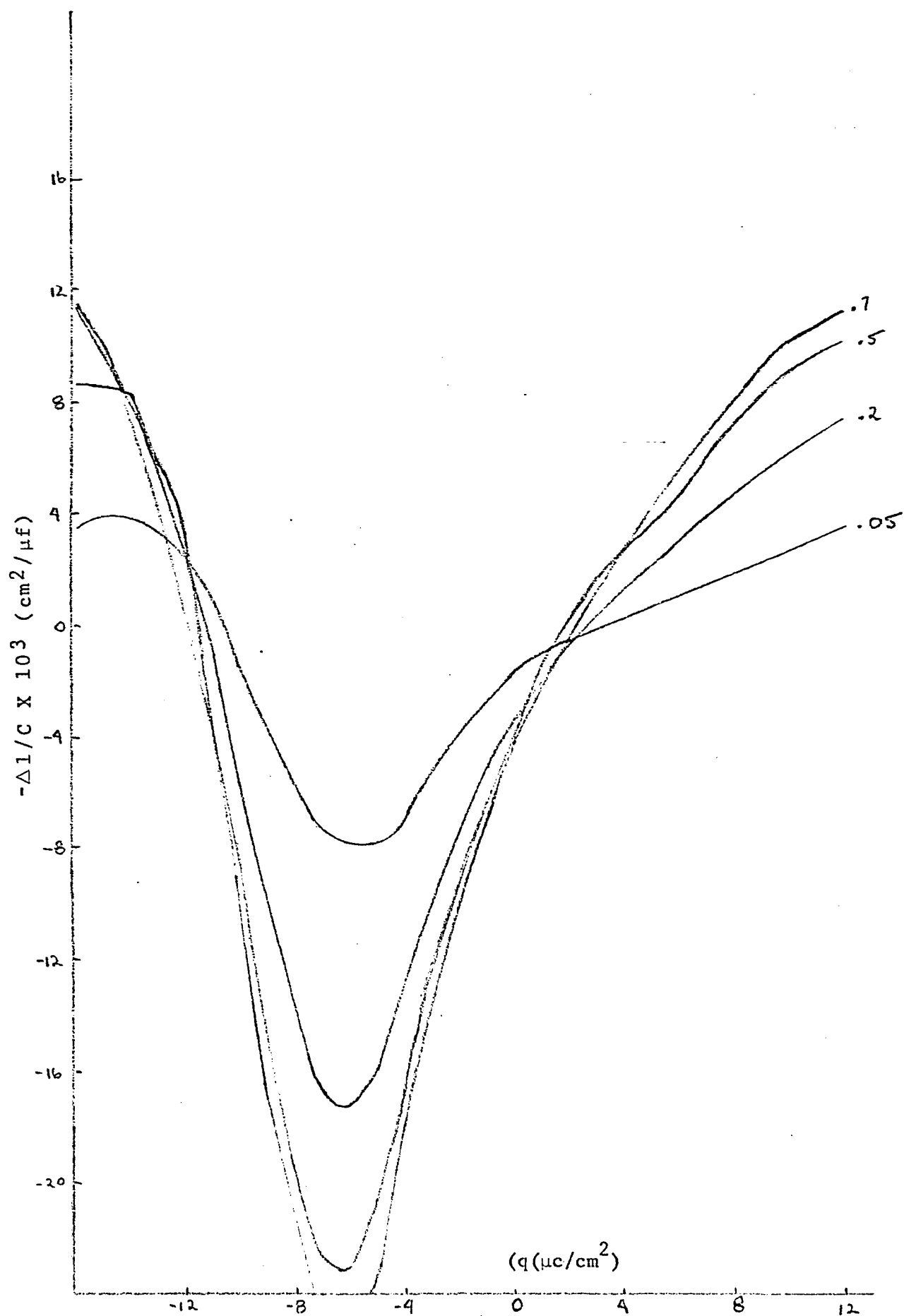


Figure 20. $-\Delta 1/C \times 10^3$ Plotted as a Function of The Surface Charge at Constant Concentration for xM 6-amino Acid + .5MKF

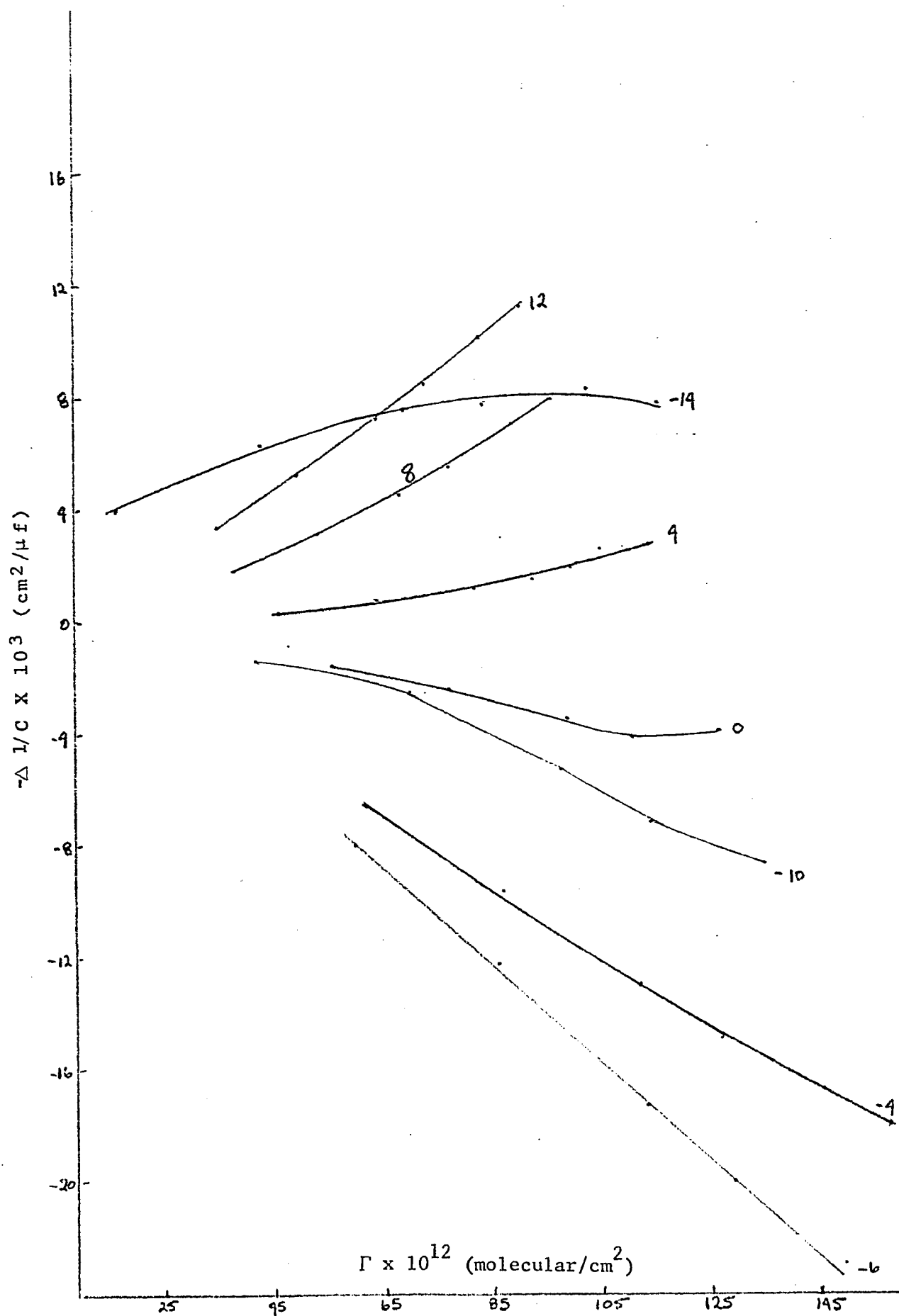


Figure 21. $-\Delta 1/C \times 10^3$ Plotted as a Function of The Amount Adsorbed at Constant Surface Charge for xM 6-amino Hexanoic Acid + .5MF

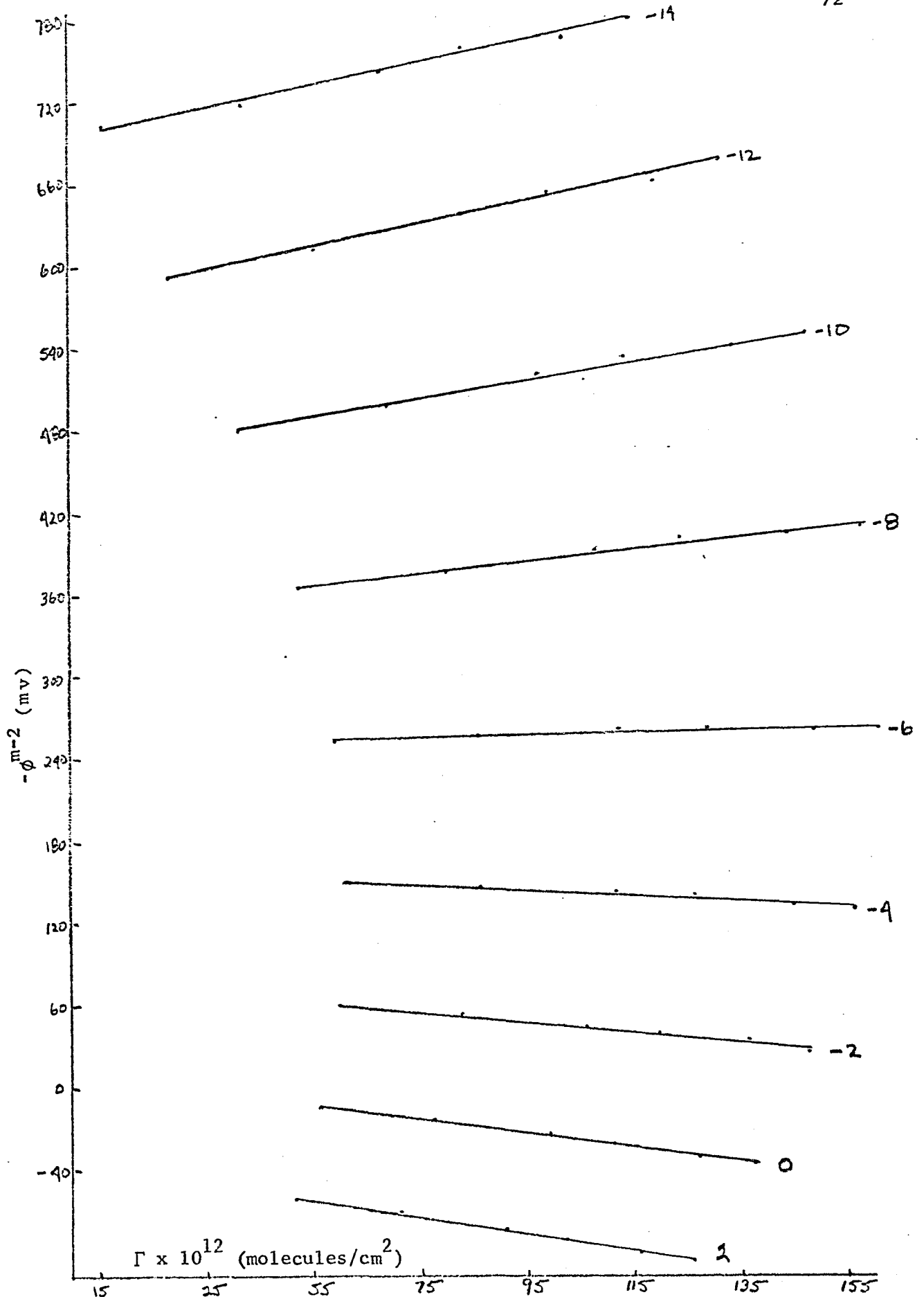


Figure 22. The Potential Across the Inner Layer ($-\phi^{m-2}$) Plotted as a Function of the Amount Adsorbed (Γ) at Constant Surface Charge

Parsons neglects ϕ_b^{m-2} which will change with q . This is justifiable if ϕ^{m-2} can be separated into two terms.

$$\phi^{m-2} = \phi_T^{m-2} + \phi_b^{m-2}$$

ϕ_T^{m-2} is that part of ϕ^{m-2} due to adsorption. We have previously shown that

$$\Delta E = E - E^b = -kT\Gamma \frac{\partial \ln \beta}{\partial q}$$

therefore

$$\phi^{m-2} = -kT\Gamma \frac{\partial \ln \beta}{\partial q}$$

$$\left(\frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = -kT \frac{\partial \ln \beta}{\partial q}$$

In Figure 22, $\left(\frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = 0$ at $q = -6$.

Assuming

$$\delta = q + 6$$

$$\left(\frac{\partial \phi^{m-2}}{\partial \Gamma} \right)_q = kTb(q + 6)$$

This model is correct except at large positive values of q where either b is getting smaller or one of the other assumptions is no longer tenable. Actually if b is not constant, we do not have congruent isotherms and the analysis is no longer rigorous.

Conclusion

Within the range of surface charge available, 6-amino-hexanoic acid is maximally adsorbed at $q = -6$ with a quadratic standard free

energy of adsorption. A quadratic standard free energy of adsorption is to be expected for a point dipole. In this case, the distance between the amino and carboxyl groups is much larger than the inner layer which is only 3-5 Å. It was therefore expected that the system would demonstrate the characteristics of ionic adsorption. It was our expectation that adsorption would be maximal at large absolute values of the surface charge density and that the molecule would reorient itself in the vicinity of the point of zero charge. The quadratic charge dependence implies that adsorption should be considered to occur in the entire double layer rather than be restricted to the inner layer for only then does the point dipole model make sense. The entire double layer for a .5MKF solution has a thickness of 40-50 Å. In line with the quadratic charge dependence, one must assume that water is preferentially adsorbed as $|q + 6|$ becomes large.

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VI. APPENDIX

Table I and Table II consist of the experimental data for the KF + KBr and .5MKF + 6-amino-hexanoic acid system respectively. The procedure for handling both sets of data is identical in all but two respects. All of the diffuse layer cards must be changed since $q^1 = 0$ in the 6-amino hexanoic system and the total ionic concentration is .5M. Care must also be taken not to exceed the maximum permissible exponent in programs where powers of Γ appear. These differences are trivial and the programs and data will be discussed only for the KBr + KF system.

The purpose of Program I is to integrate the experimental capacity versus potential curve. The input for this program consists of Table I. The first and second cards are the title. The second card was always blank since the title was short. The third card gives the initial values of q , γ , E , C , and the concentration, and indicates the direction of integration and whether specific adsorption is assumed. Provision is made to correct E values to E^+ if necessary. For 1MKF, this card consists of experimentally determined values. For all of the x MKBr + $(1-x)$ MKF sets, this card consists of the $q = -19$ values for 1MKF. The following cards in each set consist of the experimentally determined potential and capacity values arranged according to the direction of integration. The program is capable of interpolating the value of C at $q = 0$, but this was not used, rather C was found directly. The program fits the first three points to a parabola and finds all integral values of q which lie between the endpoints. It then drops the first point, reads another point and repeats the process using the previously computed values of the second point as the integration constants. This

procedure is repeated until all of the points have been read. The output consists of E , C , γ , ξ at integral values of q . If no specific adsorption is present, C^d , and C^i and ϕ^{m-2} are also determined. Specific adsorption is assumed absent for KF. This program is a modified version of one originally developed by Payne. Tables III and IV are the output for IMKF and .5MKF respectively.

Table V consists of the output cards of the first program for $q = +4$. The second card is the IMKF card and the next nine are the KBr + KF cards. With the control card, this forms the input for Program II. The second program fits ξ to a cubic equation $\ln x$, the derivative of which is q^1 . It also calculates $\bar{\phi}$, C^d , $-\Delta 1/C$, ΔE , ϕ^2 , ϕ^{m-2} . Table VI contains the printed output of Program II for $q = +4$.

Program III obtains $q^1 C^i$ from a quadratic fit of ϕ^{m-2} to q^1 . Program IV obtains $\left(\frac{\partial q^1}{\partial q}\right)_\mu$ from a cubic fit of q^1 to q . The input cards for both programs are the output cards of Program II. In the first case they are arranged at constant charge and in the second at constant concentration. Program V evaluates C^i , $q^1 C^i$ and $-\Delta 1/C^i$ using the output of Programs II, III, and IV. It can be easily modified to use the constant values of $q^1 C^i$ obtained from Figure 9. The input cards for Program V are shown in Table VII. The first nine cards are the output of Program III. The next card is the IMKF output card from Program I. The next nine cards are the output of Program IV, and the last nine are the output of Program II. All cards are for $q = +4$. Table VIII consists of the printed output of Program V.

Programs VI, VII, and VIII are used to determine whether the data will fit a Frumkin isotherm. Program VI iterates A and θ to give universal plots of $\ln \Phi/kT\Gamma_S$ versus $\ln a\beta/\Gamma_S$. Programs VII and VIII

iterate A and Γ_S and use experimental values of Γ and a to determine the best values of A and Γ_S once a rough fit of A is made. The input cards for Programs VII and VIII consist of the output cards of Program II at constant charge (J indicates the number of such sets). The fineness of the iteration can easily be varied. Program IX simply gives Γ and $\ln a/\Gamma$ which are used to check for a virial isotherm. This would have been included in Program II except that there was not enough space left to print it out.

PROGRAM I
INTEGRATION OF THE CAPACITY

```

C   INTEGRATION OF DOUBLE LAYER CAPACITY
C   L = 1 NO SPECIFIC ADSORPTION
C   K = 1 ANODIC INTEGRATION K = 2 CATHODUC
100 READ(5,20)
    20 FORMAT (55H                                     )
       READ(5,21)
    21 FORMAT(55H                                     )
       READ(5,30)K,CORR,Q1,G1,E1,C1,CON,L
    30 FORMAT(I2,8X,6F10.0,12)
       WRITE(6,40)
    40 FORMAT(37H1 INTEGRATION OF DOUBLE LAYER CAPACITY//)
       WRITE(6,20)
       WRITE(6,21)
       IF(L)404,404,402
402 WRITE(6,51)
    51 FORMAT(1H,4HE(V),5X,9HQ(MC/CM2),2X,10HG(ERG/CM2),2X,11HXI(ERG/CM2
       1),2X,9HC(MF/CM2),4X,3HI/C,10X,2HCD,11X,2HCI,11X,4H)/CI/)
       GOTO403
404 WRITE(6,50)
    50 FORMAT(1H,4HE(V),5X,9HQ(MC/CM2),2X,10HG(ERG/CM2),2X,11HXI(ERG/CM2
       1),2X,9HC(MF/CM2),4X,3HI/C/)
403 IF(C1)22,22,24
    22 READ(5,70)EP,CP
    70 FORMAT(2F10.0)
       READ(5,70)E2,C2
       READ(5,70)E3,C3
       D2=E2-EP
       D3=E3-EP
       A2=C2-CP
       A3=C3-CP
       R=(A3/D3-A2/D2)/(D3-D2)
       S=(A2*D3/D2-D2*A3/D3)/(D3-D2)
       C1=R*(E1-EP)**2+(E1-EP)+CP
       GOTO23
    24 READ(5,70)E2,C2
       READ(5,70)E3,C3
    23 E=E1
       CE=C1
       QE=Q1
       GE=G1
       XN1=0.0
    1  EC=E+CORR
       CR=1./CE
       XIE=GE+QE*EC*10.0
       KE=QE
       IF(L)65,65,400
400 F=11.72

```

```

PH12=2.*.02569*ALOG((QE/F)+SQRT((QE/F)**2+1.))
CD=228.5*COSH(19.46*PH12)
CI=(CE*CD)/(CD-CE)
B=1./CI
PHIM2=E+0.4750-PHI2
WRITE(6,61)E,KE,GE,XIE,CE,CR,CD,CI,B,PHIM2
61 FORMAT(1H0,F7.4,2X,13,8X,F7.2,5X,F7.2,6X,6(E11.4,2X))
WRITE(7,63)QE,XIE,EC,CE,CI
63 FORMAT(F5.1,F8.2,F7.4,2E11.4)
GOTO401
65 WRITE(6,60)E,KE,GE,XIE,CE,CR
60 FORMAT(1H0,F7.4,2X,I3,8X,F7.2,5X,F7.2,6X,E11.4,2X,E11.4)
WRITE(7,62)QE,XIE,CON,EC,CE
62 FORMAT(F5.1,F8.2,2F7.4,E11.4)
401 IF(QE-Q1)11,2,11
2 IF(K-1)3,3,4
3 QE=QE+1.0
GOTO200
4 QE=QE-1.0
200 D2=E2-E1
D3=E3-E1
A2=C2-C1
A3=C3-C1
R=(A3/D3-A2/D2)/(D3-D2)
S=(A2*D3/D2-D2*A3/D3)/(D3-D2)
5 XN=XN1+1.0/CI
N=0
6 XN1=XN-(R*XN**3/3.+(S*XN**2)/2.+C1*XN-(QE-Q1))/(R*XN**2+S*XN+C1)
Y=ABS(XN1-XN)
IF(Y.LT.0.00001)GOTO8
XN=XN1
N=N+1
GOTO(6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,6,7),N
7 WRITE(6,80)
25 READ(5,70)E4,C4
IF(E4-999.99)25,15,15
8 Z=ABS(XN1)
Z3=ABS(D3)
IF(Z-Z3)9,10,10
9 E=XN1+E1
CE=R*XN1**2+S*XN1+C1
GE=-10.*(R*XN1**4/12.+S*XN1**3/6.+C1*XN1**2/2.+Q1*XN1)+G1
GOTO1
10 READ(5,70)E4,C4
G1=-10.*(R*D2**4/12.+S*D2**3/6.+C1*D2**2/2.+Q1*D2)+G1
Q1=R*(E2-E1)**3/3.+S*(E2-E1)**2/2.+C1*(E2-E1)+Q1
IF(E4-999.99)300,15,15
300 E1=E2
E2=E3
E3=E4
C1=C2
C2=C3
C3=C4

```

```
GOTO200
11 IF (K-1) 12, 12, 13
12 QE=QE+1.
   GOTO14
13 QE=QE-1.
14 GOTO5
15 GOTO100
80 FORMAT(32H NO SOLUTION AFTER 20 ITERATIONS)
   END
```

II

Program II - Determination of q

```

$PUFFT
PUFFT VERSION 3/1/68
C CURVE FIT FOR XI = A+BX+CX2+PX3
DE XIE FC CI BASE SOLUTION VALUES
DIMENSION(4,4),VL(6),Y(15),CON(15),X(15),TE(15),OE(15),OC(15),SP(1
15),ASP(15),ACON(15),CS(15)
201 READ(5,109)A,C,EZ
109 FORMAT(13,F5.1,F7.4)
READ(5,402)OE,XIE,EC,CE,CI
402 FORMAT(5,1,F9.2,F7.4,F2E11.4)
150 D=2001*PI*N
200 READ(5,110)Y(1),CON(1),E(1),CS(1)
110 FORMAT(5X,F6.2,2F7.4,E11.4)
08I=1,N
8 X(LI)=.2569*ALOG(CON(I))
AN = N
J = 1
SX = 0.0
SX2 = 0.0
SX3 = 0.0
SX4 = 0.0
SX5 = 0.0
SX6 = 0.0
SY = 0.0
SY2 = 0.0
SY3 = 0.0
D(1,1) = AN
D(2,1) = SX
D(3,1) = SX2
D(4,1) = SX3
D(1,2) = SX
D(2,2) = SX2
D(3,2) = SX3
D(4,2) = SX4
D(1,3) = SX2
D(2,3) = SX3
D(3,3) = SX4
D(4,3) = SX5
D(1,4) = SX3
D(2,4) = SX4
D(3,4) = SX5
D(4,4) = SX6
35 GOTO (42,44,46,48,50),J
42 VL(2,4) = (VL(1,1))*D(2,3)*D(3,4) + D(2,3)*D(3,4)*D(4,2) +
VL(2,2)*D(3,2)*D(4,3) - D(2,3)*D(3,2)*D(4,4) - D(4,2)*D(3,3)*D(2,4)
44 VL(2,3) = (VL(1,2))*D(2,1)*D(3,1) - (D(1,2))*D(2,1)*D(3,1)*D(4,4) +
2-D(2,2)*D(3,4)*D(4,3) - (D(1,2))*D(2,1)*D(3,1)*D(4,4) +
3D(2,3)*D(3,4)*D(4,3) - D(2,4)*D(3,1)*D(4,4)
56437
56437
56451
56451
56467
56467
56500
56531
56531
56542
56564
56567
56571
56573
56575
56577
56601
56603
56605
56607
56611
56613
56615
56626
56634
56644
56654
56664
56674
56704
56712
56722
56736
56753
56755
56757
56761
56763
56765
56767
56771
56773
56775
56777
57001
57003
57005
57007
57011
57013
57025
57042
57063
57111

```

```

4-D(2,4)*D(3,2)*D(4,1) - D(2,1)*D(3,4)*D(4,2)) + (D(1,3))*D(2,1)
5-D(3,2)*D(4,4) + D(2,2)*D(3,4)*D(4,1) + D(2,4)*D(3,1)*D(4,2) -
6-D(2,2)*D(3,1)*D(4,4) - D(2,4)*D(3,2)*D(4,1) - D(2,1)*D(3,4)*D(4,2)
7)) - ((D(1,4))*D(2,1)*D(3,2)*D(4,3) + D(2,2)*D(3,3)*D(4,1) +
8-D(2,3)*D(3,1)*D(4,2) - D(2,2)*D(3,1)*D(4,3) - D(2,3)*D(3,2)*D(4,1)
9- D(2,1)*D(3,3)*D(4,2)))
J = J + 1
IF (J-6) 35,52,52
44 D(1,1) = SY
D(2,1) = SX
D(3,1) = SX2Y
D(4,1) = SX3Y
GO TO 42
46 D(1,2) = SY
D(2,2) = SX
D(3,2) = SX2Y
D(4,2) = SX3Y
D(1,1) = AX
D(2,1) = SX
D(3,1) = SX2
D(4,1) = SX3
GO TO 42
48 D(1,3) = SY
D(2,3) = SX
D(3,3) = SX2Y
D(4,3) = SX3Y
D(1,2) = SX
D(2,2) = SX2
D(3,2) = SX3
D(4,2) = SX4
GO TO 42
50 D(1,4) = SY
D(2,4) = SX
D(3,4) = SX2Y
D(4,4) = SX3Y
D(1,3) = SX2
D(2,3) = SX3
D(3,3) = SX4
D(4,3) = SX5
GO TO 42
52 CONTINUE
A = VL(2) / VL(1)
B = VL(3) / VL(1)
C = VL(4) / VL(1)
P=VL(5)/VL(1)
WRITE(5,200)0
300 FORMAT(8H)CHARGE=F,5.1)
WRITE(6,301)A,B,C,P
301 FORMAT(5H)X1=(,E11,4,3H)*(,E11,4,3H)X2+(,E11,4,3H)X3)
303 FORMAT(1H)O,3HCUN,6X,5HLNCON,4X,3HQSA,5X,2HSP,7X,3HLSP,6X,2HX1,7X,4
1HDIFE,5X,2HCO,11X,2HDE,7X,4HPH12,5X,6HPH1M-2)
IF(EC1400,501,400
501 005021=I,N
DE(1)=0.0
DC(1)=0.0
SP(1)=0.0
ASP(1)=0.0
502 CONTINUE
GOTO500

```

```

400 DS403I=I,N          57530
DE(I)=EC=ET(I)        57541
DC(I)=(1./CF)-(1./CS(I)) 57547
SP(I)=XIF-Y(I)        57562
IF(SP(I)-.005)403,404 57570
404 ASP(I)=ALOG(SP(I)) 57600
403 CONTINUE          57615
500 DS302I=I,N        57616
XIC=A+B*X(I)+C*X(I)**2+P*X(I)**3 57627
QSA=B+2.*O*C*X(I)+3.*O*P*X(I)**2 57661
F=11.72
PHI2=2.*.02569*ALOG((IQ+QSA)/F)+SQRT((IQ+QSA)/F)**2+1.5) 57706
PHIM=E(I)-E2-PHI2
DIFF=XIC-Y(I)
CO=228+.5*COSH(19.46*PHI2)
AC2(I)=ALOG(CO*(I))
4PIE(6,304)CON(I),ACON(I),QSA,SP(I),ASP(I),Y(I),DIFF,CO,DC(I),DE( 60006
I),PHI2,PHIM,X(I)
304 FORMAT(1H0,2(F7.4,2X),F6.2,2X,F7.2,2X,F7.4,2X,F7.2,2X),2(E11.4,2 60074
X),4(F7.4,2X))
406 ARITE(7,406)CON(I),QSA,SP(I),CO,DC(I),DE(I),CS(I),Q,PHIM 60074
406 FORMAT(F7.4,F6.2,F7.2,2E11.4,F7.4,E11.4,F5.1,E11.4)
302 CONTINUE          60141
GOTO201              60142
END                  60143

```

```

**0** EXECUTING

```

22

Program III - Determination of $\left(\frac{\partial q}{\partial \phi}\right)_{n=2}$

```

310      CHPT(1)=2.0193853E-01
320      LEAST SQUARES CURVE FIT FOR LOGARITHMIC EQUATION V = 2 + BX + CX^2
330      DISCRETE VALUES OF X AND Y ARE STORED IN X(1),Y(1) TO X(N),Y(N)
340      N=10
350      X(1)=1.05189
360      Y(1)=1.05189
370      X(2)=1.05189
380      Y(2)=1.05189
390      X(3)=1.05189
400      Y(3)=1.05189
410      X(4)=1.05189
420      Y(4)=1.05189
430      X(5)=1.05189
440      Y(5)=1.05189
450      X(6)=1.05189
460      Y(6)=1.05189
470      X(7)=1.05189
480      Y(7)=1.05189
490      X(8)=1.05189
500      Y(8)=1.05189
510      X(9)=1.05189
520      Y(9)=1.05189
530      X(10)=1.05189
540      Y(10)=1.05189
550      X(11)=1.05189
560      Y(11)=1.05189
570      X(12)=1.05189
580      Y(12)=1.05189
590      X(13)=1.05189
600      Y(13)=1.05189
610      X(14)=1.05189
620      Y(14)=1.05189
630      X(15)=1.05189
640      Y(15)=1.05189
650      X(16)=1.05189
660      Y(16)=1.05189
670      X(17)=1.05189
680      Y(17)=1.05189
690      X(18)=1.05189
700      Y(18)=1.05189
710      X(19)=1.05189
720      Y(19)=1.05189
730      X(20)=1.05189
740      Y(20)=1.05189
750      X(21)=1.05189
760      Y(21)=1.05189
770      X(22)=1.05189
780      Y(22)=1.05189
790      X(23)=1.05189
800      Y(23)=1.05189
810      X(24)=1.05189
820      Y(24)=1.05189
830      X(25)=1.05189
840      Y(25)=1.05189
850      X(26)=1.05189
860      Y(26)=1.05189
870      X(27)=1.05189
880      Y(27)=1.05189
890      X(28)=1.05189
900      Y(28)=1.05189
910      X(29)=1.05189
920      Y(29)=1.05189
930      X(30)=1.05189
940      Y(30)=1.05189
950      X(31)=1.05189
960      Y(31)=1.05189
970      X(32)=1.05189
980      Y(32)=1.05189
990      X(33)=1.05189
1000     Y(33)=1.05189

```

```

300 CONTINUE
      A = VL(2)/VL(1)
      M = VI(1)/VI(1)
      C = VL(4)/VL(1)
      WRITE(6,30010)
30010 FORMAT(1F12.2,2F8.2,2F2.2)
      WRITE(6,3011A)B,C
3011A FORMAT(1D10.5,PHI)=,E11.4,1E4,511.4,3HOSA,114,511.4,5HOSA*2)
      WRITE(6,302)
302 FORMAT(1D10.5,INC,6X,2HOSA,6X,6HPHI,6X,5H2=,1W,8X,5H(SPHI)
      1000000)
      PRINT=,5H(GSA),J,5H,(GSA),J,2)
      PRINT=,5H(2,0*(GSA),J)
      GO TO 1E,0/DEN,1W
303 WRITE(6,304)CON(J),GSA(J),PHI(V(J),PHINC,DOSPHI)
304 FORMAT(1F10.5,1E10.5,1E4,2A,1F8.2,2X,3(F),5,4,2X)
      WRITE(7,305)CON(J),DOSPHI
305 FORMAT(1E10.5,1E4,2,1A,5,6)
306 CONTINUE
      GO TO 291
      END

```

SCALIA
END

Program IV - Determination of $\left(\frac{d\sigma}{d\Omega}\right)_\mu$
STARS

77

CHM201-2701,305,300,1000

\$TD

SPUEEJ

050=H+X+Y+PX3

DIMENSION SA(30),L(30),X(30),Y(30),D(4,4),VL(6)

201 REAO(5,BUO)N,COM

500 FORZ(1,3,FI,4)

DCR011=I,N

REAO(5,2,2)OSAL(1,4,1)

502 FORMAT(7X,6,2,47X,F9.1)

X(1)=05A(1)

501 CALL ABSE

AM = N

SV = 0.0

SV2 = 0.0

SV3 = 0.0

SV4 = 0.0

SV5 = 0.0

SV6 = 0.0

SV7 = 0.0

SV8 = 0.0

SV9 = 0.0

SV10 = 0.0

SV11 = 0.0

SV12 = 0.0

SV13 = 0.0

SV14 = 0.0

SV15 = 0.0

SV16 = 0.0

SV17 = 0.0

SV18 = 0.0

SV19 = 0.0

SV20 = 0.0

SV21 = 0.0

SV22 = 0.0

SV23 = 0.0

SV24 = 0.0

SV25 = 0.0

SV26 = 0.0

SV27 = 0.0

SV28 = 0.0

SV29 = 0.0

SV30 = 0.0

SV31 = 0.0

SV32 = 0.0

```

FD(2,2)*D(3,1)*D(4,2) - D(2,2)*D(3,1)*D(4,3) - D(2,3)*D(3,2)*D(4,1)
S = D(2,1)*D(3,2)*D(4,3) + D(2,2)*D(3,3)*D(4,1)
J = J + 1

```

```

IF (J=6) 35,24,52
44 D(1,1) = SY

```

```

D(2,1) = SX
D(3,1) = SX
D(4,1) = SX
GO TO 42

```

```

45 D(1,2) = SY

```

```

D(2,2) = SY
D(3,2) = SY
D(4,2) = SY

```

```

D(1,3) = SX
D(2,3) = SX
D(3,3) = SX
D(4,3) = SX

```

```

GO TO 42

```

```

46 D(1,4) = SY

```

```

D(2,4) = SY
D(3,4) = SY
D(4,4) = SY

```

```

D(1,5) = SX
D(2,5) = SX
D(3,5) = SX
D(4,5) = SX

```

```

GO TO 42

```

```

50 D(1,6) = SY

```

```

D(2,6) = SY
D(3,6) = SY
D(4,6) = SY

```

```

D(1,7) = SX
D(2,7) = SX
D(3,7) = SX
D(4,7) = SX

```

```

GO TO 42

```

```

52 CONTINUE

```

```

4 = VL(3) / VL(1)
C = VL(4) / VL(1)

```

```

P = VL(5) / VL(1)
WRITE(6,803)CUN

```

```

803 FORMAT(1M1,4NCON=F/4)

```

```

WRITE(6,804)

```

```

804 FORMAT(1M0,1F0,6X,2M0SA,5X,4M0SAC,4X,2M0SAC)

```

```

OSAC = ATN(0.11) * C * 0.11 * 2 * 2 * 0.11 * 3
DSAS = 2 * 2 * 0.11 * 0.11 * 3 * 0.11 * 0.11 * 3 * 2

```

```

WRITE(7,805)DSAC,5(1),CUN

```

```

805 FORMAT(7,4AEP,1AEL,4I)

```

```

WRITE(6,807)0(1),0SA(1),0SAC,0DSAC

```

```

807 FORMAT(1M0,1F0,1,2X,31F6,2,2X)

```

```

808 CONTINUE

```

```

809 GO TO 42

```

```

810 DATA

```

```

FMT

```

-----Program V - Determination of the Components of Capacity-----

```

$PUFFT          56437
PUFFT          56437
C              56450
DIMENSION DQSA(9),CON(9),CD(9),CS(9),DQSPHI(9)
12 DO I=1,9
READ(5,11) DQSPHI(I)
11 FORMAT(7X,F5.1,F6.2)
100 CONTINUE
50 FORMAT(11X,E11.4)
DQI=1.9
READ(5,2) DQSA(I)
2 FORMAT(7.4)
1 CONTINUE
DO J=1,9
READ(5,4) CON(J),CD(J),CS(J)
4 FORMAT(7.4,13X,E11.4,10X,E11.4)
3 CONTINUE
WRITE(6,5)
5 FORMAT(11I,2HQ,F5.1)
WRITE(6,5)
6 FORMAT(1H0,3HCUN,6X,1HC,12X,2HCD,11X,4HDOSA,9X,2HCI,11X,5HDOPHI,9X
176HGSPHI,7X,3HDCI)
DLOK=1.9
REI=.075*(K)-(I-.075*(K))*I+.005*(K)
CI=1.0/R
YEI=.07*CI*-R
PK=(1.0/DQSPHI(K))*DQSA(K)
57.07P
WRITE(6,8) CON(K),CS(K),CD(K),DQSA(K),CI,S,DQSPHI(K),T
8 FORMAT(1H0,F7.4,2X,7(E11.4,2X))
10 CONTINUE
GOTO 12
END

```

***** EXECUTION *****

Program VI

```

10 CHX201-2701,305,300,200 SEARS
SPJFFT
C-FRUMKIN-ISOTHERM
READ(5,1)A,N
1-FORMAT(F5.1,13)
DO6J=1,N
  THETA=0.0
  IF(J.50.1)GOTO12
  A=40.5
  13 WRITE(6,4)
  4-FORMAT(1M1,16)FRUMKIN ISOTHERM
  WRITE(6,5)A
  5-FORMAT(1H0,2HA=F5.1)
  WRITE(6,7)
  7-FORMAT(1H0,5HTHTA,2X,3PHI,6X,4HAPHI,5X,1HB)
  COI=1,23
  IF(1.65.5)GOTO14
  IF(THETA<.07)8,14,14
  8 GOTO(9,10,11),1
  9 THETA=0.01
  GOTO12
  10 THETA=0.03
  GOTO12
  11 THETA=0.07
  GOTO12
  14 0=1
  THETA=(D=3.0)*0.05
  12 PHI=-1.0*ALOG(1.0-THETA)+(A/2.0)*(THETA**2)
  APHI=ALOG(PHI)
  B=ALG((THETA)/(1.0-THETA))+*THETA
  WRITE(6,2)THETA,PHI,APHI,B
  2-CONTINUE
  3-CONTINUE
  6 CONTINUE
  END
$DATA

```

CARD COUNT 6037

Program VII

```

5 ID----- CHM201-2701,305,3050,200 SEARS
SPUFF
C-FRANKIN-ISOHERM-
DIMENSION CON(10),QSA(10),SP(10),O(10),GAM(10),ASP(10)
DO12J=1,2
DO14I=1,5
READ(5,1)CON(I),QSA(I),SP(I),O(I)
1 FORMAT(F7.4,F6.2,F7.2,40X,F5.1)
14 GAM(I)=1.0*QSA(I)*0.60232E+24/U*.964925E+11
DO18L=1,5
P=L
A=7.5*0.1*P
DO15A=1,21
R=K
GAMS=0.1480E+15+0.0020E+15*R
F=C(1)
WRITE(6,6)A,GAMS,F
6 FORAT(1H1,2HA=F,5.1,5X,5HGAMS=E11,4,5X,2H0=F,5.1)
WRITE(6,7)
7 FORMAT(1H0,3HCON,6X,3HGAM,10X,3HQSA,6X,2HSP,7X,4HDIFF,5X,3HSPC,6X,
14HASC,5X,3HASP,6X,3HPER)
DO16X=1,9
THETA=GAM(I)/GAMS
IF(THETA.GE.1.0)GOTO9
GOTO8
9 PHI=0.0
APHI=0.0
ASP(M)=ALOG(SP(M))
GOTO10
6 PHI=-1.0*ALOG(1.0-(THETA)+(A/2.0)*(THETA**2))
PHI=0.135042E-15*298.13*GAMS*PH
ASP(M)=ALOG(SP(M))
APHI=ALOG(PHI)
10 DIFF=SP(M)-PHI
PER=DIFF/SP(M)*100.0
WRITE(6,2)CON(M),GAM(M),QSA(M),SP(M),DIFF,PHI,APHI,ASP(M),PER
2 FORAT(1H0,F7.4,2X,E11,4,2X,7(F7.2,2X))
16 CONTINUE
15 CONTINUE
18 CONTINUE
13 CONTINUE
END
5DATA

```

CARD COUNT 0044

Program VIII

```

5 ID      CHK201-2701,305,t000,200  SEARS
$PUFFT
C-FRUNKIN ISOTHERM
DIMENSION CON(10),QSA(10),SP(10),Q(10),GAM(10),ASP(10)
D013J=1.0
D014I=1.0
READ(5,1)CON(1),QSA(1),SP(1),Q(1)
1  FORMAT(F7.4,F6.2,F7.2,40X,F5.1)
14  GAM(1)=(1.0)*QSA(1)*0.60232E+24/0.064935E+11
D018L=1.15
PEL=
A=4.6+0.2*P
D015K=1.16
R=X
GAMS=0.1600E+15+0.0020E+15*R
F=Q(1)
WRITE(6,6)A,GAMS,F
6  FORMAT(1H1,2HA=F,5.1,2X,PHGAMS=F,11.4,5X,2H0=F,5.1)
7  WRITE(6,7)
7  FORMAT(1H0,3HCON,6X,3HGAM,10X,3HOSA,6X,5SHAETHA)
D016M=1.09
THETA=GAM(M)/GAMS
IF(THETA.GE.1.0)GOTO9
GOTO8
9  ABETA=0.0
GOTO10
8  ABETA=-1.0*ALOG(CON(M))+ALOG(GAMS)+ALOG(THETA/(1.0-THETA))+A*THETA
10  WRITE(6,2)CON(M),GAM(M),QSA(M),ABETA
2  FORMAT(1H0,F7.4,2X,E11.4,2X,F7.2,2X,E11.4)
16  CONTINUE
15  CONTINUE
18  CONTINUE
13  CONTINUE
END
$DATA

```

CARD COUNT 0036

Program IX

```

$PUFFT VEPSION 3/1/68
PUFFT VIRTUAL ISOTHERM
C
12 WRITE(6,J)
1 FORMAT(1H1,15HVIRTUAL ISOTHERM)
2 FORMAT(1H0,3HC0N,6X,3HGSA,5X,3HGAM,10X,1H0,6X,12HL(C0N)/(GAM))
D011=1.0
3 READ(5,3)C0N,QSA,0
4 WRITE(6,4,F6.2,4X,F5.1)
5 GAM=(-1.0*QSA)/(0.6023E+24)/(0.9549E+11)
IF(GAM)4,4,6
4 STOP
6 F=ALOG(C0N)-ALOG(GAM)
6 WRITE(6,10)C0N,QSA,GAM,0,F
10 FORMAT(1H0,F7.6,2X,F5.2,2X,F11.4,2X,F5.1,2X,F8.3)
11 CONTINUE
GO TO 2
END

```

```

56437
56443
56443
56447
56447
56460
56472
56472
56507
56513
56514
56524
56542
56542
56543
56544

```

```

**0** EXECUTION

```

Table I: Experimental Data for XKBr + (1-x)MKF Arranged
As Used For Input of Program I.

1XKF	25	DEG	-0.4750	26.30	1.0	1
1	-0.4413	27.01				
	-0.4119	27.61				
	-0.3815	28.01				
	-0.3516	28.35				
	-0.3214	28.58				
	-0.2905	28.69				
	-0.2606	28.76				
	-0.2307	28.77				
	-0.2007	28.81				
	-0.1703	28.80				
	-0.1404	28.90				
	-0.1106	29.04				
	-0.0608	29.68				
	-0.0124	30.44				
	+0.0367	32.33				
	+0.0699	33.66				
1XKF	25	DEG				
2	-0.5025	25.77	-0.4750	26.30	1.0	1
	-0.5526	24.61				
	-0.6034	23.03				
	-0.6533	21.60				
	-0.7041	20.47				
	-0.7514	19.42				
	-0.8012	18.55				
	-0.8487	17.83				
	-0.8777	17.24				
	-0.9491	16.80				
	-1.0014	16.57				
	-1.0514	16.47				
	-1.1022	16.30				
	-1.1504	16.34				
	-1.2015	16.46				
	-1.2517	16.88				
	-1.3007	16.89				
	-1.3511	17.18				
	-1.4021	17.53				
	-1.4525	17.94				
	-1.4971	18.35				
999.99						
.001	XKR	25	DEG			
	-19.0		-103.053	-1.4914	16.295	.001
	-1.4546	18.04				
	-1.4047	17.59				
	-1.3542	17.25				
	-1.3045	16.95				
	-1.2540	16.70				
	-1.2043	16.50				
	-1.1538	16.30				
	-1.1041	16.35				
	-1.0535	16.59				
	-1.0039	16.54				
	-0.9537	16.81				
	-0.9040	17.23				

-0.8537	17.79				
-0.8040	18.53				
-0.7535	19.46				
-0.7040	20.61				
-0.6549	21.04				
-0.5042	23.52				
-0.5526	25.44				
-0.5040	27.62				
-0.4724	29.08				
-0.4426	30.67				
-0.4127	32.18				
-0.3821	33.51				
-0.3524	34.69				
-0.3225	35.45				
-0.2720	36.20				
-0.2227	37.37				
-0.1727	40.41				
-0.1230	47.61				
-0.0792	64.80				
-0.0496	99.63				
999.99					
005M. KBR 25 DEG					
-1.4515	17.97	-19.0	-103.023	-1.4914	18.293
-1.4021	17.55				.005
-1.3518	17.20				
-1.3024	16.91				
-1.2520	16.66				
-1.2023	15.46				
-1.1520	16.34				
-1.1023	16.30				
-1.0519	16.35				
-1.0023	16.52				
-0.9518	16.80				
-0.9023	17.23				
-0.8521	17.83				
-0.8029	18.65				
-0.7526	19.68				
-0.7030	21.04				
-0.6527	22.86				
-0.6031	25.31				
-0.5526	28.64				
-0.5228	31.10				
-0.4922	34.91				
-0.4625	38.69				
-0.4329	39.13				
-0.4030	41.09				
-0.3719	42.39				
-0.3422	43.28				
-0.3127	44.12				
-0.2825	45.43				
-0.2526	50.12				
-0.1817	61.35				
-0.1324	87.87				
-0.0836	179.00				
999.99					
01 M. KBR 1KDEG					
-19.0		-103.023	-1.4914	+18.293	.01

-1.4520	17.97		
-1.4018	17.59		
-1.3511	17.22		
-1.3011	16.82		
-1.2503	16.48		
-1.2003	16.14		
-1.1507	15.87		
-1.1008	15.53		
-1.0502	15.38		
-1.0004	15.55		
-0.9506	16.85		
-0.9005	+17.31		
-0.8496	17.96		
-0.8018	18.82		
-0.7513	20.04		
-0.7013	21.67		
-0.6507	24.06		
-0.6009	27.47		
-0.5509	32.04		
-0.5150	35.96		
-0.4840	39.15		
-0.4539	41.93		
-0.4239	43.90		
-0.3937	45.34		
-0.3634	46.55		
-0.3335	49.44		
-0.3038	57.08		
-0.2734	74.39		
-0.2431	118.60		
999.99			
.02M .KBR .25 DEG			
1	-19.0	-103.055	+18.293 .02
-1.4538	18.06		
-1.4041	17.65		
-1.3537	17.29		
-1.3041	16.98		
-1.2537	16.73		
-1.2039	16.53		
-1.1535	16.37		
-1.1039	16.34		
-1.0534	16.39		
-1.0035	16.57		
-0.9529	16.86		
-0.9030	17.38		
-0.8513	18.12		
-0.8012	19.13		
-0.7506	20.62		
-0.7006	22.84		
-0.6501	26.14		
-0.6022	30.68		
-0.5751	33.31		
-0.5517	36.59		
-0.5251	39.92		
-0.5019	42.25		
-0.4504	45.91		
-0.4006	47.12		
-0.3501	48.00		
-0.3024	51.93		

-0.2521	58.91				
-0.2025	78.63				
-0.1525	176.5				
999.99					
.04M	KBR 25 DFG				
1		-19.0	-103.093	-1.4914	16.293 .04
-1.4501	18.01				
-1.4018	17.61				
-1.3512	17.24				
-1.3013	16.96				
-1.2507	16.70				
-1.2019	16.53				
-1.1515	16.40				
-1.1018	16.37				
-1.0513	16.43				
-1.0019	16.64				
-0.9513	17.00				
-0.9015	17.56				
-0.8512	18.41				
-0.8014	19.70				
-0.7509	21.64				
-0.7013	24.67				
-0.6512	29.14				
-0.6016	35.08				
-0.5793	37.62				
-0.5513	41.40				
-0.5209	43.70				
-0.5018	46.02				
-0.4758	47.14				
-0.4515	48.09				
-0.4303	48.23				
-0.4050	48.49				
-0.3852	48.64				
-0.3624	47.76				
-0.3031	55.04				
-0.2932	67.29				
-0.2043	338.8				
999.99					
.01M	KBR 25 DFG				
1		-19.0	-103.053	-1.4914	+18.293 +.1
-1.4520	18.12				
-1.4040	17.89				
-1.3543	17.27				
-1.3044	16.76				
-1.2541	16.72				
-1.2042	16.52				
-1.1536	16.43				
-1.1038	16.41				
-1.0539	16.52				
-1.0035	16.78				
-0.9533	17.22				
-0.9039	17.79				
-0.8542	19.20				
-0.8034	21.14				
-0.7532	24.21				
-0.7039	29.50				
-0.6532	34.87				
-0.6036	38.29				

-0.0030 41.94
 -0.0377 44.46
 -0.0534 45.55
 -0.0280 40.03
 -0.0018 40.74
 -0.0414 40.93
 -0.4928 40.98
 -0.0423 47.02
 -0.0400 47.50
 -0.0378 50.04
 -0.0341 50.80
 -0.0320 50.80
 -0.0279 54.88
 -0.0204 57.54
 37797
 -0.025 KBR -25 DEG

-19.0 -103.003 -1.4914 10.293 32
 -1.4941 10.11
 -1.4025 17.60
 -1.3915 17.23
 -1.3018 17.03
 -1.2213 10.78
 -1.2016 10.81
 -1.1913 10.73
 -1.1016 10.23
 -1.0212 10.89
 -1.0012 17.03
 -0.9912 17.09
 -0.9017 10.78
 -0.8015 20.55
 -0.8019 23.41
 -0.7510 27.07
 -0.7022 33.50
 -0.6029 40.11
 -0.5200 43.07
 -0.5054 47.07
 -0.5207 47.07
 -0.5233 48.68
 -0.5291 48.13
 -0.5038 47.23
 -0.4790 49.07
 -0.4518 47.06
 -0.4298 49.44
 -0.4044 50.52
 -0.3798 52.26
 -0.3504 60.84
 -0.2808 70.35
 -0.2317 110.70
 39797
 -0.025 KBR -25 DEG

-19.0 -103.003 -1.4914 10.293 32
 -1.4940 10.69
 -1.4021 17.69
 -1.3917 17.23
 -1.3013 17.03
 -1.2208 10.80
 -1.2003 10.81
 -1.1903 10.77
 -1.1006 10.23
 -1.0202 10.89
 -1.0002 17.03
 -0.9902 17.09
 -0.9007 10.78
 -0.8005 20.55
 -0.8009 23.41
 -0.7500 27.07
 -0.7012 33.50
 -0.6019 40.11
 -0.5200 43.07
 -0.5054 47.07
 -0.5207 47.07
 -0.5233 48.68
 -0.5291 48.13
 -0.5038 47.23
 -0.4790 49.07
 -0.4518 47.06
 -0.4298 49.44
 -0.4044 50.52
 -0.3798 52.26
 -0.3504 60.84
 -0.2808 70.35
 -0.2317 110.70
 39797
 -0.025 KBR 25 DEG

-19.0 -103.003 -1.4914 10.293 32
 -1.4940 10.69
 -1.4021 17.69
 -1.3917 17.23
 -1.3013 17.03
 -1.2208 10.80
 -1.2003 10.81
 -1.1903 10.77
 -1.1006 10.23
 -1.0202 10.89
 -1.0002 17.03
 -0.9902 17.09
 -0.9007 10.78
 -0.8005 20.55
 -0.8009 23.41
 -0.7500 27.07
 -0.7012 33.50
 -0.6019 40.11
 -0.5200 43.07
 -0.5054 47.07
 -0.5207 47.07
 -0.5233 48.68
 -0.5291 48.13
 -0.5038 47.23
 -0.4790 49.07
 -0.4518 47.06
 -0.4298 49.44
 -0.4044 50.52
 -0.3798 52.26
 -0.3504 60.84
 -0.2808 70.35
 -0.2317 110.70
 39797
 -0.025 KBR 25 DEG

-1.1007 16.66
 -1.0504 16.86
 -1.0023 17.42
 -0.9517 18.36
 -0.9013 19.72
 -0.8512 22.38
 -0.8010 26.51
 -0.7512 32.01
 -0.7015 38.30
 -0.6511 42.68
 -0.6034 47.37
 -0.5543 47.58
 -0.5142 45.75
 -0.4693 49.07
 -0.4193 48.95
 -0.3694 48.72
 -0.3160 48.94
 -0.2620 52.28
 -0.2023 60.60
 -0.1326 17.60
 599.99

5% KAR 25 DEG
 -19.0 -103.053 -1.4714 +18.253 . 80
 -1.4518 18.07
 -1.4020 17.70
 -1.3524 17.36
 -1.3029 17.08
 -1.2529 16.88
 -1.2035 16.79
 -1.1536 16.81
 -1.1042 16.96
 -1.0544 17.36
 -1.0048 18.09
 -0.9549 19.43
 -0.9058 21.60
 -0.8559 24.90
 -0.8065 29.37
 -0.7567 35.33
 -0.7072 41.19
 -0.6584 43.83
 -0.6073 45.31
 -0.5517 47.36
 -0.5080 48.12
 -0.4585 48.47
 -0.4079 48.42
 -0.3570 48.19
 -0.3064 48.12
 -0.2518 48.31
 -0.2024 49.19
 -0.1403 53.67
 -0.0723 63.94
 -0.0066 83.52
 999.99
 1%ER 25 DEG
 -19.0 -103.053 -1.4714 +18.253 1.00
 -1.4637 18.30
 -1.4173 18.21
 -1.3719 17.30

-1.4032 17.83
 -1.3578 17.51
 -1.3165 17.27
 -1.2862 17.19
 -1.2642 17.05
 -1.2377 17.00
 -1.2041 16.91
 -1.1552 16.74
 -1.1061 17.17
 -1.0543 17.63
 -1.0040 18.52
 -0.9530 20.11
 -0.9029 22.62
 -0.8524 26.37
 -0.8023 31.44
 -0.7518 37.33
 -0.7019 42.96
 -0.6730 45.42
 -0.6514 46.91
 -0.6227 47.93
 -0.6016 48.32
 -0.5736 48.39
 -0.5512 48.25
 -0.5225 48.09
 -0.5015 48.20
 -0.4731 48.04
 -0.4513 50.06
 -0.4034 53.68
 -0.3530 57.83
 -0.3035 51.06
 999.99

CARD COUNT 0390

Table II: Experimental Data for α M6-Amino Hexanoic Acid

Arranged as Used for Input of Program I:

.5M KF					
1		425.7	-0.4740	25.10	1
-0.4515	25.56				
-0.4015	26.35				
-0.3513	26.92				
-0.3016	27.36				
-0.2514	27.58				
-0.2018	27.81				
-0.1516	28.04				
-0.1020	28.42				
-0.0518	28.97				
-0.0024	29.70				
999.99					
.5M KF					
2		425.7	-0.4740	25.10	1
-0.5010	24.51				
-0.5515	23.54				
-0.6017	22.42				
-0.6515	21.30				
-0.7024	20.20				
-0.7523	19.23				
-0.8046	18.27				
-0.8549	17.57				
-0.9042	17.13				
-0.9537	16.71				
-1.0032	16.42				
-1.0534	16.26				
-1.1036	16.21				
-1.1532	16.24				
-1.2033	16.35				
-1.2528	16.52				
-1.3028	16.78				
-1.3527	17.08				
-1.4022	17.43				
-1.4515	17.98				
999.99					
.01M 6AH					
1		424.1	-0.4656	24.96	0.01
-0.4516	25.14				
-0.4018	26.05				
-0.3518	26.72				
-0.3020	27.20				
-0.2520	27.57				
-0.2022	27.83				
-0.1523	28.36				
-0.1025	28.95				
-0.0525	29.76				
-0.0031	30.95				
999.99					
.01M 6AH					
2		424.1	-0.4656	24.96	0.01
-0.5016	24.00				
-0.5516	22.57				
-0.6024	21.64				
-0.6543	20.46				

-0.7042	19.45				
-0.7542	18.59				
-0.8041	17.81				
-0.8540	17.34				
-0.9041	16.94				
-0.9540	16.65				
-1.0041	16.49				
-1.0537	16.42				
-1.1038	16.41				
-1.1537	16.47				
-1.2037	16.59				
-1.2537	16.78				
-1.3038	17.05				
-1.3538	17.32				
-1.4039	17.62				
-1.4537	18.13				
999.99					
0.05M	6Ah				
1		421.6	-0.4597	24.13	0.05
-0.4515	24.17				
-0.4016	25.48				
-0.3515	26.54				
-0.3015	27.41				
-0.2514	28.12				
-0.2014	28.80				
-0.1513	29.61				
-0.1014	30.59				
-0.0516	31.97				
-0.0019	33.82				
999.99					
0.05M	6Ah				
2		421.6	-0.4597	24.13	0.05
-0.5017	27.74				
-0.5516	21.24				
-0.6021	19.84				
-0.6522	18.63				
-0.6954	17.66				
-0.7506	16.89				
-0.8008	16.42				
-0.8509	16.12				
-0.9019	16.05				
-0.9512	16.09				
-1.0013	16.27				
-1.0664	16.49				
-1.1001	16.77				
-1.1505	17.05				
-1.2008	17.29				
-1.2510	17.56				
-1.3015	17.78				
-1.3566	18.04				
-1.4011	18.30				
-1.4463	18.61				
-1.4880	18.95				
999.99					
0.1V	6Ah				
1		421.3	-0.4506	23.60	0.1
-0.4023	25.12				

-0.3519	26.46				
-0.3020	27.62				
-0.2518	28.60				
-0.2022	29.56				
-0.1520	30.69				
-0.1023	32.06				
-0.0522	33.79				
-0.0023	36.04				
999.99					
.01N-6AH					
2		421.3	-0.4206	23.60	0.1
-0.4519	23.59				
-0.5024	21.96				
-0.5521	20.33				
-0.6028	18.51				
-0.6525	17.57				
-0.7030	16.53				
-0.7500	15.83				
-0.8058	15.38				
-0.8658	15.17				
-0.9039	15.18				
-0.9470	15.35				
-1.0016	15.74				
-1.0512	16.19				
-1.1016	16.62				
-1.1513	17.21				
-1.2015	17.72				
-1.2517	18.17				
-1.3015	18.54				
-1.3512	18.87				
-1.4017	19.17				
-1.4514	19.44				
-1.4797	19.61				
999.99					
G-2K-6AH					
1		416.4	-0.4393	23.07	0.2
-0.4040	24.38				
-0.3537	26.01				
-0.3043	27.49				
-0.2540	28.53				
-0.2047	30.16				
-0.1544	31.80				
-0.1050	33.68				
-0.0549	35.92				
-0.0058	38.75				
999.99					
.2V-6AH					
2		416.4	-0.4393	23.07	0.2
-0.4534	22.67				
-0.5037	20.89				
-0.5532	19.29				
-0.6034	17.80				
-0.6529	16.47				
-0.7050	15.41				
-0.7538	14.70				
-0.8040	14.28				
-0.8535	14.02				

-0.9036	14.14		
-0.9530	14.37		
-1.0031	14.77		
-1.0535	15.31		
-1.1037	15.97		
-1.1534	16.71		
-1.2036	17.48		
-1.2530	18.25		
-1.3033	18.93		
-1.3528	19.34		
-1.4030	19.99		
-1.4522	20.70		
-1.5011	20.50		
997.99			
0.3V	6AH		
1			
		+10.3	-0.4317 22.72 0.3
-0.9012	24.03		
-0.9509	24.81		
-0.9911	27.54		
-0.9708	24.04		
-0.9209	30.70		
-0.9106	22.83		
-0.9109	34.99		
-0.9098	27.89		
-0.9016	40.91		
997.99			
0.3V	6AH		
2			
		416.3	-0.4317 22.72 0.3
-0.9510	22.19		
-0.9515	20.41		
-0.9511	18.78		
-0.9013	17.40		
-0.9512	15.71		
-0.9704	14.88		
-0.9713	14.10		
-0.9813	13.70		
-0.9714	13.32		
-0.9716	13.94		
-0.9717	13.74		
-1.0022	14.14		
-1.0220	14.70		
-1.1025	15.36		
-1.1525	16.13		
-1.2031	17.00		
-1.2500	17.88		
-1.3013	18.77		
-1.3512	19.62		
-1.4016	20.43		
-1.4517	20.74		
-1.4760	21.16		
900.00			
0.3V	6AH		
1			
		+13.1	-0.4219 22.85 0.3
-0.9403	23.80		
-0.9523	23.82		
-0.9302	27.87		
-0.9213	27.84		

-0.2017	31.89				
-0.1517	36.43				
-0.1018	37.30				
-0.0520	40.20				
-0.0022	44.23				
999.99					
0.5N	6AH				
2		413.1	-0.421y	22.65	0.5
-0.4504	41.87				
-0.5007	19.93				
-0.5506	18.20				
-0.6011	16.61				
-0.6510	15.29				
-0.7010	14.27				
-0.7511	13.58				
-0.8013	12.18				
-0.8513	13.03				
-0.9015	13.09				
-0.9515	13.33				
-1.0017	13.74				
-1.0520	14.30				
-1.1004	14.98				
-1.1508	15.79				
-1.2010	16.73				
-1.2518	17.74				
-1.3001	18.75				
-1.3507	19.82				
-1.4014	20.85				
-1.4518	21.71				
-1.4825	22.17				
999.99					
0.7Y	6AH				
1		411.7	-0.4153	22.59	0.7
-0.4013	23.24				
-0.3513	25.32				
-0.3012	27.57				
-0.2512	29.82				
-0.2012	32.11				
-0.1512	35.03				
-0.1016	38.46				
-0.0517	42.23				
-0.0021	46.79				
999.99					
0.7M	6AH				
2		411.7	-0.4153	22.59	0.7
-0.4512	21.24				
-0.5012	19.35				
-0.5512	17.68				
-0.6012	16.21				
-0.6511	14.85				
-0.7010	13.83				
-0.7510	13.17				
-0.8012	12.80				
-0.8511	12.87				
-0.9011	12.87				
-0.9510	12.87				
-1.0010	13.30				

-1.0509	13.83
-1.1008	14.48
-1.1508	15.27
-1.2010	16.13
-1.2510	17.14
-1.3012	18.24
-1.3513	19.39
-1.4015	20.54
-1.4523	21.68
-1.4927	22.78
999.99	

CARD COUNT 0311

Table III: INTEGRATION OF DOUBLE LAYER CAPACITY FOR IMKF

IMKF 25 DLG	$\frac{E}{V}$	$\frac{q}{C(MC/CM^2)}$	$\frac{Y}{G(ERG/CM^2)}$	$\frac{S}{X(ERG/CM^2)}$	$\frac{C}{C(MF/CM^2)}$	$\frac{1/C}{1/C}$	$\frac{c^d}{CD}$	$\frac{c^1}{C1}$	$\frac{1/c^1}{1/C1}$	$\frac{c^{m-2}}{PHM2}$
	-0.4750	0	0	0.2638E-02	0.3791E-01	0.2285E-03	0.2982E-02	0.3353E-01	0	0
	-0.4376	1	-0.19	0.2708E-02	0.3692E-01	0.2293E-03	0.3071E-02	0.3256E-01	0.3304E-01	0.3304E-01
	-0.4012	2	-0.73	0.2778E-02	0.3600E-01	0.2310E-03	0.3156E-02	0.3169E-01	0.6510E-01	0.6510E-01
	-0.3554	3	-1.62	0.2820E-02	0.3546E-01	0.2359E-03	0.3203E-02	0.3122E-01	0.9655E-01	0.9655E-01
	-0.3202	4	-2.56	0.2852E-02	0.3506E-01	0.2414E-03	0.3235E-02	0.3082E-01	0.1276E-00	0.1276E-00
	-0.2852	5	-4.43	0.2868E-02	0.3487E-01	0.2484E-03	0.3242E-02	0.3084E-01	0.1584E-00	0.1584E-00
	-0.2604	6	-5.34	0.2876E-02	0.3477E-01	0.2561E-03	0.3239E-02	0.3087E-01	0.1893E-00	0.1893E-00
	-0.2257	7	-8.60	0.2877E-02	0.3475E-01	0.2661E-03	0.3226E-02	0.3100E-01	0.2202E-00	0.2202E-00
	-0.1909	8	-11.21	0.2881E-02	0.3471E-01	0.2766E-03	0.3216E-02	0.3109E-01	0.2513E-00	0.2513E-00
	-0.1552	9	-14.16	0.2883E-02	0.3469E-01	0.2881E-03	0.3204E-02	0.3121E-01	0.2824E-00	0.2824E-00
	-0.1214	10	-17.45	0.2890E-02	0.3450E-01	0.3004E-03	0.3208E-02	0.3117E-01	0.3136E-00	0.3136E-00
	-0.0873	11	-21.06	0.2921E-02	0.3423E-01	0.3134E-03	0.3222E-02	0.3104E-01	0.3447E-00	0.3447E-00
	-0.0532	12	-24.97	0.2960E-02	0.3379E-01	0.3270E-03	0.3254E-02	0.3073E-01	0.3757E-00	0.3757E-00
	-0.0197	13	-29.15	0.3026E-02	0.3305E-01	0.3412E-03	0.3321E-02	0.3012E-01	0.4061E-00	0.4061E-00
	0.0128	14	-33.55	0.3134E-02	0.3191E-01	0.3559E-03	0.3436E-02	0.2910E-01	0.4358E-00	0.4358E-00
	0.0441	15	-38.08	0.3289E-02	0.3041E-01	0.3711E-03	0.3609E-02	0.2771E-01	0.4643E-00	0.4643E-00

Table IV: Integration of Double-Layer Capacity For .5 MKF

ϕ (V)	ϕ (MC/CM ²)	G (ERG/CM ²)	XI (ERG/CM ²)	C (MF/CM ²)	$1/C$	C^d	$1/C^d$	$\phi^{m=2}$ PHM2
-0.4740	0	425.70	425.70	0.2510E 02	0.3984E-01	0.1616E 03	0.2972E 02	0.3365E-01
-0.4348	1	425.51	421.15	0.2588E 02	0.3854E-01	0.1627E 03	0.3078E 02	0.3249E-01
-0.3966	2	424.93	417.00	0.2642E 02	0.3789E-01	0.1662E 03	0.3141E 02	0.3183E-01
-0.3592	3	423.99	413.22	0.2695E 02	0.3725E-01	0.1718E 03	0.3182E 02	0.3143E-01
-0.3220	4	422.70	409.82	0.2718E 02	0.3679E-01	0.1794E 03	0.3204E 02	0.3121E-01
-0.2854	5	421.05	406.78	0.2744E 02	0.3645E-01	0.1887E 03	0.3211E 02	0.3115E-01
-0.2490	6	419.05	404.11	0.2759E 02	0.3624E-01	0.1995E 03	0.3202E 02	0.3123E-01
-0.2128	7	416.70	401.80	0.2776E 02	0.3602E-01	0.2115E 03	0.3195E 02	0.3130E-01
-0.1770	8	414.01	399.85	0.2792E 02	0.3581E-01	0.2246E 03	0.3189E 02	0.3136E-01
-0.1413	9	410.97	398.25	0.2811E 02	0.3559E-01	0.2385E 03	0.3186E 02	0.3139E-01
-0.1059	10	407.61	397.03	0.2839E 02	0.3523E-01	0.2532E 03	0.3197E 02	0.3128E-01
-0.0708	11	403.92	396.14	0.2874E 02	0.3479E-01	0.2685E 03	0.3219E 02	0.3107E-01
-0.0363	12	399.96	395.61	0.2920E 02	0.3425E-01	0.2843E 03	0.3254E 02	0.3073E-01

INTEGRATION OF DOUBLE LAYER CAPACITY

.5M KF

E(V)	Q(MC/CM2)	G(ERG/CM2)	X(ERG/CM2)	C(MF/CM2)	I/C	CD	CI	I/CI	PHIM2
-0.4740	-2	425.70	425.70	0.2510E 02	0.3994E-01	0.1616E 03	0.2972E 02	0.3368E-01	0.
-0.5144	-1	425.50	420.64	0.2436E 02	0.4104E-01	0.1627E 03	0.2865E 02	0.3490E-01	-0.3423E-01
-0.5552	-2	424.87	435.99	0.2344E 02	0.4257E-01	0.1662E 03	0.2728E 02	0.3668E-01	-0.5999E-01
-0.5998	-3	423.78	441.77	0.2246E 02	0.4452E-01	0.1718E 03	0.2584E 02	0.3870E-01	-0.1076E 00
-0.6454	-4	422.18	448.00	0.2144E 02	0.4665E-01	0.1794E 03	0.2435E 02	0.4107E-01	-0.1475E 00
-0.6922	-5	420.03	454.69	0.2039E 02	0.4903E-01	0.1887E 03	0.2287E 02	0.4373E-01	-0.1899E 00
-0.7435	-5	417.26	461.87	0.1939E 02	0.5157E-01	0.1995E 03	0.2148E 02	0.4655E-01	-0.2350E 00
-0.7964	-7	413.82	469.57	0.1849E 02	0.5427E-01	0.2115E 03	0.2027E 02	0.4934E-01	-0.2830E 00
-0.8517	-8	409.67	477.81	0.1771E 02	0.5666E-01	0.2246E 03	0.1923E 02	0.5201E-01	-0.3336E 00
-0.9092	-2	404.78	486.61	0.1708E 02	0.5854E-01	0.2385E 03	0.1840E 02	0.5435E-01	-0.3868E 00
-0.9686	-10	399.13	496.00	0.1661E 02	0.6070E-01	0.2532E 03	0.1778E 02	0.5625E-01	-0.4422E 00
-1.0294	-11	392.75	505.98	0.1633E 02	0.6124E-01	0.2685E 03	0.1739E 02	0.5752E-01	-0.4991E 00
-1.0909	-12	385.68	516.59	0.1621E 02	0.6153E-01	0.2843E 03	0.1719E 02	0.5817E-01	-0.5570E 00
-1.1525	-13	377.97	527.89	0.1624E 02	0.6158E-01	0.3005E 03	0.1717E 02	0.5825E-01	-0.6152E 00
-1.2139	-14	369.69	539.64	0.1638E 02	0.6105E-01	0.3171E 03	0.1727E 02	0.5789E-01	-0.6733E 00
-1.2745	-15	360.90	552.08	0.1662E 02	0.6016E-01	0.3341E 03	0.1749E 02	0.5717E-01	-0.7309E 00
-1.3341	-16	351.67	565.12	0.1697E 02	0.5894E-01	0.3512E 03	0.1783E 02	0.5610E-01	-0.7875E 00
-1.3924	-17	342.05	578.75	0.1736E 02	0.5761E-01	0.3687E 03	0.1822E 02	0.5490E-01	-0.8430E 00
-1.4492	-18	332.11	592.97	0.1739E 02	0.5591E-01	0.3863E 03	0.1876E 02	0.5332E-01	-0.8972E 00
0					EOF PEAD ON UNIT 00005				---
					EXECUTION TERMINATED				

Table V: Input Cards for Program II.

```

+9..+4.0=0.4750
4.0 -16.07-0.3302 0.2852E 02 0.3430E 02
4.0 -18.26-0.0050-0.3932 0.4150E 02
4.0 -19.47 0.0100-0.4147 0.4435E 02
4.0 -21.03-0.0200-0.4381-0.4642E 02
4.0 -22.63 0.0400-0.4606 0.4782E 02
4.0 -25.26-0.1000-0.4931 0.4892E 02
4.0 -27.95 0.2000-0.5189 0.4922E 02
4.0 -30.52 0.4000-0.5424 0.4909E 02
4.0 -33.19 0.8000-0.5636 0.4846E 02
4.0 -34.57-1.0000-0.5732 0.4659E 02

```

CARD COUNT 0024

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Table VI: Output of the Program II.

CHARGE= 4.0

$$X1 = (-0.3441E-02) + (-0.1771E-02)X + (-0.4309E-01)X^2 + (-0.4577E-02)X^3$$

X	ln X	q	SP	ln q	s	DIFF	CD	$\frac{1}{DC}$	$E-E^b$	ϕ^2	ϕ^{m-2}	X(I)
CON	LNCON	QSA		LSP	XI				DE	PHI2	PHIM-2	
0.0050	-5.2983	-6.00	2.19	0.7839	-18.26	-0.02	0.2318E 03	0.1101E-01	0.0630	-0.0087	0.0905	-1.3611
0.0100	-4.6052	-7.53	3.40	1.2238	-19.47	-0.01	0.2386E 03	0.1252E-01	0.0845	-0.0153	0.0756	-1.1831
0.0200	-3.9120	-9.06	4.96	1.6014	-21.03	0.07	0.2489E 03	0.1352E-01	0.1079	-0.0216	0.0585	-1.0050
0.0400	-3.2189	-10.59	6.56	1.8810	-22.63	-0.08	0.2621E 03	0.1415E-01	0.1304	-0.0276	0.0420	-0.8269
0.1000	-2.3026	-12.62	9.29	2.2289	-25.36	-0.08	0.2836E 03	0.1462E-01	0.1629	-0.0350	0.0169	-0.5915
0.2000	-1.6094	-14.15	11.88	2.4749	-27.95	0.12	0.3022E 03	0.1475E-01	0.1887	-0.0402	-0.0037	-0.4135
0.4000	-0.9163	-15.68	14.45	2.6707	-30.52	0.04	0.3226E 03	0.1469E-01	0.2122	-0.0452	-0.0222	-0.2354
0.8000	-0.2231	-17.21	17.12	2.8402	-33.19	-0.22	0.3443E 03	0.1443E-01	0.2336	-0.0498	-0.0390	-0.0573
1.0000	0.	-17.71	18.50	2.9178	-34.57	0.16	0.3516E 03	0.1440E-01	0.2430	-0.0512	-0.0470	0.

 EOF READ ON UNIT 0005 === EXECUTION TERMINATED

Table VIII Printed Output of Program V.

0^d	c	c^d	$(\frac{\partial q}{\partial q})^d$	DQSA	CI	DQPHI	DQSPHI	$-\Delta \frac{1}{c}$
0.0050	0.4158E 02	0.2318E 03	-0.1132E 01	0.4061E 02	0.2730E 02	0.9439E 02	0.6286E 02	
0.0100	0.4435E 02	0.2386E 03	-0.1229E 01	0.4254E 02	0.2708E 02	0.9160E 02	0.7404E 02	
0.0200	0.4642E 02	0.2489E 03	-0.1299E 01	0.4397E 02	0.2678E 02	0.8897E 02	0.8168E 02	
0.0400	0.4782E 02	0.2621E 03	-0.1345E 01	0.4499E 02	0.2647E 02	0.8648E 02	0.8685E 02	
0.1000	0.4892E 02	0.2826E 03	-0.1367E 01	0.4601E 02	0.2623E 02	0.8339E 02	0.9176E 02	
0.2000	0.4922E 02	0.3022E 03	-0.1355E 01	0.4653E 02	0.2619E 02	0.8121E 02	0.9420E 02	
0.4000	0.4909E 02	0.3226E 03	-0.1318E 01	0.4682E 02	0.2621E 02	0.7914E 02	0.9555E 02	
0.8000	0.4846E 02	0.3443E 03	-0.1257E 01	0.4677E 02	0.2655E 02	0.7716E 02	0.9530E 02	
1.0000	0.4830E 02	0.3516E 03	-0.1231E 01	0.4690E 02	0.2674E 02	0.7654E 02	0.9590E 02	
*#0**	EJF READ UN UNIT 00005 --- EXECUTION TERMINATED							